Appendix A

Supplemental Water Information

		Toppy.

City of Loveland
Estimated Monthly/Annual Usage for Test Year by Customer Class Per Tap Size / Units for Multi-Family
Water Fund

2. 2. Residential (Outside City)						100000000000000000000000000000000000000									
2* sidential (Outside City) 3/4*	82,00	90,404,002 006,000	400 316	30,156,016	112,032,039	162,474,387	272,641,949	333,701,260	120,623,021	276,380,967	183,455,900	104,696,786	94,309,659	107,472	2,173,087,67
Sidential (Outside City)	•	366,200	414,000	475,000	698,760	1,068,300	1,512,000	1,928,400	1,618,800	1,580,400	1,166,800	25.75 26.75	2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2.068.860	21,188,18
	8	6.017.008	***************************************												
	•	24.67	19,867	25,000	178,75	44,714	6000	45,714	C3,857	2012	27,000	27,528	21,476	164,778	\$6.540.000 494.300
2 2	٠.	204.867	100.007	. 744 006	. 5										
ъ	•	387,500	357,000	369,000	300,450	448,300	200,000	474,450	416,850	200	390,750	386.800	442.050	1,560,000	231230
. 50		2 130 620	78.87	77.16	88.5	707,857	12021	1,752,867	1,610,286	1,462,000	1,056,000	744,286	827'53	12,784,429	1274.5
Total Residential	21,218	108,077,251	96,800,702	97,980,456	122,680,495	196,684,581	200,401,411	254.004.953	267,728,478	256,781,873	158,301,473	116,286,786	05,793,418	24, EAS, EAS)	230753487
d-Family 2-6 Units	Y.F. Units														
.5%	1,608	7,170,112	6,436,408	6,581,774	7,122,900	9,128,850	12,000,207	15,332,016	15,507,037	13,244,083	9,638,097	6.894.172	6.676.918	22.86	116.601.20
	1,078	4,601,011	4,146,439	4,219,462	4,308,014	5,286,701	7,096,914	8,069,721	8,449.408	7,932,250	6,367,084	4.652.815	4561.274	64,640	CD.0001.13
	2 8	2386,035	2,006,119	218,48	2342,800	3,301,185	4,400,375	4,051,014	5.863 108	5,413,849	4074,694	2,542,501	2,519,865	195'05	42,015,80
f-Family S+ Units							-			200	460,519	408,301	200,000	200	4,675,37
34.	28	317,639	306,029	230,423	281,300	207,719	348,310	373,342	40,079	354,042	371,201	26.04	250.537	67.123	4005.4
	i 1	27.15	809,334	876,890	990,966	1,001,308	1,222,360	1,292,381	1,410,011	1,360,024	1.182.326	860,329	946.349	41.973	13,063,40
11/2	2 2	2343.867	2.121.500	20000	2 200 337	2745.534	25.50	200	67,206	8	8 38	58,729	66,714	36,656	77.77
N	200	2287,073	2,124,002	2,200,976	2278,177	3,169,369	3,625,177	4,442,978	4,417,806	4,147,910	3133,675	2332.864	2368578	8 8	A THE PARTY OF
h (3	1,966,571	1,734,857	172,737,1	1,22,143	2,421,329	3,239,243	3,896,429	3,977,714	3,820,029	2,909,400	2,032,473	1,304,857	52,52	31,692,57
Total Mutti-Family	607	73,866,777	21,711,006	22,145,534	1,532,867	1,977,867	2,958,571	2,615,000	3,004,000	3,742,000	2,576,067	1,600,814	1,682,414	7,044	28,042,294
								1	W. 10,000	C. 812,919	200000	24,233,781	24,167,010	200,000	200,011,51
ation Accounts - Inside	Y.E. Counts	!	!												
ξ:-	i s	18,337	1	37.6	477,308	2,454,936	4,527,785	5,382,587	5,790,848	5,000,100	3,222,915	599,884	67,618	270,386	27,579,362
1 1/2	8 3	1000	27.00	20,000	2 541 316	1, 571, 551	2317,460	14,130,000	17,740,000	14,913,900	10,156,360	1,496,152	23,200	997.000	80,775,08
N	ā	8.818	20.02	106,276	2,065,492	2,498,381	16.963.475	21.413.967	23,250,646	1900000	10,000,000	2,001,576	136,860	2304,912	133,684,91
h	•	7,724	30.36	3,862	478,897	4,445,103	3,349,241	10,540,586	13,809,501	11,426,759	12,119,310	2564.138	254.807	434774	66 173 78
Anna Clarifornia	~			3,000	17,380	873,080	2,636,500	3,514,200	\$,237,200	4,007,108	3,176,030	201,404	106,000	10,305,991	20,611,96
24*															
; :-				. 3	207		200	25,813	35,36	37,125	33,63	2		25.438	12,57
1 1/2	-					2008	2009	26,000	200	2007	236.160	17,760		394,312	2.54
N	=			10.228	2003	500 300	2 301 500	-	*	2007	200	8 1		2000	8,0
ь	**				208,925	061,750	1,780,000	2,857,500	3,783,000	2.149.300	540,250			200,000	14,000,00
	-					219,500	725,000	1,137,500	1,480,750	1,001,250	463,500	125,000		525.500	5,255.50
aon Accounts - Outside	•	•	•												
1 102	•		8	3	,	11,300	27,000	300,007	318,603	228,667	73.50	12,303	8	455,067	1,367,00
Total Irrigation	338	73.466	178,917	234.803	7,455,905	38,210,104	73,844,636	91,789,500	05.081.298	58.174.807	62,380,550	22,000		2,846,714	2.846.77
and the fact of the same												A COLON PORT	200	2000	473,008,011
DAY OF BRIDGE OF WAY	100	***	*******	***************************************	-										
:-	ă	5,566,792	5,251,730	6.702.833	6477.127	7.000 542	21034	10215.004	10 300 601	0.750.00	200000	2010100	4,570,017	9 1	20,00
1 1/2	r	4,970,729	4352,444	4,928,308	5,026,320	6,285,273	7,773,124	4512.874	\$,281,742	8,787,814	7,692,940	\$277.504	4.656.105	1000000	77.746.16
	ĸ	4,917,916	4,638,679	5,185,996	4770,731	6,944,440	12,010,945	14,237,681	14,518,088	13,742,846	9,822,046	6.022.048	6,281,680	1,417,966	102.000.50
h \$		1,812,009	1,730,560	1,867,500	1,899,990	2,502,004	3,636,944	4,007,571	4,911,562	4,869,576	3,961,800	2,516,169	2,019,148	3,367,236	35,886,55
. 6		200	200.00	01710	2000	600,100	56030	802,308	710,897	1,028.846	222,306	756.638	656,759	1,674,846	8374.23
nercial - Inside with WQC	•				-	1,130,000		1,530,002	200	136176	1,149,429	200.00	8136	4,77,67	14,153,01
34.	8	500,917	161,191	20,00	200,200	1,578,108	2,695,538	2,910,531	340300	2160302	3445.46	100 130	240 847	200 000	
:	*	470,912	437,006	450,230	460,536	1,169331	2229.124	2.597,448	2,634,301	254.63	2003361	750.340	Chamber of the Chambe	506.078	TATA TO
27:1	អ	366,270	362,127	204,079	018,534	1,362,962	2226.50	2,945,887	3,182,317	2,912,730	2,012,476	601,266	411,366	736.886	17530 82
to 8	ដ	1,623,537	1,341,077	1,482,308	1,520,462	3 186,923	5,423,691	6,820,000	7,730,323	7,000 677	5,202,154	2,528,615	1,420,298	2,068,564	46.531.06
h :	2	201,256	1957.641	484,231	551.05¢	1,417,038	2,319,536	3,230,718	1,942,100	3,204,256	2,068,782	508.672	478,141	1,90,42	19,624,271
merchal - Ordaide (No County)	•	200	135,000	194,000	209,000	1 461,200	2,628,000	4244,160	4,985,620	3,374,800	2.142,200	328,600	206,000	6,720,193	20,160,560
3/4"	2	440.047	***************************************	-	*******	-									
;÷	! =	283.250	251.260	270,710	226,700	2017	700,000	200	2,000,075	1,377,200	1,130,667	812,870	20.00	169,765	12,562,613
1.12	**	523,206	67.16	20.00	412.857	339.714	376.571	417.714	240 80	307.000	27.74	200 490	200	20.00	20126
W	~	51,176	Ą	57,547	25,755	164,941	276,624	228,765	246,530	230,341	118,635	76,363	56.166	812 548	1 625 000
	-	22,500	23,750	22,500	18,125	20,625	17,500	22,500	30,00%	21,876	14,210	14,375	10,625	231,290	22,125
The Continue Conti	1138	28,675,774 2	7,478,797	3,000,444	28,687,222	42.016.148	62,979,152	73,386,615	10,670,297	74,307,876	17,644,180	34,547,531	9,606,668	29,046,956	570,253,747
trial - Industrial Rate															
112	-		16,333	20,000	20,000	21,667	16,667	15,330	16,333	15,667	21,067	17,067	18,667	217,333	217,333
u ě	N *	000	20,000	20,200	46,300	50,800	8 3	59,600	009	70,600	73,200	41,800	44,600	323,900	669.800
trial - Wholesale Rate			-	-	-	-	-	0,000,000	World Co.	0,000,000	PARTICIPATE OF THE PARTICIPATE O	4,356,000	4,006,200	23,477,000	58,364,000
h	-		176,667	106,333	116,000	159,000	262,000	236.167	290.007	40:00	249 600	0101	200	2000	
4. Outside	-	- 1	462,100	737,517	418,853	1,006,317	2,324,833	2,217,000	4,794,960	3,466,285	2,158,833	869,633	633,300	19,548,950	10.564.950
Bull modern	-	1	4,282,700	6,242,850	4425.000	6,034,383	8,196,900	8,843,900	12,288,360	10,040,517	6,375,723	5,422,967	\$277.667	53,272,350	63,080,250
Wholesale City - Inside															
34.	•	5,441	87.78	223	8,368	14,265	Z,	20,676	32,363	24,412	16,086	2,674	7,206	35,441	177,206
	= '	57,411	23,534	35,110	2,38	121,603	25.75	220,848	357,411	254,726	133,668	53,656	45,344	151,646	1,668,037
N	. 4	674.000	604.019	2 8	710 047	200	200	120,429	143,200	158,000	278,671	100,114	37,857	382,514	1,912,571
4* - Impation & Pool	~				20,667	424,773	1,066,000	1,568,000	1,860,667	1,473,333	234.067	220.133	2.067	3.735.463	7.478.907
peale City - Outside		ļ		1											
1.12		555	80,1	8 8	8 8	19 1	376	7,125	6,750	8,800	3,125	rî,	3,500	99700	30,230
Total Wholesele City	30	000 870	-	*****	-	-	30.00				-	-			***
				1 000 252	200000	0.000.00	4 744 408	200	*****	2000	21,000	A STON	6,700	315,500	219,300

			" Mary and the second of the s	:
			•	

City of Loveland

Total Usage by Customer Class Per Tap Size / Units for Multi-Family
Water Fund - Average Usage - Fiscal Years 2000 Through 2006

	nnual Avg.	107,472 220,517 2,000 860	164,728 164,728 164,728 1,184,000 1,1848,400 1,2784,423	24,046,640	27, 28, 28, 28, 28, 28, 28, 28, 28, 28, 28	57.5	M.50 M.50 M.50	7,000	20,386	2,304,912	10,306,997	504,312 304,312 7,000,00	6,111,963	465867		153,760 543,412 1,009,880 1,417,986 3,927,986	477.871	228,976 28,876 20,82,62 4,720 150	160,765 231,468 2,374,479	20,20	217,253 228,500 23,477,453	3,680,167	36,441 151,646 382,514 1,183,513 3,738,433	315,000	
	Dec	25.43 26.43	5,401 201,7 20,102 20,103 20,103 20,103	1,873,300	25 25 25 25 25 25 25 25 25 25 25 25 25 2	9 5		3 3	ş	N 8 3	27000		٠.	ā.		9,250 60,000 70,000 70,000 70,000 70,100	\$17,516	7,418 16,462 14,688 68,104 47,814 68,333	22,368	10.65	18,667 22,300 2,253,100	27,000	14. 14. 14. 14. 14. 14. 14. 14. 14. 14.	88	
2006	_	F 25 41	57.7 24.7 12.6 10.6 10.6 10.6 10.6 10.6 10.6 10.6 10	1,417,863	4.00 M	3,4	1 2 3 3	8 8	1987	55.25 25.74 171,44	470,76	3 2 3 3	. 000,251	22,000		10,488 38,488 83,640 83,640 273,204	316,765	2,228 28,485 27,786 28,887 18,887 18,887	10,000 18,410 146,714	14.33	17,647 20,900 2,198,000		25.50 25.50 25.50 25.50 26.30 26.30	E 83	
Y.s 2000 -	8	5,000 8,57,52 000,561	200.8 000.8 000.8 000.8 000.80	1,823,601	864 884 885 885 885 885 885 885 885 885 88	3 5	1335	9	28716	24,063	308.015	2,525 200,51 2,000 2,000	231,625	74,385 43,425		16,773 40,434 97,310 44,020 44,462	300,176	27,797 64,237 91,476 204,878 204,878	20,200 20,200 73,460	16,250	21,667		3,618 12,151 16,714 106,266 417,333		
-Family -	9	34,677	14.38 16.38 16.71 141.80 141.80	2,386,300	827	25	1 4 4 5	2.03	48,217	18.30 18.30 18.30	2001.504	12,375 90,840 3,000 281,879	027,750,1	27,22 20,73		19,000 11,417 100,000 100,000 100,000 100,000	40,500	26.20 20.20 20.20 20.20 20.20 20.20	27,570	21,875	15,667		4,482 11,000 11,		
ut for Mult	Awg	16,500 40,835 250,800	202,21 202,12 202,12 207,95 202,061 202,061	2577.500	27,2 2007, 2007, 3	27.5	1 4 4 9	3.00	56,538	400,000	2,666,600	12,250 14,000 14,000	00,000	106,278		## ## ## ## ## ## ## ## ## ## ## ## ##					16,200 31,300 3,200 3,200,00		29,219 20,066 200,066		
e or Per Ur	35	16,504 41,156 321,400	15,677 28,577 28,167 110,286 128,150	2,907,036	25 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	9 5	E 2007	20.00				10,528 86,330 16,000 286,807				1,690 11,050 11,570 11,740 11,440 11,440					15,333		25.2 26.12 26.00 2		
by Yap Siz	unc	13,484 30,960 252,000	12,610 22,027 24,000 105,071 1,72,000 1,202,571	2,230,967	3 3 4	900	955	7,48				11,188 61,440 16,000 200,238				16,783 16,783 16,683 176,883 176,883					16,667	- 233	822.45 823.82 827.721 800.002		
by Month	Mary	200 miles 200 miles 200 miles	200 X 100 X	1,304,974	2 4 2 2	3,500	2000	100	24,068	20,000	3	3.875 18,120 6,000 64,945	219,000	13,167		0,418 6,729 8,461 7,6461 7,0402	398,963	25 to	14,519 21,246 160,867	20,62	25,600	100621	2,853 11,056 13,229 14,369 12,239	3 85 8	
age Usage	Yes	552 2007 304,811	42.2 42.2 42.2 42.2 62.4 62.4 63.4 63.4 63.4 63.4 63.4 63.4 63.4 63	1 835,673	2 2 2 2 2	3,310	2 2 2 2	3,00	6	20,00	8,600	38.3	ž.	250		478 31,000 64,201 21,110 20,701	74,285	8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	21,70	18.125	20,22		5. 5. 5. 5. 5. 5. 5. 5. 5. 5. 5. 5. 5. 5	35 85	
Awer	Mar	440 2017 2017	002. 00.00. 00.00. 00.00.	1,632,063	2,631	3,417	2,760	272	Ħ	3 2 3 4	8	. 8 . 8		£ .		86,000 36,000 61,970 72,007 200,770 200,700	36.0%	16.25 17.75	24,610 24,610 27,714	22.500	86.00 86.00 81.00 81.00	146,333	25. A 25. A 25. A 25.	8 8	
	2	108	2008 2008 2008 2008 2008 2008 2008 2008	1,659,244	4,007 3,846 2,510	1600	2,807	170	Ε	= F 3 F			• •	Ħ .		8 4 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	338.153	14,098 14,098 16,460 10,358 10,764 10,000	22.000 27.000 27.000 27.000 27.000	87.73	25,00 25,00 30,00		1,147 2,000 11,000 4,000	8 8	
	280	2 6 6 8	12 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2,130,933	3 3 5 3	3,736	8 70 2	3,639	š	8 2 2 3				8 ·		00.0 34.4 34.19 44.19 74.00	30,60	257.2 191.191 190.000 100.000 201.000 700.000	25 M 12 M	22.500	35,000	100,667	2222.2008 20071.2128 25-17-258 00018	SC SE	
П		7,406,157	94,442,122 44,333 78,000 2,312,000 4,798,897 12,794,453	731,036	115,474,623 47,687,003 22,911,148 2,444,143	75,557	AT 251 AND 101	394,000	064,337	713.576 574.286 316.300	722.044	2,816,514 70,000 10,666,129	255,500	171,714 Bel.714 776,300		74,428,566 74,426,566 60,000,522 74,774,713 74,773,67	67,200	200,507 104,625 771,846 964,994	16.557 72.63 73.63	76,291	27,233 20,200 20,000	3,680,167			649'10
	1			"										ľ											3,314,231,63
	1		20,100, 27,012 20,128 20,138 20,139 20,139	П	4410,681 4410,681 1,374,078	340	1,980,1 1,980,5	1,000,01	9788	78.87 78.80 217.31	K			C2 .		4,731,100 5,000,300 3,004,701 2,304,400 2,304,400	A. S.	518.75 52.118.1 52.118.1 52.24	319,500	24,025,080	18.007 31.807 31.874	75,000 633,000 3,977,438	72,000 72,000 72,000 72,000 72,000 72,000	4,067 8,900	146,424,350
	MON	181,001,02 172,037 000,000	527,020 52,020 52,020 52,030 52,030 54,240	100,274,241	6.704.006 4.519.014 1.408.401 2.22.714	20,000	2,110,000	1,600,814	53.03	1,489,386	672,489	12, 2000 10,000	. 000,221	22,000		6,100,000 6,100,000 4,240,000 2,740,743 874,443	70,236	22,44001 22,44000 22,44000 24,777	746,961 277,286 146,714	30,510,410	17,667 23,567 3,140,000	167,667	8,800 18,114 78,314 24,623 24,620	1,265,381	105,824,518
18-Family	3	1,770,000	6,319,336 27,000 77,000 191,000 378,000 1,006,000	174,313,149	3,466,503 6,163,386 2,223,014 246,714	1,092,714	3261.571	2,574,067	2812.151	2072.CS 2073.CS 275.03	2268,500	25,47,81 65,000 1,000,001	463,500	40,43		2,046,454 7,132,570 8,074,900 7,090,700 4,402,000 1,007,714	175,000	2307,161 1,646,57 4,904,857 2,304,857 1,446,74	1,047,160 332,000 138,867	18,877 80,846,78	21,867	2,194,633	17,871 17,851 17,800,1 17,000,1	4,167 21,500 2,961,981	302,319,778
Units for Mu	8	2,782,286	72,702,11 25,128 25,128 25,128 25,129 25,129	240,896,170	13,136,340 7,704,143 2,385,434 236,744	381,000	4,187,286	3,742,000	997'095'	14,423,000	2,842,230	28,236 648,857 9,000 2,374,236	1,001,200	196,000		8,753,541 7,124,814 8,895,380 6,396,429 1,146,429	1,094,286	2272,140 2390,140 6,596,340 14570,467 2,410,577	1,206,681 048,140 17,271 200,439	26,000	16,667	3,466,785	20,714 246,706 166,000 2,600,714 1,678,871	7,203 16,000 4,778,619	436,773,161
or Number o		3,187,781	190,000,1 190,000 190,000,1 190,000,1 190,000,1	314,343,608	16,200,864 8,206,429 3,197,143 3,157,143	1,300,140	4,385,414	3,924,000	5,001,867	14,319,714	3,812,286	2,721,577	2,161,714	273,786 619,429 64,974,776		10,280,507 70,505,77 70,605,27 10,605,286 5,67,737	1,357,143	2,356,000 2,000,714 7,100,343 4,390,629 3,564,014	1,566,707 422,000 170,428	73,55 70,500 70,500	16,333 44,714 4,006,863	4.794,560	95,10 96,754 96,251 palante 786,000,1	8000 38,600,000 6,600,000	113,397,446
Ath by Tap Size or Number	3	221,367,370 3,204,314 803,500	STOLFE STOLE	315,722,443	16,207,287 7,887,086 2,845,686	1,194,623	C.161.286	3 616,000	4,006,671	12.102.57	2,510,143	2,400 2,400 1,400 2,404,714	1,137,500	585,429 584,577 58,610,214		8,642,401 8,008,786 8,002,714 10,282,814 4,482,867	307 0027	2,745,160 2,202,140 2,410,271 6,332,867 3,001,440	1,313,777 388,867 208,867 291,143	28,714 54,014,885	4,000	2217,000	20,000 304,000 120,429 2,881,714 1,580,000	3,600 54,000 4,674,843	10,016,496
Jeage by Mon		2410,429	11,508,701 68,000 68,000 210,143 600,571	57.080,580	12,161,214 6,400,429 2,461,429 270,439	341,286	337.007	2,984,571	3,990,714	12,381,000	1,880,214	28,571 428,87 16,000 1,700,714	726,000	286,714		4,001,000 4,143,600 6,000,140 6,000,071 4,043,271	1,161,667	2,44,240 1,480,487 1,481,774 5,006,284 2,464,614	247,744,1 246,146 240,246	20,000	16,667 40,286 3,740,714	2304,833 4,684,900	22,145 217,867 140,145 2,386,571	3,846,287	6 500 443
May	(au	1,444,000	4,73,4 4,73,4 4,73,4 10,286 10,286 10,286 10,286 10,286	72,919,200	8,084,586 6,134,671 1,880,114 14,000	291,774	2,152,286	1,877,867	2342,043	6,000,744 6,047,643 230,1023	623,629	128,429 1,000 5,000 500,000	219,400	75,000 134,000 815,01,9		5,000,000 5,000,000 5,010,400 7,010,71	*15.00	1,048,443 1,046,673 1,118,143 2,501,143 1,571,590 1,571,590	385,738 300,514 738,837 345,005	22,47.7	21,667 36,286 3,456,143	159,000	13,857 385,814 286,140 386,772,886 917,889	30,500	A576,881 44
Average Me		281,714 281,714 281,180	000,000,000 000,000 000,000 000,000	00000000000000000000000000000000000000	7,046,013 4,184,123 1,223,000 1,73,423	17,72	61,236 1,770,143 2,119,643	1,150,267	616,475	24,000	12,414	2,667	110,306	20,714 2,1,1 5 605,000		4485,286 4878,217 4,075,145 3,446,57 2,111,100 597,867	100,471	40.00 40 40 40 40 40 40 40 40 40 40 40 40 4	200,309 200,000 200,429 116,286	398,714	2,731,429			38,000	740,894 24
	1		2000 B 10,000 B 10,00		(408,300 (408,140 (110,286 140,140	284,571	47,007, 47,007, 720,206	110,017	18.88	8,459 2,605	2,143	. 2 . 2	٠.			4437,194 5,071,294 3,071,007 3,774,413 70,571				ľ	36,867			31,000	354,546 142
2		422,507 422,507 172,500	18,857 18,857 18,857 18,550 17,8,571	4,562,679	420,000,000 000,000,000 000,000,000	738,852 171,188	462,00 1,682,07 1,975,07	1775(476)	2,857	57.73 50.74 50.74				100,001		4,000,000 5 4,000,000 5 3,000,000 5 4,000,000 5 4,000,000 5 6,000,000 5				11	16.333 36.236 2,553,629	- 11		1,200 25,500 30,475 1,	751,569 137.
	1		5,167,600 172,900 172,800 173,700 173,		24.11.72 4.448.70 1.300.666		000000000			8 3 8				1,000		4,000,000 4,000,000 1,000,000 1,000,000 1,000,000 1,000,000				П	15.330 27.420 2.770,867	- 11		- 11	132
Щ		35	2 4 4 4 4	8	233.		300.5700	1				**-				353338		4 4 8 4 5 5	CXXO	× 20		2,50	2 9 8	1	146,50
Avg. YE	Y.E. Counts	17,0	6	20 61	Y.E. Units	* H	8833		Y.E. Cou	. H M 4	of .		-1.51			\$ \$ 8 8 5 °		8 R # R # *	8 2 4	1,036			** 6 ** 5 **	8	25.25
									8		e		alde		200	ı	WGC	į		zināš			79		_
Veter Size	(Inside City)	Outside City	%- <u>5</u> 2254	Residential	Femily 2-6 Units 1* 1 1/2* 2*	34.	7 7 7 7	Atuati-Family	ocounts - ins	, h	1ty - Inflatio	* - 5 "	4° Counts - Out	1 1/2" migation	- Imide no W	\$ - 2 66 6 4 1	- Inside with	\$ = \frac{1}{2} + 8 + 9	** - 2. Y	Commercial	1 1/2" 2" 3" Professele Ret	3" - Outside	11. 1.12. 2. Impation & P.c. Outsidee	1 1/2" Molessele City	ul Classes
Class and	Residentia	Residential		Total	Multi-Famil	Mort-form		Total	irigation A		Wholesale		Irrigation Ac	Total	Commercial		Commercial			Total	Industrial - I	Total	Wholesale C	Total	Total

			(:

City of Loveland

Total Usage by Customer Class Per Tap Size / Units for Multi-Family
Water Fund - FY 2006

	Dec Annual Avg.	4,518 113,472 6,460 230,001 100,104,£ 000,001						1005 44,235						3.20 3.20; per																7,400 210,000				120,000 4.145,000 200,700 41,873,700			15,200 ZZC,200 20,546 1,117,850		
	Nov	338			-	:	2,922	3,000	273	2.507	3,761			22,250 58,300																12,007			. 3	116,000 11			H.200		
	Oct	22.564 22.564 284.500			•		2,007	3,484	2,78	3,734	5 5			258,457																30,000				306,000 1			20,200		
	Sep Sep	38.55 38.50 38.50	20,00	86,200 116,467	0000017.	;	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	\$ 600 800 800 800 800 800 800 800 800 800	3,200	520	3			564,316 444,462 1386,655																27,500				200000		2,800	20,600		22,000
	Aug Aug	16,216 46,200 46,500	41,336	10,000	2,070,000	1	2007.	8 23	855	51.2	10,7%			662.565 562.565																17,400				6.100,000 5			122,500		92,000
	y Tap Size	17,866 45,513 431,000	40,330	16,000 16,000 16,000	2,610,000	1	22.5	4,000	3,200	87.8 64.8	11.291		78,510 258,094	506,171	3,294,000	20,000	16,000	1,461,000	74,300		8	77,152 124,752	178,606	133,000	46,672	188,000	394,800	700%	171,000	28,000				006,000			170,857		90,000
	by Month b	14,720 726,000	18.17 130.00	130,000	2,150,000		8,00	8 8	1 8 8	8,708	8		204,27	647,800 648,720	1,803,000	76.655	346,636	1,360,600	114,000		70.00	106.561	140,197	475,278	46,910	18,70	300,100	20,200	13,000	15,000		000,71	2,280,500	729,000		3,400	151,000		8,00
	May	11.25.21 10.00 10.00	28,333	000 ti	8004		333	419	120	4.079	7.500		27.25 23.25	256,267	960,500	30,05	5,000	443,500	46,000		13.000	200	248,001	319,000	25,730	68,730	272,000	15.977	18,583	27,400		20,000	2,254,000	315,000		1,800	78,071		000'19
	Apr	82.7 80.81			•	;	2,000	3,218	3152	4 5 5	18		17,741	182×		2,125	2,777	22,000	6,667		600	20.00	120,264	113,000 304,000	9,146	8 8 8	2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11,190	15,750	17,500		18,000	1,743,000	346,000		00 11	22,800	1,000	72,000
	Mar	4,162						2,712						2007.							7.688	34.35	113,100	207,000	3	15,000	20,700	9230	218,800	27,200 26,000		36,500	1,586,500	300,000		8 82	000.CI		2002
	E.	172.50						3,16:						2017 2017 2017 2017 2017 2017 2017 2017							7.31	2 2 2	111,001	101,800	730	15,500	2 8 8 1 8 8 8	223	15,417	10,000		12,000	1,387,000	207,000			2,500		
	dan	817.9 157.9 004.00	10,000	175.90	1,800,000	•	3,000	87.5	2,607	2862	41		Ħ.	â ü .	•			•	199		2003	25,775	126,800	267,667	486	18,850	2,000	200	15,917	2,000		14,00	1,363,000	155,000		8 8	9034	۰	37000
	Total	2,190,801,467 19,568,468 6,801,000	ACE, ACE, ACE, ACE, ACE, ACE, ACE, ACE,	2,961,000	18,800,000	10000	62,645,876 34,257,870	5.484.000 4.132.742	000,000,01	47,105,384 34,114,500	30,000,000		90,677,000	117,960,000	25,063,000	3,043,000	19,766,000	11,777,000	1,062,000	000'000'005	80 967 522	65.25.205	34,473,387	7,236,900	23,467,579	16,094,000	19,482,000	12,102,906	1,711,000	3,436,000	0.00	201,000	51,417,000	4,145,000	98,225,700	2,276,000	1,161,000	1,000	28,306,029
	Sec	45,468	13,234	000,000	1,180,000		4340,764	263,742	64,000	1.944.00	1,640,000		4,000	000,000,	2,000				1,000	2,103,000	4405.772	5.143,878	1,062,387	1,672,000	623,539	40,000	000,000	962,099	120,750	18,000	Wer2,019	17,000	3,878,000	280,700	\$,049,700	29,000	76,000		17,000
	Nov	84,622,000 501,000 415,000	13,000	200,000	1,010,000	902249	4,127,100	000,775	38,000	1,971,000	1,485,600		945,000	2,354,000	220,000	٠.	2,000		98	2,191,000	4.808.000	3,573,000	1,563,000	1,000,000	76,500	00,188	200,007	772,440	38,000	152,000	1			2,753,000		26,000	000,100	٠	718,500
	Oct	171,280,611 1,710,000 548,000	30,000	375,000	1,300,000	0.796.000	3,358,000	8 8	972,000	2,901,000	31,403,300		10,064,000	12,223,000	3,130,000	1,000	1,372,000	86,000	20000	94,800,000	8,021,000	7,784,000	3,645,000	756,000	2361,500	2,009,000	1,281,000	963,290	91,000	210,000	2	17,000	5,106,000	3,810,000	9,368,000	11,000	000,191,1		1,461,000
	Sep Sep	2,727,000 2,727,000 76,000	10,915,287	000,000	1,710,000	001 200 61	7.894,000	478,000	1,064,000	3.551,000	3,019,000		16,064,000	16,222,000	3,900,000	25,000	3,307,000	1,366,000	122,000	96,477,000	9364,000	9,978,000	4,990,000	725,000	3,445,000	2,819,000	2,448,000	013,000,1	102,000	294,000		16,000	5,047,000	6,870,000	11,385,000	14,000	103,000 2,424,000 3405,000		3,877,000
	Aug of U	313,677,175 33,70,000 831,000	12,200	348,000	2,070,000	401000	4,770,000	46,000	1.063,000	4,004,000	4,248,000		30,615,000	22,656,000	5,615,000	718,000	14,000	1,500,000	35,000	116,014,000	10,316,000	10,000,000	5,012,000	1,210,000	3,368,000	3,014,000	1,384,000	1,415,700	102,000	35,000		16,000	4534000	42,000	11,218,000	14,000	2,695,000		\$500,000
	Jun Jul	328,140,734 3,580,000 386,000	15,796,731	48,000	2,610,000	900 900	4,554,000	507,000	1,067,000	4,240,000	4,460,000		21,508,000	24,442,000 14,244,000	6,588,000	716,000	36,000	1,300,000	22,000	125 629 000	10,465,000	000,000,00	11,854,000	1,256,000	4,138,000	3,775,000	3,948,000	1,680,270	256,000	566,000		14,000	6,587,000	7,257,000	14,536,000	13,000	2302,000		4,860,000
	Jun	3,44,000	16,066,326	468,000	2,150,000	960	3,727,000	574,000	1,086,000	3,968,000	4,555,000		10,043,000	22,230,000	3,666,000	000,57	3,502,000	1,015,000	342,000	000 172 70	9,238,000	7,165,000	4,405,000	1,429,000	4175,000	2,715,000	3,455,000	1,524,630	139,000	MACOO 000 000 000 000 000 000 000 000 000		17,000	4561,000	778,000 6,774,000	12,139,000	416,000	2,114,000		70,000 4,894,000
	May May	1,568,000	9,448,800	363,000	227,306,122	900000	3,474,000	326,000	915,000 000,17	3,168,000	23,790,000			11,656,000																35,000 55,000	1			3,064,000		218,000	000,000,1		2,731,000
ľ	Apr	114,484,659 548,000 384,000	90,000	298,000	1,180,000	000000	42:6,000	251,000	717,000 71,000	2316,000	1,737,000		1,308,000	3,047,000		17,000	30,000	46,000	17,000	10,285,000	4491,000	3,006,000	1,654,000	912,000	514,000	400,000	266,000	783,250	170,000	38,000		18,000	3,466,000	346,000	6.720.000	122,000	748,000	86,1	1,229,000
	der	384,000	000,00	300,000	260,000	91790	300,920	88 88	668,000	300,000 888,000	354,500		2,000	7,000					900,	11	900,000	400,000	297,000	000,000	000,014	00,00	140,000	576,110	166,000	112,000		18,000	73,000	300,000	000/49	2,000	000'000		000/20
1	H	34,000			11			237,000					0,000	23,000						Ш										70,000	1			1,286,800	1		691,000		751,000
1	8	-			17						17								- 1	1										- 1	1			- 1					П
	- Table	71,000,547 447,000 300,156			- 11	6.247.6	2,161,0	271,000	A K	2,420	1,471,0		R i	3					3	020										10,000	1	2 2 2 2	3,966,0	1,122,400	Pro-	22.22	616,000		27,000
1	Counts - Units	10.001 87 5	¥ ° .	***	20,281	Y.E. Units	2 V	, s	3 8	2 1 2	300	Y.E. Counts	មិនខេ	000'5	**		- :		0 -	340	**	1 3 2	8 =		8 8	88	ō u	R	!! - !	5 2 2		- 4	"			* =	u z u	•	- 8
	Size	24. 27. 146 CITY)		864	6. lented	Units	. ½,	Palls 14°	14.	445	Family	ts - Inside	ž : §	4.6	rrigation	4.			16°	lon	de no WGC	. 6	la h	2 Milh WOC		2.	h =	aide (No Sewer)	2.	arciel	'tal Rarbe	21.	sale Parle	utside	naide	·.	00 th Pool	Outside 4.	Light State City
	Class and Motor	3/4* 1* 2* Residential (Outside City)			Total Resid	Multi-Femily 2-6 L	•	Mutti-Femily 9+ U		-	Total Multi-	Irrigation Accoun			Wholesale City - I				angeron Account	Total Infga	Commercial - Insi			Commercial - Insid	9	- "		Commercial - Out	-	Total Comm	Industrial - Industr	- 14	Industrial - Whole	Total Industry	Wholesale City - L	a.	4 Impa	Wholesale City -	Total Whole

City of Loveland

Total Usage by Customer Class Per Tap Size / Units for Multi-Family

Water Fund - FY 2005

	Annual Avg.		98,137 192,333 106,000 1,106,000 1,2130,000 19,410,000		41,340 40,001 88,400 88,800 46,373 46,373 60,001		73,667 394,145 607059 1,228,000 8,274,000 8,677,000		14,226 14,226 14,14,14 14,14,16 14,100 14,100 14,100 14,100 14,100	222,147 572,448 814,222 1,989,000 2,001,384 7,432,600	156,866 287,251 1,796,000 510,133 280,000	210,000 27,000 2,190,000 4,190,000 5,190,000 5,190,000	25,400 11,101,101 13,102,400 1,002,400 1,000 1,000 1,000 1,000
	å		\$,001 \$,000 \$4,000 114,000 154,000 15,000,000 1,000,000		25.0 20.0 20.0 20.0 20.0 20.0 20.0 20.0				47.6 64.65 17.65 18.00 19.00 10.00 1	8 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	8848 804,111 804,111 804,013 804,013	14,000 26,000 1,001,000 1,110,000	000 8000 8000 8000 8000 9000 9000 9000
	Nov		4.814 28.000 28.000 28.000 28.000 28.0000 28.0000 28.0000 28.0000 28.0000 28.0000 28.0000 28.0000		3,468 3,000 3,000 3,000 3,000 3,000 1,000	4,896 74,047 13,423		8 8	27.22 27.22 27.22 27.22 20.22	251.0 251.0 200.0	8,161 16,077 80,000 00,000 00,000	000,00 00,000,00 000,000,00 000,000	06.00.00.00.00.00.00.00.00.00.00.00.00.0
b-Family	8		611.8 505.61 500.15 500.00 500.00 500.00 1300.	5,779 5,681 4,641 3,246	4,000 4,000	34,904 127,488 294,809 347,115 3,274,500	25,000 60N02 127,70 264,000 56,000	16,000	15,549 45,874 90,273 162,000 163,000 416,000	20,101 00,101 20,000 20,000 20,000 7,000 000 000 000 000 000 000 000	15,487 30,154 86,000 81,466 20,000	2,264,000 2,264,000 2,204,000 2,204,000	2,600 18,000 101,363 686,000
nit for Mus	Sep	78,81 28,85 000 Mil	408,51 600,00 84,000 87,000 87,000 12,000,000 2,000,000,2	2007 2007 2004 2004	117.2 50.6.2 50.6.2 50.7.5 50.7.5 50.7.8	186,723 188,196 196,772 460,400 1,008,406 25,575,50	16,000 88,000 877,675 1,313,000 686,000	CCC,232	14,600 174,156 354,417 146,000 34,417	34,022 106,001 24,002 266,000 1,517,001	36,230 36,230 36,000 36,000 30,000	15,000 4,500 17,000 5,45,000	2,000 24,231 16,400 167,813 608,000
o or Per U	Aug	000,01 000,04 000,050	36,036 36,000 87,000 82,000 122,000 2,256,000	810.6 604.7 609.8 700.7	200 M	18,042 18,043 18,7,043 2,004,300 3,617,000	21,000 104,429 204,125 1,500,000 1,646,000	74 SEC 300	21,754 21,254 21,255 21,050 20,000 20	00,75 110,004 100,767 100,004 100,004 100,004	77,273 86,208 14,000 760,001 10,000	17,000 23,000 33,40,000 12,601,000	4,000 34,000 34,000 1,174,000 1,000,000 1,000,000
by Yap Stz	Jul.	271,81 03,02 000,705	41,088 41,000 41,000 197,000 2,180,000	2334	3 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	84,746 884,871 900,000,000,000,100,100,100,100,100,100,	522.9: 58,485 50,405 25,73,73 500,807,1	86,00	7.00.20 2.00.00 2.00.00 2.00.00 2.00.00 2.00.00 2.00.00 3.00 3.00.00 3.00.00 3.00.00 3.00.00 3.00.00 3.00.00 3.00.00 3.00.00 3.00.00 3	78,000 78,000 136,000 201,000	12,730 26,300 171,000 12,000 1.	36,000 36,000 36,000	3,400 3,410 3,410 3,000
by Month	nn	24,702 24,713 88,883	000,021 000,021 000,024 000,024,1 000,002,1	8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	# # # # # # # # # # # # # # # # # # #	24,00 008,00 78,000 211,00 008,000 005,100	20,000 89,867 82,000 745,000	57,867	17,223 16,180 16,480 27,430 14,200 14,200 14,200 14,200	24,810 244,810 244,810 244,810 802,500	25.24 200,441	2,545,500 2,545,500 345,500 345,500 6,452,500	3,000 26,385 25,000 335,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 355,000 35
age Usage	Mey	500 1000 1000	6.880 34.000 36.000 36.000 36.000 36.000 36.000 36.000 36.000 36.000 36.000 36.	REES	2002 2002 2003 2004 2004 2004 2004 2004	14,500 102,162 116,816 227,500 172,700	5,667 6,000 3,000 1,000 10,000	136,000	2000 2007 2007 2007 2007 2007 2000 2000	98,000 111,70 101,80 10	814.01 80.00, \$1,000 \$1	21,500 21,500 212,000 21,501,500	2400 11,815 18,400 24,600 113,400
Aver	Apr		4,342 0,000 101,000 100,000 1,000,000 1,000,000		2022 2002 2004 2,423 3,423 3,433	201.0 201.0 100.0	2000		2.62.2 2.62.2 2.62.2 2.62.2 2.60.3 2.60.3 2.60.3 2.60.3 2.60.3 3.	2 C M M M M M M M M M M M M M M M M M M	25 26 25 25 25 25 25 25 25 25 25 25 25 25 25	800,007 000,007 	88 827, 4 8 445
	Mar		212.00 22.000 21.000 21.000 21.000 21.000 21.000 21.000 21.000		2002 2002 2004 2004 2004 2004 2004 2004	88.3	· · · · · ·	a .	20,4 21,10,7 21,10,0 20,0,7 20,0,0 20,0 20,	2 X X X X X X X X X X X X X X X X X X X	14-00 27-00 7-00 7-00 7-00 7-00 7-00 7-00	20,000 3,107,500 3,44,000 2,522,100	80.1 8.43 8.43 9.43 9.43 9.43 9.43 9.43 9.43 9.43 9
	Peb de		41.4 26.00 26.000 26.000 26.000 12.000,012,1		2,002 2,400 2,400 2,100 2,100 3,100 3,100	s	awg	8 .	2477, 247,16 247,16 247,16 27,16 27,16 20,18 20,	5722 5423 5423 5423 5623 5623 5623 5623 5623 5623 5623 56	7,288 16,000 20,000 700,000	000,17.7. 000,187.7. 000,187.7. 000,187.7.	8 11 8 11
	Jan	28.	\$251 \$200 \$200 \$400 144,657 306,000	4,150	442 6 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	3.84			SAGE CALCO CACO CA	5,467 18,81 18,667 18,000 17,000 18,0	25,11 25,000 20,000 20,000 20,000	16,000 28,000 1,20,400 30,000 10,000 10,000	00 2452 2000 0000 57004
	Total	373,102,008,1 373,000,004,71 374,200	84,225,100 677,000 347,000 2,210,000 12,150,000 18,450,000	161,757,800 62,747,800 26,148,200 4,756,000	3,481,000 11,567,000 788,000 42,884,000 36,284,000 27,281,000 362,582,000	24,625,000 62,619,000 107,246,000 61,127,000 44,816,000 22,606,800	28,000 2,688,000 6,346,000 6,346,000 5,077,000	3,257,000	77,966,600 61,286,400 72,296,900 76,701,622 30,798,700 7,635,000	19,992,300 16,401,300 1,425,000 22,015,000 24,662,000	10 994,800 3.384,000 1.794,000 2.70,380 380,000 484,700,661	210,000 740,000 52,772,000 4,150,000 54,500 54,500	127,000 2344,000 872,000 17,722,000 1,000 1,000
	2	374,000	20000000000000000000000000000000000000	000,000 000,000 000,000 000,000	156.000 712.000 64.000 2.542.000 2.642.000 2.642.000 22.542.000	24,000 27,000,000,000,000,000,000,000,000,000,0		88	5,245,000 5,245,000 5,247,000 5,647,	25,200 26,000 26,000 26,000 26,000	11,000 11,000 12,000 12,730	18,000 53,000 53,000 63,000 6,140,000	0012 00012 00012 00012 00012 00012 00012
			2000 2000 2000 2000 2000 2000 2000 200		27,000 6,000 2,34,000 2,37,000 1,74,000 2,1,74,000 2,1,74,100 2,1,74,100	400,000 970,000 970,000 78,000		8 8 8			"		25,000 25,000 50,000 501,000 280,000 51,000
	Nov	-	ľ					3,61000	4,716,000 4,716,000 3,736,000 1,382,000 946,000 942,000	2 8 2 2 2 2	F 8 2 5 8	18,000 3,100 3,807,000 6,603,000	~ 11 21 25 25 E
mily	8	203,000	4,184,00 21,00 21,00 20,00 20,00 20,00 20,00	8,148,000 6,101,000 3,007,000 000,000	354,000 1,000,000 1,000,000 3,000,000 3,117,000 32,600,000	1281,000 10,454,000 11,812,000 16,225,000 4,602,000	26.00 26.00 26.00 26.00	57.134.000	00,1627, 00,000, 0,000,000 0,000,000 4,25,000 1,000,000,000	2,792,000 2,853,000 1,790,000 6,183,000 2,230,000 1,560,000	21,002,479 24,000 34,000 35,245,389	20,000 2,000	00.01 00.01 00.07 00.01 00.01
Units for Muttl-Fa	ges	206,506,018 3,157,000 552,000	00,142,11 00,152 00,000 00	1275,000 7225,000 7225,000 725,000	304,000 1,340,000 71,000 5,746,000 4,046,000 3,386,000 42,847,000	\$228,000 15,422,000 21,500,000 11,372,000 \$,687,000 \$,151,000	44,000 614,000 1,313,000 878,000	196,000 77,000 71,076,000	3,445,000 6,455,000 10,000,722 4,192,000 675,000 1,000,000	3,002,000 3,002,000 2,002,000 4,003,000 3,003,000 3,003,000 3,003,000	1,140,200 47,000 126,000 720,000 50,0	15,000 87,000 4,936,000 217,000 5,456,000 10,481,000	11,000 311,000 82,000 2,000,000 1,070,000
fumber of	Aug	3,327,000	00,252,00 72,00 72,00 72,00 73,00 70	4,724,000 4,104,000 900,000	1 30,000 67,000 4,421,000 4,675,000	\$,566,000 15,566,000 25,164,000 15,370,000 7,322,000	000.00 000.000 000.000 000.000 1.448,000	230,500 632,000 84,967,000	11,417,000 10,174,000 11,375,000 4,736,000 486,000 1,000,000	4,775,000 1,346,000 2,601,000 1,046,000 1,800,000	072,002,1 000,002 000,001 000,001 000,001	17,000 6,600.000 5,620.000 12,000.000 10,138,000	2,340,000
ap Size or P	3	736,400 ,482,000 (\$1,000	13,130,000 121,000 191,000 412,000 1,720,000 2,180,000	20,130 20,130 20,130 20,00 20,00	36,000 1,277,000 8,000 1,786,000 4,727,000 4,727,000 4,747,000	964,000 340,000 047,000 091,000	40,000 623,000 2,043,000 1,514,000	254,000 MG,000 MG,000	7,372,889 9,346,000 7,250,000 12,092,000 3,227,000 600,000 1,080,000	26,200 26,000 21,200 20,200 20,200	2000 78,000 78,000 17,000	14,000 64,000 34,000 34,000	14,000 14,000 14,000 14,000 14,000 14,000 14,000 14,000 17
Touth by T		•	ľ		- 11			- 11				- 11	88888 8
Usage by A	Sun Jun	4	000,052 000,053 000,053 000,052 000,052 000,052 000,052 000,052 000,052 000,052	1	424,000 990,000 67,000 1,1460,000 1,1460,000 2,479,000	1,777,2 1,000,0 1,000,0 1,000,0	60,000 419,000 90,000 900,000 746,000	177. 188. 187. 189.	8,098,111 8,138,000 6,342,000 8,644,000 3,318,000 740,000 880,000	2,006,0 2,006,0 2,007,0 2,007,0 1,006,0	2.022 0.347 0.050	16,000 64,000 4,687,000 366,000 11,864,000	14,000 3-41,000 12,000,000 6-71,000
ared Total	May	900,204 900,000 428,000	24,000 24,000 34,000 342,000 342,000 342,000 342,000 342,000 342,000	00,777,800 4,400,000 1,001,000,400	19,000 87,000 64,000 2,285,000 2,287,000 2,005,000	1,380,000 4,000,000 1,130,000 344,400	27,000 24,000 36,000,000,000	30,000 136,000 14,473,280	4,886,000 6,6802,000 4,961,000 7,362,000 730,000 700,000	26,000 2,130,000 26,000 26,000 26,000	000,425 000,425 000,625 000,03	21,000 457,000 121,000 151,000	13,000 151,000 151,000 27,000 27,000 1416,800
Moss	ă	198,300	200.000 200.000 300.000 300.000 300.000 300.000 300.000 300.000	88,000 61,200 34,000	172,000 740,000 840,000 7,76,000 1,776,000 1,877,000 1,887,000	100,000 306,111 306,000 118,000 23,000 51,900	88		3,478,000 1,996,400 1,000,000 2,000,000 2,000,000 2,000,000 4,000	27,000 71,000 64,000 12,000	25,880 25,000 15,700 15,700	1,420,000	4,000 33,000 74,000 74,000
	-		ľ								٦		
	Mor	κ.	140000 140000 12000 12000 140000 140000		257,000 74,000 2,187,000 2,287,000 2,287,000 1,276,000 2,776,000			- 11	6,088,000 6,000,078,2 6,000,078,2 6,000,078,1 6,000,088 6,000,088	614.0 467.0 1,850.0 1,550.0 1,500.0	2,107 2,018 2,003 2,005	80,000 6,715,000 8,216,000 9,316,100	000.00 000.00 000.00
	ş	20,766,60 201,00	20,000,000,000,000,000,000,000,000,000,	4,127,000 4,272,000 1,439,000 336,000	216,000 718,000 60,000 1,604,000 1,404,000 1,404,000	000.E 000.E		1,000	4,004,000 4,000,000 1,000,000 47,000 1,000,000	277,000 277,000 246,000 4,000,000 115,000	510,170 200,000 80,000 80,000 90,000	73,000 744,000 74,000 74,000 74,000 74,000	200 4 4 000 45 7 0000
	Jen	400,000	4,816,000 16,000 186,000 26,000 26,000 16,00	6,746,000 4,463,000 2,074,880 261,000	25 005,195 E8 05,100 T	000 at		8	4,978,000 6,098,000 4,192,000 4,022,000 1,238,000 390,000	462,000 462,000 338,000 477,000 100,001	800,340 354,000 24,000 86,000 86,000 86,000	16,000 36,000 336,000 1,046,500 6,306,500	4,000 285,000 41,000 718,000
3	Units	E 8 "	8 8	9455	2888388	§ x a 4 x ~ ~		e - E	32888000	88885"	8 2 - 0 - 6	- ~ ~ ~ ~ ~	22254 - · 6
Year	Y.E. Cou			Y.E. Uni		9 9							
		92					. 8		g 9		· · ·		
	and Moter Size intial (Inside City)	3/4* 1* 2* mtsa (Outside Chy)	\$ - E 10 to to 0	amily 2-6 Units 34" 1" 1" 1" 2" 2" 2" 2" 1" 1" 2" 2" 2" 2" 2" 2" 2" 2" 2" 2" 2" 2" 2"	Account to the last of the las	on Accounts - Insk 34° 112° 27° 3° 3° 3° 4° ale City - Infection	34* 112* 72* 74 74 64*	34° 1 1/2° obsi irrigation	arcial - Inside no W 3/4* 1 1/2* 2 2 2 3* 4 6 6 6	7	344 1 1/2 2 2 2 2 2 2 4 2 4 3 4 4 4 4 4 4 4 4 4	al - Industrial Rate 1 1/2" 3" al - Wholesale Rate 4" - Ovrside ntal Industrial	Wholesale City - Inides 3/4 1/7 1/7 1/7 1/7 1/7 1/7 1/7 1/7 1/7 1/7
				~ 4	Le .	. 9							

City of Loveland Total Usage by Customer Class Per Tap Size / Units for Multi-Family Water Fund - FY 2004

	M Avg.	90,198 181,449 #ONUD	91,623 124,000 424,000 912,000 1,426,647 11,515,000	50,000 50,000 50,000 50,000	67,864 48,000 58,277 57,748 67,748	200,200 200,007 200,007 772,40 600,180	34,000 36,887 4004 970,000 3,000,000 236,687	56,533 57,883 57,889 56,500 56,000 66,000	216,143 448,887 786,888 786,888 1,870,888 86,748,888	50,134 06,730 01,000 70,667	241,000 202,100 000,114,17 000,1182,20	36,000 172,006 170,400 1,199,200 2,004,300 26,000 26,000
	ec Annu		4,000 12,000 12,000 12,000 11,000 10,	8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	3,120 2,200 3,100 3,200 3,200 3,200 3,200 3,200 3,200 3,200 3,200				331255		21,000 2 21,000 3 21,000 27,4 21,000 5,2	2,227 6,600 1,600
	Nov C		4.00 M 00.00 M 00.00 M 00.00 M 00.00 M		4 3 0 3 0 5 C 5 C 5 C 5 C 5 C 5 C 5 C 5 C 5 C 5						14,000 2 22,500 2 2008,000 2,15 367,000 21	000,1 000,000 000,000 000,000 000,000
	Oct		2000 2000 2000 2000 2000 2000 2000 200	4,972 4,197 3,1908 2,790	200 M 100 M		64,675 12,887 12,887 12,000 14,000 14,000 14,000		22 4 15 15 15 15 15 15 15 15 15 15 15 15 15		2000 2000 2000 2000 2000 2000 2000 200	2,600 17,100 17,000 100,633 200,000 1,000
	for Mutti-F		4 10 10 10 10 10 10 10 10 10 10 10 10 10	6,00 8,00 1,00 1,00 1,00 1,00 1,00 1,00 1	5333354		5,500 5,443 6,443 184,500 184,000 184,000 184,000 184,000		20,200 118,700 270,400 202,304 202,304		17,000 24,000 2,500,000 2,000,000 1,000,000	2,000 2,000 3,000 1,000 11,000 11,000 1,00
	Average Usage by Month by Tap Size or Per Unit for Multi-Family for Multi-Family for May Jun Jun Jul Aug Sep Oct	28,672 28,679 60M/0	2002; 2002; 2002; 2006;	5,480 5,480 2,880	5336538	20,200 166,203 407,841 408,731 1,374,000 2,209,000	SELOT STANCO STANCO COLOMA, COLOMA, CO	25,27 25,28 110,270 110,270 10,270 200,214 200,284	35,012 76,138 36,300 36,300 26,500 2,175,000	117,81 20,825 000,91 000,92	2,286,000 2,286,000 2,11,130,000 2,130,300 2	22,00 22,00 22,00 22,00 32,00 40,00
	by Tap Size		21C.21 22.000.02 20.000.02	4 3 4 3	200 200 200 200 200 200 200 200 200 200	44.67 194.67 191.82 191.60 191.60 191.60 191.60	2000 2000 2000 2000 2000 2000 2000 200	16,485 116,710	31,200 20,100 20,100 200,700 200,800 1,100,000	207,71 C15,02 C20,021 C20,021	14,000 27,000 2,344,500 4,100 2,106,000	2,000 20,400 24,000 11,157
	by Month		195.01 795.02 795.02 795.02 785.00 78		228222		6000 24,000 36,000 36,000 46,000 26,000 26,000	25.12 25.28 25.28 25.00 25.00 20.00	27.24 20.17 20.100 20.100 20.100 20.100 20.100	221,122 221,123 231,030 732,84 700,00	86.75 86.08 86.02 86.72	2,600 18,400 18,400 004,301 000,1
	rage Usage May		8,613 19,233 40,000 20,000 147,000 977,000 2,016,000		6 4 8 9 9 4 8		. 17.51 20.003 20.002 2	25,43 24,43 200,88 200,881 200,881 200,881	21,316 20,730 80,231 180,186 112,664 770,600	14,413 22,520 22,520 72,520 10,000 10,000	24,000 2,415,000 206,000	2,600 10,697 14,800 10,667
	Apr		2020 2020 2020 2020 2020 2020 2020 202		2 4 612 2 4 612 2 4 613 2 6 613 2 6 613 2 6 613				7,7 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5		200 M 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	1,000 1,000
	Mar		31.6 00 31.00 00 71.00 00 71.00 00 20.00 00 190.00 190.00 190.00		# # # # # # # # # # # # # # # # # # #				25.00 20.00		22,200 24,500 300,100,100	2,244
	- Feb		\$177 \$401 \$233 7,607 \$2,000 25,000 \$2,000 72,000 \$2,000 700,607 \$2,000 700,607 \$181,40 1,181,500		400 1386 400 400 400 400 415 100 2501 234 3470 100 400 100				2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	8 = 8 B · · · · · · · · · · · · · · · · · ·
	lab.	450	~ 4 4 4 5 5 4	र र त त	******		ş	3 58 58 57 57 57 57 57 57 57 57 57 57 57 57 57	562.2 594.21 594.21 594.72 596.72 596.72	2 4 2 3 3	20,000 20,000 1,000,000 0	1200,0001 0000 0000 0000 0000 0
	Total	00,000,000	94,281,000 372,000 45,000 4,284,000 4,287,000 11,515,000 27,777,510	34,809,000 62,313,000 24,600,110 3,204,000	3,547,000 10,262,000 312,000 31,642,000 31,642,000 315,541,110	18,007,000 58,186,000 68,591,000 52,898,000 28,006,000	2,071,000 2,071,000 2,601,000 3,500,000 1,044,000 1,044,000	75,531,800 72,150,400 60,577,000 77,605,000 73,605,000 8,730,000	12,156,000 13,047,000 14,507,000 17,127,400 13,896,000	10,353,800 4,076,000 1,801,000 2,162,000 90,000	341,000 64,834,000 64,834,000 14,944,500	130,000 1,952,400 82,000 17,348,000 6,256,000 21,000 21,000 21,000
	Dec Dec	97,004,811	4,223,000 13,000 44,000 164,000 381,000 865,000 12,900,000	6.455,000 4.257,000 1.880,110	255,000 828,000 82,000 23,70,000 2,127,000 2,145,000	26,000 2000,1 2000,1 2000,1 30		000 100 171,000 1716,000 1716,000 1716,000 1716,000 1716,000	30,000 36,000 44,200 54,300 14,000	576,500 337,000 57,000 57,000	21,000 53,000 4,311,000 115,000 115,000 115,000 115,000 115,000 115,000	200001: 00001: 000001:
	tov	84,881,388	4467,000 22,000 38,000 72,000 308,000 1,510,000		200,000 734,000 44,000 1.984,000 1.986,000 1,386,000 1,386,000	310,000 1,014,000 1,000,000 271,000 377,000			100,000 167,000 100,000 1,000,000 116,000	17	9 000'990'9 9 000'29' 9 000'80'9	2000 20100 20100 20100 20100 20100 20100 20100
		1,144,000	27,000 27,000 27,000 137,000 305,000 1,600,000 1,600,000		380,000 877,000 118,000 2,598,000 2,588,000 2,546,000 78,882,000 78,882,000		000,000 000 000,000 000 000,000 000 000,000 000 000,000 00		1,880,000 1,388,000 1,510,000 3,846,000 1,646,100		82,000 4,940,000 66,000 1,178,000 1,	11
	off-Family Oc		*				ľ					
	Units for M	1,284,000	31,000 31,000 31,000 162,000 17,000 18,000 1,000,000 1,000,000 1,000,000		384,000 1,034,000 84,000 4,134,000 3,440,000 2,440,000 35,494,000	3200. 10.41.1. 10.41.4. 10.42. 10.42. 10.42.	000,124 000,124 000,000 000,000 000,000 000,000 000,000	4,847,400 7,380,000 6,200,000 1,841,000 100,100 100,000 100,000 100,000	2.005,0 1.009,0 2.276,0 6.469,0 2.225,4 1.465,0	A81.1 0.000 0.001 0.000 0.001 0.001 0.001	000,71 000,87 ,000,000 ,000 ,000,000 ,000,000 ,000,00 ,000,00 ,000,00 ,000 ,000 ,000 ,000 ,000 ,000 ,0	1,000 301,000 81,000 2,251,000 1,236,000
	r Number o	2,237,000	20,000,000 2	11,263,361 50,863,00 3,014,00 303,875	462,000 962,000 642,000 3,447,300 3,477,000 3,677,000 3,677,000	3,506,000 12,400,000 17,946,000 10,663,000 6,496,000 4,673,000	000,249 000,249 000,000,1 000,000,1 000,000,1 000,000,1 000,000,	9,177,20 00,000,00 00,746,0 00,287,0 00,287,0 000,000	2,734,000 2,734,000 4,126,000 2,502,000 4,340,000 4,340,000	383,000 383,000 285,000 285,000	17,000 34,000 8,912,000 1,131,000 8,130,200 1,224,300	26,000 235,000 111,000 2,863,000 1,460,000
	Month by Tep Size or I	2,136,000	11,238,000 64,000 10,000 10,000 10,000 1,286,000 1,286,000 1,286,000 1,286,000	11,687,611 7,000,000 2,600,000 312,000	362,000 1,096,000 77,000 8,402,000 3,846,000 3,130,000 31,130,000	3,868,000 11,282,000 13,694,000 4,094,000 2,888,000	1,600 1,861,000 1,294,000 781,000 100 1	8,1940,700 8,194,000 8,496,000 10,364,000 378,000 386,000	2,621,000 2,004,000 2,344,000 6,344,000 2,900,000 2,200,000	372,000 372,000 300,000 300,000 300,000 300,000 300,000	14,000 54,000 4,777,000 044,000 7,694,000	14,000 120,000 12,697,000 1,446,000 1,446,000 4,787,400
	Jun	2,301,000	374,000 20,000 34,000 34,000 1,110,000 1,814,000 206,130,811	0,914,000 6,254,000 2,694,000 361,000	258,000 1,002,000 84,000 3,445,000 2,948,000 2,948,000 34,816,000	0,284,000 0,284,000 4,115,000 1,190,000 1,190,000	2,000 2,000 26,000 36,000 1,00	7,284,000 7,234,000 4,201,000 8,197,000 4,807,500 480,000	272,000 267,000 (482,000 (47,200	37,000 37,000 134,000 284,000 16,000	17,000 00,000 6,004,000 641,000	1,000 1,000
	Total Usage		64,000 40,000 40,000 41,000 500,000 5,000,000 5,000,000		284,000 863,000 60,000 2,344,000 2,744,000 1,984,000 1,884,000 1,884,000	2,586,000 2,542,000 7,246,000 9,000,000 1,000,000 1,000,000 1,000,000 1,000,000					\$ 000'00" \$ 000'00" \$ 000'00"	13,000 91,000 91,000 320,000 200,000 1,000,000
	Measured	-	1				ľ					
	Apr	104,700,970	2,000 2,000 34,000 340,000 340,000 340,000 340,000 340,000 340,000 340,000 340,000 340,000 340,000		203,000 794,000 72,000 2,249,000 2,259,000 1,449,000 27,606,000	2,286,000 2,286,000 2,46,000 3,4,000	31,000	2,707, 2,500, 2,	007,000 000,000 000,000 000,000 000,000	246.0	2,200 4,000 4,751,000 26,007,000	45,000 63,000 923,000 5,000 1,048,000
	Mar	2000 2000 2000 2000 2000 2000 2000 200	1,500 1,100 1,100 1,500	6.310,000 4.096,000 1.431,000 21,000,715	304,000 74,000 2,004,000 1,942,000 1,346,000 20,513,000	800.12 800.02 80.13		4,746,000 4,746,000 3,446,000 1,156,000 480,000	000,000 000 000,000 000 000,000 000 000,000 00	27,703 960	22,000 24,000 191,000 171,000	6,000 84,000 64,000
	£	386,000	2000 2000 2000 317,000 70,000 70,000 70,000	4,001,388 2,502,000 1,480,000 228,000	21.00 21.00	§§		4,187,000 8,013,000 3,388,000 1,778,000 40,000 80,000	28,000 28,000 28,000 28,172 28,172 28,172 28,172 28,173 28,173	578,790 223,000 197,000 66,000 19,000 12,781,890	13,000 2,7,000 3,255,000 3,419,000	000, 1, 000, 15, 000,
	Jan	86,106,632 647,000	21,000 31,000 31,000 31,000 31,000 21,001,000 500,000	4,300,000 1,346,000 247,000	337,000 776,000 86,000 1,996,000 2,125,000 1,396,000	8	8.	4,346,200 1,716,000 1,716,000 1,400,000 3,710,000	466,000 387,000 1,388,000 414,500	4000 44000 44000 10000	16,000 27,000 3,041,000 109,000	600 21,000 34,000 602,000 602,000 603,000 7,000 1,000
	- Units	18.610 M	M 2 - 4 2 60	* 3 3 2 8	2 # 8 E # 3 # 8	86184.	ar	84828**	****	E 5 - 0 - 00.1	- " " - " "	45484 6
	Counts Y.E. Cou			Y.E. Un		i 3						
						5 8	. 1	0	io Sower)	27200	e E	3. 2
	Meter Size	34° 1° 2° (Outside C	A : - 12 : 12 : 12 : 12 : 12 : 12 : 12 :	34° - 112° - 112° - 2° - 112° - 2° - 112° - 2° -	34* 11/4* 11/2* 2* 0 0 To Total Mutti-Family	X = 2 % % % }	117. 117. 27. 37. 37. 38. 117. 38. 38. 70. 70. 117. 70. 117. 70. 117.	1. Inside no 344 1. 1. 1. 2. 1. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2.	2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 -	2 - 1 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 -	11/2" 2" 2" 2" 3" Wholesale R 3" 4" - Outside ndustriel	Whosesse Chy . Texas 112. 112. 4" - Ingological & Poli Whosesse Chy . Counide 34" 112. 70th Wholesse Chy
	Class and I	Residential	Jan 1	Multi-Femily	Total		Tigation Ac	Commercial	ommercial	7000	dustrial - I	70 100
٠		-		-				5)	

		Stage	

City of Loveland

Total Usage by Customer Class Per Tap Size / Units for Multi-Family

Water Fund - FY 2003

AM GWA	97,443 78,208 100/10	116,333 396,000 1,229,000 1,533,667 13,530,000 75,696,000	25,425 27,716 25,427 20,43	41,000 36,901 40,717 70,000 70,000	25.75 25.75 25.75 26.75	201,500 6,752,000 6,752,000 214,330 2,677,000	25 M 20 00 00 00 00 00 00 00 00 00 00 00 00	2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2000	15 00 00 00 00 00 00 00 00 00 00 00 00 00	99 99 44 99 99
Annua		-					2 146,073 8 477,381 3 1342,000 9 5213,000 1 1313,303			2040s x 2000s-1; c c c c c c c c c c c c c c c c c c c	13,400 12,000 17,000 13,11; 09 13,84,500 14,500
8		11 3,515 33 7,333 00 47,000 00 127,333 00 1,055,000 00 2,501,000		752 750		. W	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			2,44,000 2,44,000 01,000 01,000	000,1 000,8
Nov		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2			182,7 26,736 26,736 26,736 26,736 30,		10,457 10,457 10,457 111,657			2000/2012 2000/2012 2000/2012 2000/2012	2,000 12,600 13,600 135,000
att Family Oct		2008 7367 00 73600 107,000 7 127,000 1,180,000		2,000		417,00 130,003 130,003 130,003 130,003 140,003	16.213 46.044 24.646 13.744 18.2500 18.2500			000,15 000,171,£ 000,171,£ 000,17	2,400 11,200 17,200 102,577 471,000 2,600 100,000
Unit for Mit		11,900 4,000 141,500 1,181,607 1,181,607 1,181,607		2012 2012 2014 2014 2015 2015 2015 2015 2015 2015 2015 2015		28,429 00,000 1,000,000 1,000,000 1,000,000 1,000,000	19,517 60,584 108,108 200,695 668,400 161,867			25.790 266,000 267,900 27,747,1	7,500 17,100 19,400 190,400 100,000
Avverage Usage by Month by Tap Size or Per Unit for Blutti-F. pr May Jun Jul Aug Sop		11,460 11,607 70,000 24,500 124,200 2,607,000		4,012 2,736 3,526 8,236 5,434 7,812	20,72 74,72 74,72 74,72 74,73	982.88 2000.09 305.70 300.09 300.07 3	21,419 61,766 106,569 223,442 778,390 148,333	26,000 64,550 174,000 221,560 260,300 1,610,000	21,200 21,000 21,000 20,000 20,000	2000 2000 2000 2000 2000 2000 2000 200	4,800 17,800 34,000 34,000 1,000 1,000 1,000
Dy Tap Si	70000	13,486 29,000 13,000 94,000 124,333 1,400,000 2,312,700		907 A 2 A 3 A 3 A 3 A 3 A 3 A 3 A 3 A 3 A 3	27.272 21.25.05 21.25.05 20.25.00 20.25.00 20.25.00 20.25.00	55,425 578,625 578,625 500,536 500,336 500,336	13,86.21 18,523 18,721 18,721 18,030	25,22 25,22 25,24 25,25 26,25 26,25 26,25 26,25 26,25 26,25 27	25,250 25,500 25,000 25,000 25,000 25,000 25,000	000,71 000,74 000,272	2,600 17,600 17,600 18,5,007 1,000 1,000 1,000
by Month		61818 788.E1 000,06 789,291 000,205.E1 000,205.E1		4 4 4 4 6 3 3	284.7 284.7 704.00 004.00 00	885,86 201,951 200,889 200,891,1 793,05 793,15 793,15 793,15	13,853 48,077 70,346 186,360 116,360 46,000	17,039 4,111 66,633 106,639 502,600	16,587 21,160 246,000 48,500 10,000	000.00.E	3,000 13,700 10,700 10,000 10,
ago Usaga May		6,568 6,667 24,000 81,000 11,000 26,000 1,811,940	86. 500. 500. 500.	2012	8,514 86,000 86,254 7,660 10,750 10,000	151,1 100VC4 151,81 100,001 10	678.8 60,386 69,00 65,17 69,101 600,000	10,012 21,880 38,056 78,350 52,150 68,000	200,21 200,71 200,000 200,000 200,000	100004 100019-C3	3,000 1,400 1,400 1,400 1,000
Apr		1,754 6,330 71,000 108,007 108,007 1,790,006	2554 2554 2555 2555	2,659 2,760 2,760 2,964 2,912 3,463	86 17.0 86.0 81.00	9001	2007, 2007, 2008,	6.518 12,522 16,100 46,000 46,000	57.1.1 000,48 000,00 000,00 000,01	10000 10000 177,000	2.450 5.500
Mar		124,667 124,667 124,667 124,667 124,667 124,667	2,26	2000 2000 2000 2000 2000 2000 2000 200	* 8 ¥		8,005 31,000 57,846 01,940 26,883	25. 24. 25. 25. 25. 25. 25. 25. 25. 25. 25. 25	28,133 28,133 378,000 31,000 10,000	2,011,000	2,200 7,200 7,200 1,200
8	4,422 6,104 804/101	708,8 200,72 20,000 20,101 20,000 20,	2681	932 933 93	超器 路		A.135 M.145	5,852 18,500 18,	000,122 000,122 000,000 000,000	1367,000 14,000	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
e e	4,000 190,000 100,000	\$,882 7,883 28,000 125,000 888,000 2,814,670	36 37	2000 1000 1000 1000 1000 1000 1000	ĕ . ¥	. 940 	2,440 2,100 300,000 310,000 310,000	21,215 12,200 12,200 12,500 12	20,000 20,000 20,000 20,000 20,000	40,000 1116,000 1000 1000 1000 1000 1000	001 000 000 000 000 000 000 000 000 000
Ш	48.	8 8 8 8 8 8 8	8888	88888888	888888 8	8 · 8 8 8 8 8 8 8 8	8888888	888888	888888	. 88 88 8	88888 8 lol W
Total	1,736,730,386	91,114,000 394,000 2,444,000 4,601,000 13,000,000 1,800,000 1,800,000,395	101,990 80,602 21,484 2,2791	3,463,000 11,374,000 778,000 31,772,000 31,377,000 20,674,000 304,674,000	17,404,000 50,202,000 58,007,000 59,000,000 11,200,000	2,204,000 5,287,000 6,753,000 6,753,000 2,077,000 277,588,000	75, C20,000 74, 100,000 57, 724,000 70, 100,000 70, 100,000 7, 100,000 7, 100,000 8, 770,000	16,174,0 11,747,0 11,296,0 36,092,0 12,175,0	11 (74,2 4,021,2 4,020,2 4,000,1 4,74,907,4	275,000 36,162,000 1,430,000 25,774,000 36,341,000	1216.000 1216.000 8800.000 16,741.000 7,060.000 31.000 86,106,000
8	\$14,000	3,077,889 22,000 47,000 382,000 1,056,000 2,501,000	4,44,000 4,215,000 1,456,000 207,000	28,000 773,000 84,000 2,557,000 2,561,000 1,561,000 1,561,000 1,561,000	274,000 14,000 16,000 110,000 		4,623,200 4,946,000 3,477,000 475,000 500,000	47,000 40,000 318,000 56,200 56,200 16,200	24.00 34.00 34.00 34.00 36.00 36.00	2,44,000 31,000 	200 A 200 M
Nov	1,020,000	18,000 18,000 188,000 188,000 1010,980	6,829,000 4,250,000 1,464,900 227,000	214,000 811,000 62,100 2270,000 2,244,000 2,244,000 2,244,000 2,240,000 2,240,000	610,000 1,816,000 3,294,000 2,116,000 1,686,000 2,000	2512000	5.411,400 5.223,000 4.171,000 4.250,000 5.425,000 673,000 673,000			13,000 20,000 20,000 2,000 2,000	100 100
H	1,947,000	2,000 2,000 28,000 31,000 38,000 1,180,000 2,375,010		205,000 92,000 3,735,000 3,775,000 2,672,000 2,672,000 2,677,000		8 8 8 8 8 8				" []	88888888
-Family Oct		1			25.2 10.2 10.2 10.2 10.2 10.3 10.3 10.3 10.3 10.3 10.3 10.3 10.3	20,000 1,044,000 1116,000 1116,000 1116,000 1116,000 1116,000	7,200,000 7,100,000 6,110,000 7,100,000 7,000,000	2378, 1,581, 2,186, 4,704, 2,406, 1,580,	27.1 27.1 24.6.1	21,000 31,17,000 71,000 71,000 71,000	17,000 11,1000 1,541,000 5,000 5,000 2,718,000
inits for Mult Sep	2,672,000	24,000 24,000 43,000 283,000 1,880,000 2,624,890 24,077,438	13,057,000 7,513,000 2,467,000 231,000	304,000 1,204,000 64,000 3,727,000 4,644,000 4,679,000	4,027,000 11,187,000 14,442,000 12,648,000 7,948,000 3,000,000 11,000	2.594,000 1.244,500 1.445,500 1.25,000 1.25,000 1.25,000 1.25,000 1.25,000	10,140,000 9,027,000 7,027,000 10,361,000 6,384,000 1,390,000	2,001,000 2,007,000 6,007,000 3,446,000 3,446,000	21,231,540 354,000 210,000 218,000 60,206,300	24,000 3,648,000 387,000 1,247,000	34,000 171,000 84,000 1,740,000
Number of U	2516,000	14,407,000 28,000 197,000 197,000 1,866,000 21,677,000	15,082,800 7,732,000 3,483,000 258,000	333,000 1.157,000 7.,000 3.473,000 4.231,000 44,473,800	4,622,000 13,194,000 14,319,000 15,219,000 4,000,000 25,000	2,694,000 1,672,000 1,672,000 1,772,000 1,772,000 1,772,000 1,772,000 1,772,000	11,136,000 8,401,000 6,367,000 11,818,000 7,733,000 896,000 1,110,000	2.905.000 1.798.000 3.132.000 6.438.000 3.250.000	1,383,500 383,000 213,000 706,000 70,011,600	2,000 4,000,000 713,000 1,004,000 6,346,000	34,000 34,000 17
by Month by Tap Size or Number of Units for Multi-	247,830,408	12,447,000 12,000 13,000 13,000 14,00	11,440,200 5,870,000 2,207,000 175,000	344,000 673,000 54,000 3,427,000 3,427,000 2,520,000 34,183,000	3,013,000 9,014,000 10,673,000 11,534,000 2,085,000	1,41,000 1,62,000 940,000 187,000 41,186,000	7,204,000 8,000,000 8,189,000 8,189,000 4,647,100 606,000 990,000	1,488,000 1,577,000 1,772,000 3,468,000 1,465,000	1,161,770 342,000 254,000 101,000 10,000 10,000 10,000 10,000	17,000 3,046,000 277,000	13,000 174,000 174,000 2,296,000 1,386,000 3,864,000
by Month by	8.472,88E	41,000 41,000 30,000 27,000 1,205,000 2,714,300	0.00,000 0.00,000 0.00,000 0.00,000	262,000 26,000 26,000 2,000,000 2,010,000 2,010,000 2,010,000 2,010,000	1,000 1,000	903.000 908.000 1,140,000 141,000 141,000	7,184,400 0,008,000 8,195,000 696,000 900,000	444,000 1181,000 107,000 274,100 045,000	757,641	000,000	14,000 117,000 117,000 740,000 2,781,000
Otal Usage	-	24,000 24,000 24,000 162,000 233,000 1,461,340 1,511,629		24,000 918 000 2010,000 2346,000 1,440,000 1,344,000						88 . 8	ă ă
leasured	*	=					42,000,000 4,000,000 4,000,000 4,77,000 600,007 600,007		"	16,000 2,746,000 	15,000 84,000 91,000 91,000 64,000 115,4000
Apr	78,866,419	13,000 13,000 16,000 16,000 204,000 1,770,000 87,255,479	8,037,000 3,758,000 1,208,000 158,000	213,000 764,000 86,000 1,967,000 2,196,000 1,541,000 1,316,000	90,000 340,000 271,000	900'6	4,000,000 4,000,000 3,194,000 3,194,000 4,019,000 60,000	00,144 000,041 000,001,1 000,001 000,001	811,880 302,000 184,000 66,000 10,405,590	2,191,000	12,000 24,000 44,000
Mar	76,472,261	4,544,000 15,000 20,000 175,000 274,000 885,000 14,	6,316,000 3,266,000 1,227,000 139,000	204000 87,000 2,04,000 1,75,400 1,155,000	867	8 . 8	4,171,000 4,917,300 3,746,000 3,245,000 2,146,000 670,000	27,000 271,000 271,000 1,000,000 1,000,000 1,000,000 1,000,000	722,010 422,000 378,000 62,000 10,000 10,000	22,000	5,000 30,007 30,000
8	470,000	16,000 17,000 27,000 20,000 800,000 800,000	00,74,000 1,367,800 1,00,000	37,000 81,000 82,000 221,100 221,100 1,68,000 1,68,000	86.00 86.00		4,485,000 4,480,700 3,716,000 3,317,400 816,000 910,000	486,000 200,000 224,000 714,800 120,000	250,000 257,000 10,000 10,000	30,000	7,000 28,000 28,000 696,000 7,000 786,000
H	2000	2,448,000 22,000 210,000 387,000 387,000 2,614,670 7,443,185		2,000 2,000 2,000 2,000 2,000 2,000 2,000	34 % 4 1 4 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	8 . 8	439,000 431,000 431,44,000 13,44,000 13,000,700 460,000 620,000 620,000		11		570 000 570 000 570 000 570 000 570 000 570 000
23	ar.	8	ត្ត	8 8 8 8 8 8 8 8			3233348	3 8 6 5 3 5	25 8 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	40,200 2,150,000 4,000 2,007,000	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
Year End Sunts - Uni	1	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	alen alen alen	3 5 8 5 8 5 9 5 9 5 9 5 9 5 9 5 9 5 9 5 9		8	% å a a a a a	8 2 2 8 2 4	5 - 4 - 5		* * * * * * * * * * * * * * * * * * *
8	:					11		Ŷ	. 11	11	Ш
200	Comp		A			outside so WOC	Ath WGC	(No Serve	3	1 1	a Page
f Meter Siz	34 1. Outside	# # # # # # # # # # # # # # # # # # #	19 2-6 Un. 3/4" 1 1/2 1 1/2 1 1/2 1 1/2	24 112 27 27 27 27 47 47 47 47 47 47 47 47 47 47 47 47 47	25 - 27 - 26 - 26 - 26 - 26 - 26 - 26 - 26	11/2" 2" 3" 4" Intigation Accounts - Outside 304" 7-Out intigation Commercial - Inside no WIOC	34. 112. 2. 3. 6. 6. 1. Imalde	34. 1.12. 3. 3. 1. Outside	34°	Wholeselving 4*-Outsi	11.27 11.27 11.27 11.27 11.27 Innotessale
Cleas and	Resident	ğ	Mutt-Fem	20 T	Photessic	rigation J Total	ommercia	ommercia	Total	Total	Polesses
_			_		-	- 0	0	0			,

		· **	

City of Loveland Total Usage by Customer Class Per Tap Size / Units for Multi-Family Water Fund - FY 2002

[al Avg.	314,636 252,747 80N/0	113.744 160.667 723.000 723.000 12.04,000 13.674,000	78,008	60,252 34,850 44,877 50,008 57,204 72,001	214,639 200,224 274,880 111,668 106,390	28,000 28,4167 686,770 426,000 40,000 48,000	12.215 208.127 1.008.56 5.208.170 6.208.170 0.00.000	19,274 91,731 90,230 91,835 51,835	77,546 61,387 71,000 71,000	000,000,000,000,000,000,000,000,000,00	27,986 101,400 864,000 3,000,147 3,000,000 86,000 80,000
	ec Annu		14,667 14,667 28,000 127,000 127,000 131,000 14,000		4,157 3,200 3,200 3,200 3,700 3,700	* .83 		22 24 25 25 25 25 25 25 25 25 25 25 25 25 25			2 1000 12 100 12 100 12 100 12 100 12 100 12 100 12 100 12 10 10 10 10 10 10 10 10 10 10 10 10 10	2,200 2,200 2,200 3,000 3,000 3,000 4,000 4,000
	Q AO		1,520 2,000 2,000 3,000		4.181 9.224 9.226 9.226 4.667	4,886 15,403 68,720 36,000 36,500 467,500		2 247.4 22 247.7 23 247.7 24 24.0 26 010.0 26 000.0 26 0000.0 26 000.0 26 000.0 26 000.0 26 000.0 26 000.0 26 000.0 26 0			14,000 21. 14,000 21. 14,000 22.77	1,000 8,300 2,000 2,000 185,600 2,000 4,000 100,000
	ш		8,216 8,000 141,000 108,667 108,600 108,700		100 00 00 00 00 00 00 00 00 00 00 00 00		2300 57,429 69400 604,730 604,000 21,000 24,000	4,477 4,477 7 6,460 7 114,646 7 100,000 14,0		•	A100002 A100002 A100002 A10000 A10000	2,000 19,200 10,200 10,200 2,000 10,2
	Sep		11,000 12,000 12,000 12,000 12,000 13,000 10		30 30 21 21 22 22		2000 2011-6 200375 200375 20000 20000 724,000	20,254 20,724 210,742 210,917 111 20,000 20,000 20,000			2 000,00 2 000,00 2 000,00 2 000,00 2 000,00	1,400 11,600 11,600 13,400 13,400 10,000 10,
	Aug Aug		17,277 27,200 11,200 14,233 1,612,000 1,4133 1,512,000 1	70,068 7,421 8,600 2,7,6	2 4 4 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	•	6.807 16.786 a 16.786 a 174,000 a 178,000 7	7,12,206 7,1			1 100000 117 000000 117 00000000 117 000000000	12,200 12,200 130,000
	Jul		16,684 20,000 10,200 1,136,000 1,136,000	10,200 1,212 1,712 1,712	200 200 200 200 200 200 200 200 200 200		200 200 200 200 200 200 200 200 200 200	16,485 62,485 168,230 168,230 26,230 12,500 20,000 20,000			000,000 000,000 000,000 000,000 000,000	2000 X 7 7000 X 7 7 7 7
	ы		12,800 30,000 112,800 191,200 1,455,000 1,718,110 2,718,110	80 5 80 5 80 5 80 5 80 5 80 5 80 5 80 5	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		2000 16,714 46,875 506,800 506,800 506,800	16,105 56,882 80,873 80,874 40,270 40,230 40,230 40,230 40,230			260000 260000 260000 270000 270000 270000	3,000 12,000 30,600 106,533 200,000 8
	May	11,468 28,585 80WOR	4,000 1,000	6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	200 200 200 200 200 200 200 200 200 200		25,000 25,128 25,000 25,000 25,000 25,000 25,000 25,000	44,892 91,111 123,003 000,000 000,000			0.00 M M M M M M M M M M M M M M M M M M	2,000 7,000 81,947 1,000
	Apr	6,455 10,165 80WDI	2000 2000 2000 2000 2000 2000 2000 200	2 2 2 2	3,450 3,450 3,400 3,400 3,600	4.20 12.20 12.20 14.70		9,000 23,481 67,573 73,042 218,200 107,500			2,000,000 2,000,000 2,000,000	2000 2000 2000 2000 70,000 2000 2000 200
	Mar	4,514 5,200 FOWOR	A 3 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	2,50,00	2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	* N . N	· · · · · · · · · · · · · · · · · · ·	A684 34,538 68,532 71,560 206,302 330,000 330,000	6.163 13,846 17,412 60,700 37,902 70,000	2 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	2000 2000 2000 2000 2000 2000 2000 200	881. 884. 785.
	11		04.2 04.2 04.00 04	2348	1000 1700	n.88	· · · · · · · · · · · · · · · · · · ·	68.75 66.73 68.75 19.440 108.83 108.8	6,522 18,736 18,736 19,500 17,900 77,900 77,900	25,25 7,88,25 500,05 10,000 10,000	2000 2000 2000 2000 2000 2000 2000 200	88.1 88.2 72.3 8
	de	27.2 27.70 20.00	C.C.C. C.C. C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C.C.C. C. C. C. C. C. C. C. C	2 8 3 3	2,000 100.0	4 M 8 2	eng d	26,785 26,785 26,785 26,785 26,000 26,000 26,000	25 11 12 15 15 15 15 15 15 15 15 15 15 15 15 15	26,000 313,000 28,500 10,000	16,000 16,000 1,656,000	000 0000 . 80 000 con
Γ	3	13,367,000	482.00 723,000 2412.000 5,274.000 11,676,000	674,000 (622,000 (948,100	4,17,000 777,000 777,000 21,001,000 36,344,000 38,440,000	4,254,500 4,254,530 4,127,000 6,103,400 6,732,000	2,41,000 2,41,000 4,66,000 2,67,000 2,67,000	00,000,000,000,000,000,000,000,000,000	84.100 84.000 86.000 25.900	75,000 75,000 75,000 75,000 75,000 75,000	273,000 22,607,000 6,613,000 134,000	131,000 131,400 278,000 1347,200 181,000 181,000
	Ц	-	*									- 11
	Ц		5,094,500 44,000 215,000 348,000 34,000 1,994,000 80,701,642		345,000 394,000 67,000 2,182,000 2,335,000 2,007,000 77,500,100	2, 25, 28, 38, 38, 38, 38, 38, 38, 38, 38, 38, 3	000/00	4,682,000 4,584,000 3,451,300 86,000 880,000	200,092 200,072 200,621,7 200,631	20,000 30,000 30,000 30,000 30,000 30,000	21,000 227,000	28,000 28
	Nov	91,706,022 602,000	4,986,500 26,000 122,000 362,000 1,249,000 1,00,176,522	7,222,000 4,694,000 1,206,000 1,64,000	247,000 861,000 2464,000 2,004,000 2,004,000 2,004,000 2,004,000 2,004,000 2,004,000	000,000 000,000 000,000 000,000 000,000 000,000	. 00.11 00.00 00	5,482,000 4,488,000 4,791,000 4,006,100 782,000	986,000 809,000 1,166,900 2,009,000 887,300 160,000	754,000 328,000 251,000 57,000 19,000 30,417,600	2,461,000	82,000 82,000 82,000 17,000 80,175
4	904	1,546,316	7,641,100 24,000 141,000 187,000 286,000 15,877,010 15,272,010	8,544,000 5,456,000 1,466,000 241,000	401,000 1,094,000 00,000 3,274,000 2,442,000 2,462,000 25,600,000	2314,000 4,396,000 8,143,000 6,000,000 3,283,000 1,290,000	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	7.214.000 6.216.000 6.447,000 6.4590,000 6.2381,000 8.4290,000	1,347,000 1,347,000 1,440,000 1,777,000	000,232 000,230 000,031 000,031 000,031 000,040,040	27,000 3,184,000 122,000 1.20,000	12,000 12,000 12,000 12,000 720,000 11,000
tor Multi-Par	Sep	2,863,000	12,092,500 53,000 154,000 241,000 1,793,000 2513,500	2,201,000 1,331,000 2,301,000	411,000 1,364,000 8,167,000 3,913,000 4,210,000 4,210,000	2,151,000 7,754,000 7,771,000 10,296,000 2,412,000 18,000	1,401,000 034,000 134,000 724,000	8244.600 8244.600 6.785.000 16.784.000 1.200,000	2,500,000 2,200,000 1,275,000 6,120,000 1,962,100 1,486,000	1,278,400 347,000 287,000 115,000 70,000	34,000 4,117,000 844,000	17,000 134,000 614,000 2,004,000 1,600,000 41,004,000
mber of Units	Aug	3,62,600	72,000 72,000 91,000 275,000 431,000 1,512,000 2,542,000 10,716,600		47,000 7,000 7,000 7,000 4,190,00 4,190,00 3,810,000	3,619,000 7,911,500 8,105,000 10,982,000 4,142,000 566,000		\$,600,000 \$242,879 \$260,000 \$7,200,000 \$4,000 \$4,000			34,000	21,000 122,000 144,000 2,004,000 4,000,000 4,000,000
Size or Num	11	•	47,000 47,000 47,000 47,000 47,000 1,85,000 3,134,600		20,000 (2,000 (2,000 (4,00) (4,00) (4	3,190,000 6,602,000 7,006,000 11,006,000 2,906,000	- 11			ľ		
nth by Tao	jay u	•	*					4.157,800 6.158,400 6.158,400 9.662,100 786,000		П	21,000	21,000 114,000 11,400,000 1,100,000 4,000
Mace by No	ş		11,861,000 11,000 10,000 225,000 124,000 12,425,000 12,718,114 1811,812,1145	13,100,00 7,386,4 2,088,00 56,00	34,000 1,234,000 31,900 3,194,900 3,467,000 3,7740,300	2,864,000 6,880,000 6,004,000 8,506,400 1,706,000 4,000	000,071.00 000,002 000,002 000,007.00	4,16,000 4,122,400 6,226,000 1,546,000 4,562,700 686,000 970,000	2313,000 1,681,000 1,622,000 1,672,000 100,000	24,000 24,000 24,000 26	2,820,000	15,000 15,000 1,598,000 390,000
U Made Total U	May	2250,000	10,250,480 4,000 20,000 10,000	11,046,000 8,861,700 1,701,000 40,000	336,000 1,000,000 56,000 1,427,000 2,360,000 1,476,000 20,613,700	2,306,000 5,952,000 6,497,000 4,568,000 296,000	251,000 251,000 251,000 251,000 251,000 251,000 251,000	5,204,000 6,471,880 5,742,000 5,842,000 786,000 800,000	001,182,1 000,002,1 1,205,000 1,201,000 1,001,000 1,001,000 1,001,000	1,944,000 307,000 231,000 140,000 14,964,000	2540,000	13,000 24,000 24,000 121,000 1,000 1,000 1,000
Money	ě.	803,000	22,000 22,000 22,000 23,000 23,000,000 23,000,000 10,247,246,000	766,000	201,000 94,000 91,004,000 2,472,000 1,306,000 1,346,000		34,000 34,000 36,000 3,000 3,000	436,000 486,133 4274,00 5,04,00 75,00 75,00 75,00	966,000 96,000 96,000 15,000	10,200 11,000 11,000 10,200 10,200	22,000 2343,000 92,000	25,000 1,000 1,000 1,000 1,000
		-	19,000 19,000 19,000 19,000 11		12 000 MEN. 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	200 . 00				"		- 11
	Mar		1°1					4,421,00 4,97,40 4,94,00 2,001,00 60,00 60,00 60,00		*	14,000	2,000 2,000 14,000 17,4,000 2,000
	Pet de		\$1000 \$4,000 \$16,000 \$16,000 \$77,000 \$1,000		87,000 87,000 61,000 1,291,000 2,734,800 1,842,000 20,844,000		200	4,500,000 4,813,000 4,141,000 3,478,111 1,944,100 660,000	200,000 200,000 200,000 200,000 200,000 200,000	188,000 000,000 000,000 100,00	1,566,000	000.00 000.00 000.00 000.00 000.00 000.00
	raf	631,000	13,000 13,000 17,000 40,000 1,000,000 1,000,000 1,000,000 1,77,702,001	7,644,500 4,742,000 859,000 94,000	301,000 1,006,000 1,206,000 2,167,000 1,816,000 1,616,000 21,425,500	200 200 200 200 200 200 200 200 200 200	(3.5)	4,732,000 8,237,000 4,438,000 3,168,000 886,000 898,000	214,000 214,000 1,411,000 367,700 116,000	36,000 31,000 37,000 10,000 14,676,013	1,854,000	0000 1 00000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 00000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 00000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 00000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 00000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000 1 0000
ear End	Counts	8 K .	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Units Cook See as	288888	8884		31345	* # # # # # #	2 7 - 11 - 510,		*** * * * * * * * * * * * * * * * * *
-	Y. Gu		11	¥.	;	!	11		6			11
	(Apr	(Apo	3	a	1	. §	Outside o	ARP WOC	(No Sewer	3 1		10 e 60
	d Meter Sta lei (Inside C	24 1- 2 2 (Outside	8 - 5 r r r r r r r r r r r r r r r r r r	11/2 24 Uni	200 1 12 12 12 12 12 12 12 12 12 12 12 12 1	24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 1.2. 24. 24. 24. 24. 24. 24. 24. 24. 24.	1.177 7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.	* - 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	112 112 3 4	1 12 1 12 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11/2" 2" 3" 3" antrial - Wholeasie Rei 4" - Outside Total Industrial	34. 11/2. 2. 11/2. 24. 34. 11/2. 11/2.
	41.00	덛	8,	5 5	9 (:		- 4	- 4			

City of Loveland

Total Usage by Customer Class Per Tap Size / Units for Multi-Family

Water Fund - FY 2001

	Dec An	11,7617 5525 117,617 50 112,725 110,7 50 100,000 100,000 100	200	38,000	m m	2,116,610		480	11 3,389 74,919	45	1600	376	3775	97		818	g .	203					NOWIGH	. 73,000			927.01	K.E7	319,644	125,000	\$ 160	16,067	77,960	7,000	916,01	227,000	34,000 772,500		MANAGE	3,307,000	000,100,1 000,018 000,100,15 000,018		3,200	000,811 000,11 000,000 000,000	4700	2,000	IDMIDI
	_	802.13 014 803.11.208 NVI 60NVI							2003															000,71 00													20,000				0 1,118,000			3,00			
Mutti-Family		015.11 667. 528.15 668. 10V/Os 90V/Os			•				14,765 8,120															49,500													002,28			**	3,524,000			000715			
er Unit for		17,757 15,726 21,645 41,535 40,004 40,004							10,891															112,500													2000			•••	136,000			22,600			
p Size or P		19.740 10.274 10.004							877.6															158,000 141,500													900 88,000		_		000 SEL000			22,600			
lonth by Ta		13,00 10,00 10,000							8 4															521 000,021													30,000 \$0,000				000,772 000,4 000,020,000,000,000,000,000,000,000,000			56,400 20,000			
Usage by a		7,638 14,634 FDWR							35													. · ·	30	22,500													26,500 111			••	000,1			5,200			
Average		ELD STATE				-		4,600	9 5 5		7.36	3,228	3272	Ç										8,000													40,000			**	. 000,700			9 9 9			
	_	4,681 5,434 8DWG				**		4,468	3 5		72	8 2	3,185	4:30																							30,000				. 000'000			0 00 0			
	2	4,500 8,400 60Mp	7,300	77,000	138,000	1.813.850		4.33	1 60	3	1	330	2 2	4130		176	. 2	ă.		٠	·		spings														30,000				00000			8 8 5			
	ş	4,975 7,133 6DVVG	3,604	123,000 81,300	225,000	2,256,720		2007	2 2 2		3,000	3,370	3,560	4357		22	2 23	3 .			·		OWO				2000	20,400	20700	175,167	197	17,630	68.680	67,500	222.01	372,000	30,000				1,000		991	800		1000	POWE
	Total	1,814,340,347	304,000	2,106,000	6,322,000	2,010,744 NR7		128,737,000	16,806,865		13,602,000	19,813,000	26,733,500	25 820 000		20,022,900	22,117,000	21,240,500	15,205,000	136,000	3,449,200	7.915.000		1,426,000	201,298,100		78,738,387	66,250,120	41,028,040	12,000,000	18,427,120	13.678,000	41,570,000	16,126,000	11,518,770	3,042,000	340,000	NICH ST	280,000	34:37,000	21,961,000	Pr. rankov	360,100	1,164,000	3,236,000	17,000	. Other us
	š	84,702,198	16,000	36,000	310,000	2,116,610 94,658,808		7,061,000	702,465		1,021,000	1,336,000	1,964,000	72,139,465		000'89	2000	126,000		٠				٠.	227,000		6,321,680	3,869,620	2,876,800	300,000	000'629	200,000	1,569,000	150,000	639,240	227,000	10,000		19,000	3,307,000	3,000	S. January	16,000	30,000	. 687.00	2,000	200 750
	MON	10,629,230	20002	30,000	900,000	1,988,686		7,914,986	801,700		000,720,1	2,086,000	2,151,000	3,997,796		96,300	54,300	25-49,000	759,000	2,000	37,100	125,000		00 % 00 90 00 90	136,100		147,000	000'197	261,300	900,000	336,000	532,000	000,400	319,000	736,760	198,800	20,000		19,000	000'125	2,110,000	AL PACE	14.100	27,200	410,000	1,000	8
	1	2,41,000	21,000	176,000	310,000	574,476			1,827,100					П			2,899,000							26,000	П												10,000	1				1		216,000			
ulti-Family	1		3,225,000 33,000			٦																			П												ľ	1									
Units for I		3,157,000				2			3,322,040								5,682,000							228,000	П		7,997	8,019	5,571.	1,380,	3.145	2,374,	5.341	1,965,	24.	3 %	2000		ä	3573,000	4 600,000			113,000			1
Number of		3,317,000	15,319,200	90,871	0,057,	313,677,38		17,686,30	2,473,000	204.00	1,646,00	2,274,00	3,481,000	3,880,000		4,119,000	4,363,000	5,905,000	3,815,000	7,000	901 000	3,195,000		283,000	48,157,000		7,945,100	8,025,000	4,538,640	1,280,800	3,274,000	2,736,000	7,448,000	4,145,000	1,610,360	218,000	0000		30,000	3,719,000	3.616,000		2000	126,000	1,972,000	1,000	
Tap Size o		321,296,100	16,958,800	217,000	2,085,000	3,814,880		18,940,000	27,000	370,000	1,384,000	2,002,000	3,886,000	3,680,000		4,063,000	5,402,000	3,611,000	3,320,000	12,000	613,000	3,142,000		318,000	41,548,000		8,786,300	7,461,000	4,087,900	1,480,000	2,882,120	3,434,000	4,616,000	4,415,000	1,379,860	274,000	20000		27,000	3,564,000	3,986,000		000,00	131,000	2,110,000	3,000	5 540 000
ge by Month by Tap Size or Number of Units for Hulli-F		2313,000	11,748,000	000,171	000'000	316,340		500,000	1,784,000	256,000	261,000	528,000	800,000	90,000		000914	3,004,000	46,000	990,000	11,000	246,000	919,000		386,000	900.000												30,000	1	23,000		4,000			275,000			2000
Mail Usage b	1		7,122,880 11			ľ			1,075,200 1,					П								507,000			П												ľ					l					27
7 panseng 7	1.					"								11			1,130,000							65,000	П		5,639	5,048	20.00	1.260	4	8 8 8	8 8	380	980	187.	40,000				1,000		32.0	342,000	1 2		2,378.0
ě		24,16,000 48,000	31,000	00,831	740,00	\$4,034,08		7,363,00	722,800	328.00	0,00	1,004,00	1,796.00	20,226,30		277,000	8 8	200	Ö		1,000	367,000		16,000	1,618.000		4,625,000	4.224,000	3.078,900	1,280,000	608,000	471,000	1,574,000	130,000	675,720	200,000	40,000		2000	2,497,000	3217,000		12,000	90,000		•	900,100
in in	*	416,000	4,943,000	158,000	660,000	1,992,150		4,330,000	633,000	25,00	80,000	1,639,000	1,744,000	19,436,000		1,000	2007			٠					\$0,000		4,504,865	3,867,000	2,836,000	1,000,000	467,000	368,800	1,249,000	150,000	598,640	374,000	30,000		21,000	1,950,000	2,571,000		12,000	20,000			863,000
2	1	411,000	4,788,000	154,000	414,000	1,870,867		4.188,000	12,000	364,000	932,000	1,046,000	1,751,000	9743,889		13,000	000,1								49 000		310,000	472,000	364,900	120,000	463,000	300,000	419,200	130,000	698,360	270,000	20,000		21,000	394,000	8,000 646,000 2,668,000		1,000	32,000			900,000
	1		36,000			П			000,000							13,000	2,000								\$1,000												30,000				1,000 \$24,000 2,138,000 2,			20,000		1,000	0000
Par sier	1 2 2 2		g ~ .		n -	2 3427		7, 668 7,	8 -				1	П		2 3	= 1	. ~		. ,		• -			160		* *	8 2	6 9				8:	~	8 2		1 282		٠.		4		• 9		~		25
Year E	Y.E. Coun	53					Y.E. Unite								Y.E. Coun																																
Class and Meter Size	Residential (Inside City)	1: 22 Pesidential (Outside City)	¥:- 5	141	h & 1	Total Realdential	Multi-Femily 2-8 Units	34.	21.2	Multi-Family 9+ Units 3/4*	1 14	112	ı h te	Total Multi-Family	Irrigation Accounts - Inside	i g =-	112	, b :	Wholesale City - Irrigation	36:	1 1/2-	h b	Impation Accounts - Outside	1.12	Total Irrigation	Commercial - Inside no WQC	5	22.22	h v	Commoncial - insists with WOC	34.	11/2	6 P	Commercial - Outside (No Sever)	 36	21.1	Total Commercial	Industrial - Industrial Rate	2,2	Tr. Industrial - Wholesale Rate	3° 4° - Outside Total Industrial	Wholesale City - Inside	3/4	27.72	4" - Infgation & Pool Wholesale City - Outside	34.	Total Wholesale City

City of Loveland Billed Sewer Flow Analysis by Customer Class by Year Fiscal Years 2000 Through 2006

			2008				2005				2002				2003	
Class	WOA.	Counter	Billed Flow/mo.	Billed Howlyr.	WOA.	Counts	Billed Flow/mo.	Billed Flowing.	WOA*	Counter	Billed Flow/mo.	Billed Flowlys.	WOA.	Counts**	Billed Flow/mo.	Billed Flow/rr.
Residential	4,423	19,314	85,424,941	1,025,089,289	4,189	19,231	80,560,959	966,731,506	4,331	18,508	80,154,658	961,855,894	4 582	17,818	81,821,685	ł
Multi-Family	3,378	6,313	21,327,800	255,933,600	3,357	6,303		253,941,668	3,473	5,923	20,573,384	246,880,608	3,548	5,758	21,003,624	
Commercial	33,736	88	33,702,598	404,431,174	30,731	8		386,564,940	29,066	820	27,874,182	334,490,184	22,82	371	32,862,533	
Industrial	404,375	4	1,617,500	19,410,000	395,208	4	1,580,833	18,970,000	438,042	4	1,752,167	21,026,000	22,817		22.917	275,000
Government - City	52,063	ĸ	1,666,019	19,982,233	50,598	8	1,720,320	20,643,840	53.587	8	1,768,369	21 220,432	55,354	8	1,790,521	
Totals	497,975	26,662	143,738,858	1,724,866,296	484,083	26.566	135,570,995	1,625,851,944	528.439	25.427	132,750	1,585,473,118	120.955	24.580	137.501.279	V

			2002				2001				2002	
Ciass	WOA:	Я	Billed Flow/mo.	ã	WGA.	Counts	Billed Flow/mo.		WQA*	Counter	Blied Flow/mo.	Billed Flow/yr.
Residential	4,878	16,898	82,433,455	l	4,778	16,231	77,788,969		1		80.981.045	971,772,538
Muti-Family	8 8		20,833,171		3,855	5,164	19,909,180			4.984	19,598,072	235,176,862
Commercial	34,042	848	32,169,361		35,382	913	32,121,032				34 182 324	410.187.883
industrial	22,750	-	22,750		28,33	•	23,333				27,250	327,000
Sovernment - City	53,880	31	1,670,282	20,043,388	86,558	31	2,063,283	24,759,396	81,470	8	2,444,104	29,329,252
Totals	119,172	23,627	137,129,019	٣.	133,706	22,390	131,905,798		1	21,533	137,232,795	1,646,793,535

		2	Year Average	
Cises	WOA	Counter	Billed Flow/mo.	Billed Flow/yr.
Residential	4,626	17,664	81,309,387	975,712,650
Multi-Parnity	3,609	5,742	20,629,577	247,554,919
Commercial	33,411	128	31,922,730	383,072,755
Industrial	190,554	N	720,964	8,651,571
Government - City	59,159	×	5,874,700	22,496,398
Totals	291,358	24,398	136,457,358	1.637.488.294

		Š	Test Year 2003	
Class	WGA	Counts	Billed Flow/mo.	Billed Flowlys.
Residential	4,626	20,245	93,653,370	1,123,840,440
Multi-Family	3,609	6,503	23,471,185	281,654,220
Commercial	33,41	1,053	35,181,783	422, 181,396
industrial	190,554	4	762,214	9,146,571
Government - City	59,159	8	1,853.074	22,716,891
Totals	291,358	27,837	154,961,627	1,859,539,519

For classes not billed by winnsr quarter average, the annual usage for the class was divided by tweive.
 Count for Multi-Family class includes number of units, not number of taps.

:

City of Loveland Sewer Consumption Summary Fiscal Years 2000 - 2006

			Year End	Tap/Units	or Multi-F	amily Coun	ts by Year			- 1	See Headers	Below for De	talls		Ī			Son Head	Palou for Da	faile		
1	Class and Meter Size	2000	2001	2002	2003	2004	2005	2006	2000	П	2002	2003	2004	2005	2006	2000	Γ	2002	2003	2004	2006	2006
10 10 10 10 10 10 10 10	Residential (Inside City)			18				ľ		ŝ	lallons per Custo	nor per Class po	r Month by Year		l		į	tuarter Average p	rr Month by Custon	ner Class by Your		
The column		15,527	16,206	16,825	17,745		19,153	19,240	5,184	4,773	4,869	4,585	4,326	4,167	4,420	80,488,106		81,926,455	1,365,047	79,740,946	80,189,835	85,004,889
The column	1.10		2 .	2	2		ξ.	7	6,661	5,778	6,945	6255	5,645	4,948	5,271	492,939		507,000	456,638	413,712	371,124	390,052
1. 1. 1. 1. 1. 1. 1. 1.	24						- 6					•									•	
The column	Total Residentlal	15,601	16,281	16,898	17,818	18,508	19,231	19,314	11,845	10,552	11,815	10,841	9.971	9.135	9,691	90,981,045	77,788,969	82,433,455	81,821,685	80.154.658	80,560,959	85.424.941
1	Modf-Femily 2-8 Inite							L														
18 18 18 18 18 18 18 18	-3/6	1 569	180	1 689				٦,	400	Winter Quarte	r Average per Cu	stomer per Class	per Month by	Tour			Winter	uarter Average po	or Month by Custon	ner Class by Year		
18 18 18 18 18 18 18 18	; =-	900	8		300	1,516	L'es	190	4,750	4,477	4,491	4,236	4,128	3,838	3,816	7,452,346	6,968,488	7,136,126	6,575,452	6,258,746	6,029,920	6,002,962
1	1 1/2	185	2 2	38	1 5	5	200	2 2	4,282	4,350	36.4	4,005	1000	3,710	3,881	4,317,409	4,423,034	4,594,096	4,123,600	4,130,022	3,970,148	4,129,006
1	N			4	3 =	*	3 5	3 2	2000	202	2,201	2,725	2,782	2,685	2,806	2 ,12	641,862	759,486	1,233,606	1,455,000	1,862,005	1,975,272
1	Multi-Family 9+ Units		•	2	•	•	?	5		ē	900	2,746	2,070	3,066	3,208		400	38,532	21,970	16,562	346,450	397,826
18 18 18 18 18 18 18 18	3/4*	3	2	2	2	2	8	8	2774	70.7	2 804			-	-	-						
The column	: -	283	28	283	300	285	285	282	3,480	2366	3.443	2000		2,000		302,200	348,140	122		312,988	241,322	253,636
The column	1 1/4"	8	8	8	8	8	20	20	2961	2484	3076	200		200	200	100,000	305,146	204,404		763,880	766,584	708.744
The column	11/2	230	311	8	98		27	92	3,800	3404	1 950	3210		2100	2,616	20,012	49,606	61,516		83,148	66,248	68,276
18 18 18 18 18 18 18 18	ŧ.	959	714	726	726		367	E	2,606	2.625	3051	3226		200	200	200,000	1,000,010	2000,000		2,184,652	2,327,468	2,350,452
The column	ě	3	3	35	3		35	3	3277	3.369	3360	3280		3.150	3.400	200,000	0000000	2219,100		200,000	2,467,400	2,037,802
Column C	**	395	385	395	395		300	302	3,791	4,355	4,035	3,851		3,427	3.704	1.497.340	1,720,420	029 055 1		1 185 800	1,730,580	1,913,418
1	Total Multi-Family	4,964	5,164	5,752	5,758	5,923	6,303	6,313	35,704	36,240	34,707	37,136	П	35,089	35,625	19,598,072	19,909,180	20,833,171	П	20,573,384	21,161,805	21,327,800
1	Commercial - Inside on WOC							L	ľ										П			
1	Commence of the commence of th	•						_	Submit	ed in Annual Gal	ons - Divided by	12 to Determine	Monthly Averag	b per Account		8	ubmitted in Annua	Gallons - Divided	by 12 to Determine	Monthly Average	for Class	Γ
1	34	\$	\$	498	484	\$	201	499	14,246	13,212	12,730	11,820	11,792	11,862	12,239	6,895,183	6,381,366	6,374,004	5.839.167	5.825.067	6.014.050	6137.077
Column C		ä	35	\$	145	140	147	148	49,813	46,174	43,682	38,906	37,028	41,844	45,137	6.575,259	6.187,333	6.115.439	5.641.317	5 183 867	6 151 117	6600 240
1	2/11	35	6	8	8	g	8	8	102,331	91,069	34,046	74,006	78,852	76,929	80,416	5,525,875	5,190,927	5,294,917	4,810,333	4,888,833	5,000,408	5227 017
1	N 6	3	4	3	8	49	5	8	123,507	113,341	107,565	114,260	97,153	114,988	118,285	5,310,817	4,647,000	4,624,867	5,713,000	4,780,500	5.864.385	7,451,973
1	2 5		0 (9	0		= '	9	383,342	385,445	443,848	442,583	226,880	196,089	249,237	3,066,733	3,469,003	4,438,475	3,963,250	2,041,917	2,178,975	2,492,306
1,	r le	9 6			۰ د		.	10	228,181	167,063	122,500	109,444	36,500	117,250	122,250	1,369,063	1,002,500	735,000	656,667	482,500	586,250	611,250
1	ommercial - Inside with WQC	,	•	•	-		,	,L	414,928	580,417	412,083	534.167	347,083	280,000	368,417	1,244,783	1,160,833	624,167	534,167	694,167	840,000	1,105,250
1	3/4	5	4	4	83	2	8	18	S. ACM	6448	6.260	S OF CHASE	e son	-	-		Winter O	Jarler Average pe	r Month by Custom	er Class by Year		1
1	:-	22	22	20	8	8	8	ន	15,623	18,315	12.675	18.421	12.774	12 104	19918	707 107	700 700	200,000	30725	531,030	57,727	523,646
1	1 1/2	13	4	11	55	10	5	8	18,282	19,385	15,449	10,543	21,410	20,335	20.559	310.960	329 550	363 636	207 TR	206,798	20,100	2
1	iv	20	9	8	8	8	2	ន	869'89	94,102	474,474	80,613	61,421	25.52	200.30	1,373,967	1282 004	1,289,470	1612.260	1 228 411	1311 660	4 477 994
1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	in 4	Ε,	= '	12	12	=	=	9	48,226	38,163	35,825	144,042	45,325	43,955	48,814	530,491	419,796	429,902	1,728,498	498,576	483,510	468 137
1, 1, 1, 1, 1,	OW or abiging - District	•	4		2	2	7	"L	71,825	70,135	66,755	58,305	67,663	57,344	42.532	143,650	140,270	133,510	116,610	135,386	114,687	127,596
1	.7/6	*	*	*	*	2	1	ָר	Submit	od in Annual Gall	ons - Divided by 1	2 to Determine	Southly Average	per Account		8	bmitted in Annual	Gallons - Divided	by 12 to Determine	Monthly Average	or Class	
	ζ÷	e g	9 0	2 5	3 2	5 5	4 .	٠,	24,128	24,360	19,474	15,024	17,630	17.204	17,930	386,019	365,396	311,583	375,608	370,233	378,485	376,523
Fig. 10 Fig.	1 1/2*	-				: -		•	291.001	200 100	21,107	2000	200	16,063	10,240	230,823	248,167	211,067	254,417	266,167	144,750	81,917
	å	-	-	-	-				55.917	32.063	27.917	31,000	24.063	100,001	2 2 2	100,107	235,167	270,063	228,300	150,063	149,667	142,583
1 1 1 1 1 1 1 1 1 1	•				•			-							20,833			1000	99%	190'47	7.87	22,730
1	ommercial - Outside with WQC							Ц		Winter Quarter	Average per Cus	tomer per Class	per Month by Ye	'n	-		Winter Or	arter Average per	Month by Custom	or Class by Year		20,000
Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted - Submitted in Armunal Galations - Divided by 13 to Determine Miscrating - Submitted - S	Total Country	-	-	-	-	-	-	-	16,900	18,590	14,196	16,900	15,541	18,115	14,040	16,900	18,590	14,196	16,900	15,541	18,115	14.040
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Total Collaboration	416	510	255	871	88	ğ	888	1,860,217	1,971,063	1,780,787	1,965,965	1,344,671	1,267,239	1,419,394	34,182,324	32,121,032	32,169,361	32,862,533	27,874,182	30,547,078	33,702,598
1 2 2 2720 2333 2270 22617 17504 14770 27200 25330 27200 273	dustrial - Industrial Rate							L	Cobmits	of in Assessed Coult	Photograph by	September 2			ŀ	ľ						
1 1 2 2 2 2 2 2 2 2	11/2					-		1			600000	and the second	Solves Average	TA SOO	-	i i	Dmitted in Annual	Gallons - Divided	by 12 to Determine	Monthly Average	or Class	
1,	8 , 3		-	-	-	8	8	~	27,250	23,333	22,750	716,22	25,625	30,833	32,875	27.250	23,333	27.750	22 917	51,250	61 667	16,750
1 1 1 1 1 1 1 1 1 1	Control of the Contro		1	1	1	-	-	-					1,680,833	1,501,667	1,536,000		٠			1,680,833	1,501,667	1.535,000
2 2 2 2 2 2 2 2 2 2			1	1		1	7	4	27,250	23,333	22,750	22,917	1,726,542	1,550,000	1,584,625	27,250	22,333	22,750	22,917	1,752,167	1,580,633	1,617,500
3 1 1 1 1 1 1 1 1 1	holesale City - Inside no WQC							L	Submitt	d in Annual Galls	xna - Divided by 1	2 to Determine 1	Sonthly Average	Dar Account	ŀ	0	benthad to Account	Callone - Obddad	by 40 to Determine			
10 10 11 12 12 13 14 15 15 15 15 15 15 15	3/4"	n	n	n	•	6	6	l"	2,639	3,725	2,303	2,778	2,250	2333	1.528	7917	11.175	4000	9 14 to Course must	A 760	7,000	1 600
1 10 10 10 10 10 10 10		49	9	9	9	=	22	=	12,089	5,627	8,450	10,133	14,336	15,103	17.242	86,708	96,267	94,500	101.333	157.700	196 300	180 667
1,000 10 10 10 10 10 10	200	* :	* ;	* :	* :	•	4	4	105,454	30,963	54,417	15,625	15,000	16,333	22.125	421,817	123,850	217,067	62,500	60,000	68,330	88,500
Col. 1607 Col.	1.4	: '		2 '	2 +	2 *	2	3	113,002	120,968	90,892	100,967	111,825	89,417	29,260	1,243,350	1,209,663	508,917	1,009,667	1,118,250	894,167	900,006
1 1 1 1 1 1 1 1 1 1	4* - Pool Flat Rate		-	-					290 100	000	291 017	200	0000							10,000		
1 1 1 1 1 1 1 1 1 1	holesale City - Inside with WQC							L		Winter Quarter	Average per Cust	comer per Class	per Houth by Ye	20000	364,10/	/90/100	Mindre Or	419,167	18	300,633	543,067	524,167
10,478 11,462 21,570 10,478 10,714 7,000 7,000 10,478 11,482 21,570 10,478 11,482 21,570 10,478 11,482 21,570 10,478 10,478 7,000 21,00	3/6	-	-	-	-	•	-	1_	4,056	3,380	3,360	3,380	2,944	2.448	2 674	4.056	3.380	3 300	[]	2044	2440	7
1 1 1 1 1 1 1 1 1 1	11/2	-		-		•			10,478	11,492	21,970	10,478	16,714	7,020	7,020	10,478	11,492	21,970		16,714	7,020	7,000
20 31 31 32 33 34 32 977,501 000.035 738,100 600,073 710,008 2,444,104 2,003,350 1,670,202 1,700,021	Polessie City - Outside with WOC	-	-	-	-	-	-	_L	8,112	7,436	7.774	5,746	5.178	4,962	5,290	8,112	7,436	7,774	- 1	5,178	4,952	5,230
30 31 31 22 33 34 32 507,206 787,501 008,362 738,190 500,001 600,673 710,088 2,444,104 2,000,303 1	1 1/2"							٦,	ŀ	Winter Quarter	Average per Cust	omer per Class	per Month by Ye				Winter Ou	arter Average per	š	r Class by Year		
COTON'S ANIMAL'S GOOD ANIMA ANIMA	Total Wholesale City	8	31	31	я	8	*	a	907.526	787.591	606.352	738 190	500.005		710.088							40,783
															-	200	2,000,0	202010101	1,790,321	1,706,309	1,720,320	1,666,019

Section 8 – Technical Support Appendices

Appendix 8.K Air Quality Permit

The City has applied for construction permits for the WWTP as discussed in Section 4.6, but has not received any permits to date. The most recent correspondence regarding air permitting is enclosed.



CITY OF LOVELAND

DEPARTMENT OF WATER & POWER

SERVICE CENTER

200 North Wilson, Bidg. #1 • Loveland, Colorado 80537 (970) 962-3000 • (970) 962-3400 FAX • (970) 962-2620 TDD

11/13/2009

Mr. Michael J. Harris, P.E.
Stationary Sources Program
Air Pollution Control Division
Colorado Department of Public Health and Environment
APCD-SS-B1
4300 Cherry Creek Drive South
Denver, CO 80246-1530

RE: Facility Wide Permit Application #09LR0212
City of Loveland Wastewater Treatment Facility

Dear Mr. Harris:

As you may remember, we have recently completed a construction project at our Wastewater Treatment Plant which included the installation of a 1,482 hp Cummins generator for emergency backup power and for use in peak shaving. This project started in early November of 2007. At that time it was anticipated that a separate APEN for this generator was all that was required to operate this generator as facility wide emissions based on APEN reportable sources were below permitting levels and therefore didn't require a permit, However, that same month the Denver ozone non-attainment zone was redefined and the area surrounding our plant was included in the new non-attainment zone. With the lowered permitting levels associated with inclusion in the non-attainment zone, facility emission totals were then above permitting levels for VOCs. This required us to submit a facility wide air permit application. Along with the new 1,000 KW Cummins generator, this permit application included reclassifying the use of our existing 600 KW Cummins generator to include peak shaving along with emergency backup power and the inclusion of our plant in the non-attainment area required us to submit a facility wide air permit application. You kindly advised us that we could qualify as a synthetic minor contributor by agreeing on limitations on the total hours of use for these two generators. You also requested updated APEN's for the waste gas flare (02LR0076) and the Wastewater Treatment facility (96LR431).

I updated all APENS's for all sources at our facility. Where appropriate, they are based on actual 2008 data. Additionally, to satisfy the energy demand management goals of our Power Division, this updated application requests operating hours of 800 hours/year for the both generators.



Our consulting engineers, CH2M Hill, reviewed this application and noted a discrepancy in the AIR ID numbers for the Digester Flare source, 02LR0076, and the Wastewater Treatment source, 96LR431. Both APEN's had AIR ID number 089/0076/001. Additionally, the old generator, ENG01 - #04LR0076, has the AIR ID 069/0308/003. My research indicates that this air ID was assigned to the Wastewater Treatment source, 96LR431, in the 1992 APEN submittals from our facility. We are thus requesting that your department review AIR ID numbers in this submittal and correct or reissue AIR ID numbers as you deem necessary.

I also wanted to reassure you that we are not using the new 1,000 KW generator for peak shaving or emergency backup yet. We are still installing the programming for the peak shaving mode and working on operating procedures. During generator testing while installation was taking place, several problems with equipment restarting was observed. We have reprogrammed much of this sequence and are awaiting approval from the Air Pollution Control Division to proceed further.

Should you have any questions regarding the application, please contact me at (970) 962-2572.

Sincerefy

Michael McCrary

Wastewater Treatment Plant Manager

Enclosure

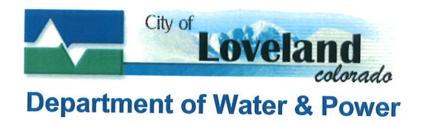
CC: Steve Adams, Water Utilities Manager Bob Miller, Power Operations Manager

Section 8 – Technical Support Appendices

Appendix 8.L Odor Control Studies

The most recent odor management study for the WWTP from 2005 is enclosed.





Wastewater Treatment Plant Odor Management Phase 2

Project W428HG

Final Report

Prepared by



May 2005

		¥

Contents

	Page
Contents	:
Executive Summary	i 1
Setting Odor Prevention and Control Criteria	, <u>1</u> 1
Baseline Modeling	, . ጎ
Modeling of Odor Control Alternatives	, <u>~</u>
Liquid Phase Treatment	. 0
Recommendations	, () ייי
Introduction	. / 14
Current Odor Control at Loveland WWTP	1.L
Setting Odor Prevention and Control Criteria	!. !)
Odor Complaint History	1.4
Odor Sampling	Լ4 <u>ֈ</u> գր-
Jerome Meter Sampling	LO IC
Flux Chamber Sampling.	12
Nasal Ranger Sampling	10 10
Baseline Model	io m
Technical Approach	10)()
Results of Baseline Odor Modeling	10 77
Odor Control Modeling	`./ >-1
Technical Approach). 21
Results of Odor Modeling with Control Scenarios) I
Liquid Phase Treatment) '1 }'7
Technical Approach)/ }7
Description of Alternatives	n M
Comparison of Alternatives	12
Liquid Phase Treatment Conclusions	16 16
Conclusions	:U IQ
Recommendations	:0 0
Immediate Recommendations	i) LQ
Short-Term and Long-Term Recommendations 5	:) (0
References5	6

÷

List of Tables

ES-1	Maximum 5-Minute and Annual Average Odor Impacts from Existing Sources at Fenceline Receptors
ES-2	Conditions Represented in the Odor Control Modeling
ES-3	Cost Summary for Long-Term Recommendations
ES-4	Odor Control Recommendations Compared to Current CIP
1	Acceptable Hours per Year of Odor Exceedance at Various D/T Ratios
2	Summary of Loveland WWTP Jerome Meter Sampling Results
3	Summary of Loveland WWTP Flux Chamber Sampling Results Based on Laboratory Results
4	Summary of Loveland WWTP Fenceline Sampling Results
5	D/T Ratio and Typical Human Reactions
6	Summary of Loveland WWTP Odor Sources Included in the Modeling Effort
7	Maximum 5-Minute and Annual Average Odor Impacts from Existing Sources at Fenceline Receptors
8	Meteorological Conditions When The Maximum Impact Occurred
9	Conditions Represented in each Odor Control Stage
10	Maximum 5-Minute and Annual Average Odor Impact (D/T) from the Entire Plant for Odor Control Scenarios
11	Summary of Dissolved Sulfide Sampling (Grab Samples)
12	Summary of Interceptor Model Results
13	Chemical Control of H ₂ S and Corrosion in Sewers
14	Dosages and Annual Costs for Chemicals Evaluated
15	Cost Evaluation of Liquid-Phase Odor Control Alternatives
16	Qualitative Evaluation of Liquid-Phase Odor Control Alternatives between the Lift Station and the Inverted Siphon
17	Odor Control Recommendation Summary
18	Cost Summary for Long-Term Recommendations

-	1		

List of Figures

- Worst-Case Baseline Modeling Results, Number of Hours per Year above 7 D/T from All Sources
- One-Day Baseline Modeling Results, Number of Hours per Year above 7 D/T from All Sources
- 3 Off-Site Receptors
- 4 Loveland WWTP Odor Source Prioritization
- 5 Predicted Off-Site Odor Reduction for Odor Control Recommendations
- 6 Aerial Photograph of the Loveland WWTP and Surrounding Vicinity
- Worst-Case Baseline Modeling Results Before Carbon was Replaced, Number of Hours per Year above 7 D/T
- 8 Location of Majority of Odor Complaints
- 9 Jerome Meter
- 10 Sampling Locations for the Plant Sampling
- 11 Flux Chamber Sampling
- 12 Nasal Ranger
- 13 Sampling Locations for the Fenceline Sampling
- 14 Percent of Time per Year Offsite Odor Impact in D/T from All Sources, Worst-Case Baseline
- Frequency of Exceedences above 7 D/T by Time of Day over a Year from All Sources, Worst-Case Baseline
- Odor Control Stage 1 Modeling Results Discontinue Use of Trickling Filters, Number of Hours per Year above 7 D/T
- 17 Odor Control Stage 2 Modeling Results Repair Digester Boiler Room Vent, Number of Hours per Year above 7 D/T
- Odor Control Stage 3 Modeling Results Odor Control for Aerated Grit Basin, Number of Hours per Year above 7 D/T
- Odor Control Stage 4 Modeling Results Odor Control for Headworks Facility, Number of Hours per Year above 7 D/T
- 20 Odor Control Stage 5 Modeling Results Odor Control for DAFT, Number of Hours per Year above 7 D/T
- Odor Control Stage 6 Modeling Results Odor Control for Primary Clarifiers, Number of Hours per Year above 7 D/T

- Odor Control Stage 7 Modeling Results Odor Control for Aeration Basin and Digesters, Hours per Year above 7 D/T
- 23 Primary Wastewater Collection System and Lift Stations
- 24 Results of OdaLog Sampling in Headworks Channel

List of Appendices

- A Windroses for 2003 by Season
- B State of Colorado Regulation 2, Part A General Provisions
- C Photographs of Odor Sources Sampled
- D Summary of Jerome Meter Sampling Results
- E Flux Chamber Sampling Report
- F Summary of Fenceline Sampling Results
- G Baseline Dispersion Modeling Input
- H Proposed Odor Control Equipment Cut Sheets
- I Dissolved Sulfide Sampling Locations and Laboratory Analyses
- J Liquid Phase Treatment Analysis
- K Material Safety Data Sheets (MSDS) for Liquid Phase Treatment Chemicals
- L Summary of Cost Estimates
- M Figures

Executive Summary

This Odor Management Plan presents the results of the odor impact assessment conducted by CH2M HILL for the City of Loveland's Wastewater Treatment Plant (WWTP). The objectives of this odor assessment were to determine the treatment plant's baseline odor impacts to the surrounding community and evaluate potential odor control improvements.

An assessment of the WWTP's odor impacts on the surrounding area was conducted with extensive sampling and odor dispersion modeling. The results of the modeling were used to quantify the WWTP's odor impact, to prioritize the potential odor sources, and to develop a phased list of capital improvements that the City will implement as-needed to reduce the offsite impacts and comply with State of Colorado regulations.

Setting Odor Prevention and Control Criteria

A key objective to a successful odor assessment and control program is to determine what level of odor will cause an odor nuisance response by the public, and then control odors to levels lower than these thresholds. It is not reasonable to expect that a treatment plant will never have odors. Neighbors of treatment plants will typically tolerate odors for small portions of time. Treatment plants located in residential communities typically have odor goals of ranging from 4 to 20 dilutions-to-threshold (D/T), with an allowance of 100 hours per year to exceed the threshold. The allowance is to provide a margin of error. Under normal operating conditions the plant is expected to meet its odor threshold. However, plant upsets and equipment failures can and do occur. These abnormal operations would be acceptable within the time period allotted for the allowable hours above the threshold. Commercial/industrial communities typically have odor goals of 20 D/T or higher, with a similar allowance of 100 hours a year to exceed the threshold.

The State of Colorado (State) regulates odors under Regulation 2, Part A – General Provisions. The regulation states that there should be no detectable odors at the site of odor impact after the odorous air is diluted by 7 volumes of odor-free air or more where the land use is either predominantly commercial or residential. For all other land uses the dilution is 15 odor-free air volumes or more. Since the City's WWTP is adjacent to many residential areas, 7 dilutions to threshold (D/T) is the appropriate criterion for the WWTP. To determine compliance with this regulation, the State does not perform any routine sampling of odors. Any testing done by the State would likely be done as the result of a complaint. When the State does come out to sample, they would determine compliance if two samples exceed the standard within a one-hour period.

As part of this Odor Management Project, CH2M HILL has developed an odor control capital improvement program that should allow the City to comply with the State Standard. Due to the conservative nature of the analysis conducted, CH2M HILL recommends that the improvements recommended meet a model-predicted odor control goal that the odor emissions will be less than 7 dilutions-to-threshold (D/T) 99 percent of the time.

Baseline Modeling

The baseline or current odor modeling assessment used emission rates obtained from the two odor sampling events conducted at the Loveland WWTP during 2003 and 2004. The purpose of the two sampling events was to capture the main odor generation periods when the City tends to see the most odor complaints, summer and fall. The first sampling was conducted with the Jerome 631-X hydrogen sulfide (H₂S) analyzer. This sampling event collected H₂S concentration data during 30 sampling rounds from October 2 to October 23, 2003. The second sampling event was conducted using an Environmental Protection Agency (EPA)-approved flux chamber to capture the odor emissions from the plant processes. This was a one-day sampling event conducted on June 2, 2004. Laboratory measurements of ammonia, reduced sulfur compounds, and odor (analysis by an odor panel) were obtained. The sampling results indicate that the odor from the Loveland WWTP is caused by more than just H₂S. To account for the combined effect of all odorous compounds, odor was modeled instead of just H₂S.

CH2M HILL entered odor emission rates from the source sampling and source parameters into an odor dispersion model, Industrial Source Complex – Short Term Version 3 (ISCST3). This model predicted off-site odor impacts at numerous receptor locations surrounding the Loveland WWTP site. Five years of meteorological data from Fort Collins-Loveland Airport were initially evaluated (1999 – 2003); 2003 was the year that resulted in the highest off-site impacts. Therefore, only 2003 meteorological conditions were modeled in subsequent model runs. It is standard practice to use meteorological data from the nearest airport when the local site does not have an on-site meteorological station; however, there may be some slight differences in wind speed and direction due to local topography at the Loveland WWTP.

The baseline odor assessment included all of the treatment processes that are typically online in the summer. Two scenarios were modeled based on the two sampling events, capturing the seasonal periods when odor complaints are received: "worst-case" and "one-day". Both baseline model results were compared to the odor threshold of 7 dilutions-to-threshold (D/T), which is consistent with the State of Colorado standard.

Worst-Case Baseline: Jerome meter sampling data as the model input. Jerome meter sampling was conducted over a three-week period. The highest concentrations for each source were selected to represent the worst-case scenario.

One-Day Baseline: Based on flux chamber sampling data as the model input. The flux chamber sampling was conducted on a single day.

The worst-case baseline is considered a worst-case because the sampling event took place in the fall, when odor complaints tend to be highest, and the highest emissions sampled over a period of three weeks were selected. In addition, the worst-case baseline uses H₂S emissions converted into total odor (D/T) while the one-day baseline uses D/T sampled from the main odor sources. The method of conversion (explained in more detail in the main report) adds some additional conservatism to the worst-case baseline. The one-day baseline may be closer to an overall average, or more "typical" day. The sampling was conducted on a single-day, with some of the sources sampled in the early morning. There may also be some differences in results due to type of measurement tool used, time of sampling event, and plant loading/operating conditions, but using the worst-case baseline to prioritize the odor

sources will provide the highest odor emissions potential. Under normal or average conditions, the plant's odors will be much lower, and even lower with controls. This conservative approach helps to ensure that the recommendations made will reduce the offsite impacts significantly.

Baseline Results

The worst-case baseline (based on the Jerome meter sampling) which includes the odor impact from all the existing sources at the Loveland WWTP and is based on a 5-minute averaging period, shows the isopleths, or contours, with the hours of yearly exceedance of an odor standard of 7 D/T. This baseline is illustrated in Figure 1. There is a significant off-site area that can perceive the 7 D/T or higher odor levels greater than 100 hours per year. A similar isopleth was created for the one-day baseline (flux chamber sampling) modeling results, shown in Figure 2. The one-day baseline represents a typical day without much noticeable odors in the community surrounding the Loveland WWTP. It shows much smaller impact area focused on the north end of the plant. As described above, the worst-case baseline is intended to capture the worst possible odor impact and is a more conservative approach, which explains the much larger odor impact.

The highest off-site odor impacts from both baseline models were tabulated by odor source to assess their contribution to off-site impacts. This information also allows control efficiency requirements for each odor source to be determined for the plant to meet the odor standard. Table ES-1 presents the maximum 5-minute odor impacts and maximum annual average odor impacts expressed as D/T for each major odor source. The maximum 5-minute odor impacts is the highest D/T predicted at an off-site receptor (location surrounding the plant site) and the annual average D/T is average D/T predicted at an off-site receptor. Figure 3 shows the receptors where the highest maximum 5-minute D/T occurred for all sources combined (Receptor A) and where the highest annual average exceedence occurred for all sources combined (Receptor B). The ratio of the maximum annual odor to the maximum 5-minute odor, peak-to-mean ratio, is a parameter indicating the frequency of the maximum odor occurrence, and is also shown in the table. Note that the maximum odor source impacts are not cumulative because they occur at different times and locations.

TABLE ES-1

Maximum 5-Minute and Annual Average Odor Impacts from Existing Sources at Fenceline Receptors

		rst-Case Bas rome Meter D		(One-Day Baseli Flux Chamber D	
Source Group	Max 5-min D/T	Avg Annual D/T	Peak-to- Mean (5-min D/T)/ (Annual D/T)	Max 5-min D/T	Avg Annual D/T	Peak-to- Mean (5-min D/T)/ (Annual D/T)
All Source	1,128	20.3	55	136	2.2	61
Digester Boiler Room Vent	1,000	18.0	56	67	1.2	56
Aerated Grit Basin	857	3.5	242	71	0.3	238
DAFT	233	0.8	293	50	0.2	293
Trickling Filter	174	1.3	132	70	0.5	133
Screw Pumps	163	1.5	107	18	0.2	107
Primary Clarifier	146	0.7	197	49	0.3	159
Flare	79	0.6	134	3	0.0	135
Headworks Door	30	0.5	63	3	0.0	63
Aeration Basins	28	0.4	69	81	1.0	81
Headworks Building Exhaust	5	0.1	70	1	0.0	69
Digesters	1	0.0	. 98	,		
Biosolids Loading	0	0.0		7 may m. (10 may m. (1		

Predictions based on 2003 surface meteorological data from Fort Collins-Loveland Airport.

Model output was converted to 5-minute average concentrations using a factor of 1.64.

For the worst-case baseline, the maximum combined 5-minute odor impact from all the sources was 1,128 D/T, which is significantly higher than the odor threshold of 7 D/T. The maximum combined 5-minute odor impact from the digester boiler room vent was 1,000 D/T at the fenceline. The digester boiler room vent is the most significant contributor to the off-site odor impact in terms of strongest odors. The next source having the highest maximum 5-minute odor impact is the aerated grit chamber, which generated 857 D/T of maximum 5-minute odor impact at the fenceline. The ratio of maximum 5-minute odor to the maximum annual odor at the digester boiler room vent was only 56, suggesting the mean impact from this source is almost as significant as the peak impact. In contrast, the peak-to-mean ratio for the aerated grit basin was 242, suggesting that this odor source is less chronic and more acute in nature.

The baseline results from both scenarios are much higher than the state standard of 7 D/T, which is an extremely stringent odor threshold to attain and maintain over an entire year. In the worst-case baseline, the worst-case odor emission rates were used and applied over the entire year, regardless of seasonal conditions. This approach ensures that the highest

potential odor release scenarios are covered and that the plant will normally have odor emissions that are well below these conservative estimates, with the odor controls recommended.

The ranking of the odor sources was based on the maximum 5-minute odor strength (D/T) and the peak-to-mean ratio analysis from the Worst-Case baseline model. Figure 4 summarizes the ranking of the major odor sources at the plant. The remainder of the analyses conducted were focused on the Worst-Case baseline since those odor impacts are more consistent with the odor complaints from the surrounding community.

Modeling of Odor Control Alternatives

With the major odor sources identified using the baseline modeling, odor control alternatives were considered to reduce the odor emissions from the major sources. The baseline model was then revised to represent the off-site odor impact changes due to an odor control improvement. Seven odor control scenarios were modeled in this analysis to investigate the effect of positively controlling the odor sources. The odor control improvements either eliminate the identified big odor sources completely, such as the trickling filters, or convert the major odor sources into the odor control scrubbers that emit significantly less odor, such as the chemical scrubber treating the Headworks and grit chambers at Stage 4. The major sources controlled were selected based on the prioritization in baseline modeling. The conditions represented in these seven odor control scenarios are shown below in Table ES-2. The check marks indicate which proposed odor control improvements (shown in rows) were modeled in each control scenario (shown in columns).

As shown later in the report (Figures 16-22), the control modeling results show that odor control approaches represented in Stages 1 through 7 can drastically reduce the off-site impacts to levels of insignificance outside the plant fenceline. The modeling results predict that the Loveland WWTP would meet their desired odor control goal of less than 7 D/T 99 percent of the time at Stage 7. However, due to the conservative nature of the modeling analysis, CH2M HILL recommends that the City implement Stages 1 through 5 to meet the State Standard. At that point, the City should continue to monitor their progress to see if additional odor control is required.

TABLE ES-2
Conditions Represented in the Odor Control Modeling

Odor Control Project	Description	Stage 1	Stage 2	Stage 3	Stage 4	Stage 5	Stage 6	Stage 7
Trickling Filters	Discontinue the use of trickling filters.	✓	√	✓	✓	\checkmark	✓	✓
Digester Boiler Room Vent	Eliminate the fugitive odors being collected in the HVAC exhaust		\checkmark	\checkmark	\checkmark	\checkmark	\checkmark	\checkmark
Aerated Grit Chamber	Cover aerated grit chamber and install a new carbon unit to treat the air from grit chamber (95% odor removal)			✓	\checkmark	\checkmark	\checkmark	✓
Headworks Building	Ventilate new or modified Headworks building at 12 ACH. Provide a new chemical scrubber to treat the air from both the aerated grit chamber and the Headworks building (99% odor removal). Replace screw pumps or cover and ventilate to the odor control scrubber.				✓	✓	✓	✓
DAFT	Maintain negative pressure inside DAFT by providing 12 ACH ventilation. Add a new carbon unit to treat the air from DAFT (95% odor removal)					✓	✓	✓
Primary Clarifiers	Cover and vent primary clarifiers to odor control scrubber (95% removal efficiency)						✓	√
Aeration Basins and Digesters	Cover and vent aeration basins to odor control scrubber (95% removal efficiency). Provide odor control for digesters with fixed roof tanks.							✓

Liquid Phase Treatment

Literature and CH2M HILL's experience indicates that liquid phase treatment of odor generating compounds in the collection system forms a cost effective component of multi-phased odor management plans for wastewater treatment facilities when the influent dissolved sulfide concentrations exceed 1.0 milligrams per liter (mg/L). For the City's collection system, the modeling and sampling conducted indicate that the City has influent wastewater dissolved sulfide concentrations greater than 5 mg/L.

The analysis conducted indicates that the Boyd Interceptor and Boyd Relief Interceptor contribute most to the sulfides at the plant. The Southside Interceptor contributes a small portion of the overall sulfide loading to the plant, but the sampling program showed that the forcemain discharge generates high peak hydrogen sulfide concentrations within the Headworks area. These peaks likely generate short-term odor releases that could lead to

odor complaints. CH2M HILL recommends an odor management strategy that addresses both of these contributors.

CH2M HILL has considered several sulfide control options. Ferric Chloride addition has the second highest life-cycle costs and ranks third in the non-economic evaluation. Ferric chloride requires special handling procedures and is a corrosive product. Bioxide™ provides the lowest life-cycle cost, but may require more stations than ferric chloride. However, the product is relatively harmless and does not have the same handling and storage requirements. The Town of Castle Rock, Colorado has used Bioxide™ to control odors in their interceptors. There are also numerous Bioxide-equivalent products that can be used.

CH2M HILL recommends that the City begin with BioxideTM (or equivalent) on the basis that it is the most cost effective and will be added at the lift stations, which will provide an additional benefit of corrosion control in the collection system. The City should consider contacting Castle Rock, Colorado staff regarding their BioxideTM program and its success. The following approach is suggested for proceeding with the liquid phase, sulfide control program:

- 1. Conduct a pilot test with Bioxide™ (or equivalent) being added at the Eastside lift station. During the pilot test, conduct sampling of both the dissolved sulfide levels of the influent and the H₂S concentrations at the odors sources.
- 2. If the pilot test is effective, implement permanent Bioxide™ (or equivalent) dosing stations for Boyd systems first (Eastside and Boyd Lake lift stations), then addresses the smaller contributors should further odor reductions be needed.
- 3. If the Bioxide™ is not effective, conduct a pilot test with another liquid phase treatment chemical, such as ferric chloride.
- 4. Commit to a data collection program that will allow stakeholders to evaluate the impact of the proposed mitigation measures. The data collection program would involve monthly sampling of the dissolved sulfide levels at the influent, as well as sampling the odor sources for H₂S using a Jerome meter.

Recommendations

A summary of the recommended long-term improvements, with cost estimates, are included in Table ES-3. CH2M HILL recommends that the City plan to incorporate Stages 1 through 5 in their current CIP, at a capital cost of \$1.3 million. It is anticipated that this level of odor control will meet the State Standard, given the conservative nature of the analysis. For the City to have a zero odor emissions plant, Stage 6 and 7 would be necessary, and the additional the cost would be approximately \$5 million Therefore, to meet the State Standard, the cost would be \$1.3 million and the cost to meet a zero odor emissions goal would be \$6.3 million total.

The average annual costs are also estimated in Table ES-3. For future operations at the Loveland WWTP with full scale odor control, the annual operating costs for odor control could be as high as 5 to 15 percent of the annual operating budget. This is what a typical WWTP spends on odor control.

The cumulative odor reduction to be expected from each odor control stage, including liquid phase treatment, is shown in Figure 5. It is assumed that liquid phase treatment is implemented after the trickling filter is taken off-line (Stage 1) and the digester boiler room HVAC intake vent is relocated (Stage 2). For Stages 3 through 7, the predicted odor reduction is shown for each stage with and without the cumulative impact of liquid phase treatment. As additional odor control improvements are implemented, the additional odor reduction impact of liquid phase treatment becomes insignificant. However, liquid phase treatment continues to have benefit by reducing the chemical requirements for the odor control scrubbers.

Plant emissions are variable and so are removal efficiencies of odor control systems. After each phase of capital improvements, the sources should be re-sampled and the odor dispersion model re-run to predict the current plant conditions. This will enable the City to assess the effectiveness of the phased recommendations and confirm if all the capital improvements below are required, or if there are other new odor sources that require control. The cost of a Jerome meter is included in Odor Control Stage 3 so the City can conduct the confirmation sampling. The effort to re-run the dispersion model is included in Stage 4 to confirm the odor control benefits of the stages up through Stage 4. The long-term recommendations provided in Table ES-3 may or may not be necessary in the future, and careful evaluation should be performed before implementation.

Prior to this study, the City was already planning to implement odor control improvements to help reduce the off-site odor impacts. Table ES-4 presents a comparison of the odor control improvements to the City's current five year capital improvement projects (CIP) intended for odor control. It is recommended that the City update their CIP to be consistent with the recommendations presented in Table ES-3 when they conduct the annual review of the CIP.

The City currently has a total of approximately \$850,000 set aside for odor control improvements during 2005 through 2006. To implement Stages 1, 2, and 3 along with liquid phase treatment will only cost the City approximately \$300,000. Stage 4 is the next odor control improvement recommended that will have a significant impact on the off-site odor reductions. If the City can increase the budget for the odor control improvement projects in 2005 and 2006, it is recommended that the odor control scrubbers recommended in Stage 4 be installed to provide odor control for the current Headworks facility. These scrubbers can be reused for the new Headworks facility, especially if the City is going to maintain the current Headworks building. Also, the City should consider implementing the new Headworks facility earlier than currently planned.

TABLE ES-3
Cost Summary for Long-Term Recommendations

Odor Control Stage	Long Term Recommendations	Air Flow Rate (cfm)	Capital Cost*	Annual Cost	Timing
1	Discontinue use of trickling filters	NA	\$10,000	\$0	2004
2	Rearrange digester boiler vent HVAC system	NA	\$200,000	\$0	2005
LPT	Conduct a pilot test of Bioxide™ or equivalent chemical	NA	\$37,000	`NA	2005
	Implement a liquid phase treatment program	NA	\$35,000	\$68,000	2005
3	Cover aerated grit chamber and vent to a carbon scrubber	250	\$68,000	\$6,000	2005
4	Provide odor control for modified Headworks processes, including screw pumps and influent collection well, within existing Headworks building. Vent air from Headworks building through a new chemical scrubber polished with bioscrubber or carbon to achieve 99% removal efficiency.	13,000	\$892,000	\$87,000	2006 / 2009
5	Vent air from DAFT in a new carbon scrubber.	800	\$84,000	\$18,000	2008
6	Cover primary clarifiers and vent to new chemical scrubbers	3,800	\$1,614,000	TBD	TBD
7	Cover aeration basins and vent to new chemical scrubbers. Replace digester covers with fixed roof covers	8,600	\$3,353,000	TBD	TBD

^{*}Total capital costs include construction and engineering costs. Construction costs include 30% contingency; engineering costs are estimated at 25% of construction cost

cfm = cubic feet per minute

TABLE ES-4
Odor Control Recommendations Compared to Current CIPa

)					
Odor Control Project	2005	2006	2007	2008	2009	Project Recommendations (Odor Control Stage)
Design & SDC odor control	\$70,000	\$72,100				Discontinue use of trickling filters, relocate digester room HVAC intake vent. liquid phase treatment, and install
Construction odor control	\$350,000	\$360,500				new odor control scrubber for aerated grit chamber (Stages 1-3)
Replace existing screw pumps ^b	\$30,000	\$339,900				
Design and SDC WAS Thickening ^b		\$372,345	\$191,759	\$197,511		Provide odor control as part of WAS thickening
Construction WAS Thickening ^b			\$1,538,305	\$1,584,455		improvements (Stage 5)
Design and SDC Influent Pumping and Headworks Facility ^b					\$514,921	Provide odor control as part of Influent Pumping and Headworks Facility Improvements — project extends
Construction Influent Pumping and Headworks Facility ^b					\$1,716,400	beyond 2009 (Stage 4)

^aCosts include an annual inflation factor

^bCost included for these projects is for the entire project, which includes design and construction of new process facilities, where odor control is portion of that project

Introduction

Wastewater treatment plants have inherent odors based on the nature of biological processes. Currently, a majority of odor complaints related to the Loveland WWTP occur in the late fall and winter, as the temperature changes from warmer to colder. Odor complaints have also been received on summer evenings and weekends when more people are at home and outside near the WWTP, making it easier to notice odors. Odor complaints may be increasing because development is moving closer to the WWTP, as reflected in new construction within 400 feet to the north of the plant. An aerial photograph of the Loveland WWTP and surrounding area is included on Figure 6.

The prevailing wind direction is blowing from the southwest, as indicated by the windroses included in Appendix A. The prevailing winds are blowing directly towards the new residential developments and what is currently undeveloped land. This undeveloped land is slated for future development, which will increase the likelihood of odor complaints if conditions remain the same at the WWTP.

The Loveland WWTP is currently undergoing expansion to meet new and more stringent wastewater treatment regulations. The current construction project started in June 2003 and will be completed by November 2004. The process changes that will be conducted as part of the construction project are to change the existing activated sludge process to a step-feed, increase aeration basin volume, install an ultraviolet disinfection system, abandon the existing chlorine contact basin, and provide significant improvements to the electrical system. The changes to the aeration basins will allow elimination of the trickling filter process, which will reduce the odor emissions at the plant.

The State regulates odors under Regulation 2, Part A – General Provisions, which is provided in Appendix B to this TM. The regulation states that there should be no detectable odors at the site of odor impact after the odorous air is diluted by 7 volumes of odor-free air ore more where the land use is either predominantly commercial or residential. For all other land uses the dilution is 15 odor-free air volumes or more. Since the City's WWTP is adjacent to many residential areas, 7 dilutions to threshold (D/T) is the appropriate criterion for the WWTP. Odor emissions are generally measured and regulated in terms of odor strength or D/T, which quantifies the degree of odor perception of a whole air sample. D/T is defined as the point where the odor is barely perceptible to the sampler. The number of dilutions of pure air required to barely perceive the odor then indicates the strength of the sample. Relatively speaking, the higher D/T number, the stronger the odor.

In 2003, CH2M HILL conducted a baseline odor sampling event for the City of Loveland using H₂S as a representative for total odor. The purpose of the sampling work was to assist the City to act quickly to understand and continue to mitigate potential offsite odors. The sampling results from this baseline odor sampling are documented in the City of Loveland Wastewater Treatment Plant Odor Sampling Technical Memorandum (CH2M HILL, 2004). The results were used to initially rank odor sources and prioritize recommended improvements. The odor sources found to be significant in the baseline sampling were targeted during the comprehensive odor study as part of the odor management study conducted in 2004,

documented in this Odor Management report. This report uses information developed in 2003 and provides updated recommendations for the City to reduce the odor impacts to the surrounding community.

CH2M HILL developed this odor management plan for the Loveland WWTP on behalf of the City. The goals and objectives of the odor management project were to understand existing odor sources, determine the off-site odor impacts, rank the odor sources, and propose an odor control improvements program that will be integrated into the City's capital improvement program (CIP). To understand existing odor sources, field investigations were performed to locate existing odor sources and sample each source's H₂S level. Hydrogen sulfide was used as a surrogate for odor in the initial testing and targeted sources were later sampled for odor as well as H₂S and ammonia. The sampling data was used to develop an odor impact model of the existing treatment plant. After the odor sources were identified, odor control measures were modeled to show the potential reduction in off-site odor impacts.

Current Odor Control at Loveland WWTP

Prior to 1986, the City has relied primarily on operational practices to reduce off-site odor impacts and there was no odor control equipment at the WWTP to reduce the off-site odor impacts. In 1986, due to increasing odor awareness, the City installed the carbon scrubber in the Headworks building to reduce the off-site odor impacts from the grit removal and screenings processes. It was acknowledged during the initial baseline study that the carbon scrubber was not providing effective odor control since the carbon in the scrubber was plugged and not removing odors from the Headworks Building. The City replaced the carbon in March 2004, which has significantly reduced the odors being released from the Headworks Building. Figure 7 shows the offsite odor impact for the Loveland WWTP prior to the carbon changeout. However, odor awareness continues to increase among the neighbors of the WWTP. In response to this increased odor awareness, the City has begun to plan for and implement odor control for the significant odor sources as part of this study.

Setting Odor Prevention and Control Criteria

Odors are highly subjective in nature and each person can have a unique response or reaction to odors at various concentration levels. A key objective to a successful odor assessment and control program is to determine what level of odor, as sensations (subjective phenomena) versus odorant emissions (objective phenomena), will cause an odor nuisance response by the public, and then control odors to levels lower than these thresholds. Successful WWTPs have tended to set their standards together with the surrounding community through a process of trial and error.

It is not reasonable to expect that a treatment plant will never have odors. Neighbors of treatment plants will typically tolerate odors for small portions of time. Treatment plants located in residential communities typically have odor goals of ranging from 4 to 20 dilutions-to-threshold (D/T), with an allowance of 100 hours per year to exceed the threshold. The allowance is to provide a margin of error. Under normal operating conditions the plant is expected to meet its odor threshold. However, plant upsets and

equipment failures may occur. These abnormal operations would be acceptable within the time period allotted for the allowable hours above the threshold. Commercial/industrial communities typically have odor goals of 20 D/T or higher, with a similar allowance of 100 hours a year to exceed the threshold.

A relationship between D/T and acceptable hours per year that the threshold D/T could be exceeded without becoming a nuisance odor was developed based on experience at other WWTPs. This relationship is described in **Table 1**. These standards were typically developed with the input of the surrounding community. The neighbors were included in decision-making sessions that determined how often the neighbors would tolerate odors above the threshold without complaining. These standards, when met, allow the community to gain trust in their neighboring WWTP. However, public response is highly subjective. A highly energized and sensitive community may have lower acceptable hours per year exceedence thresholds.

TABLE 1
Acceptable Hours per Year of Odor Exceedance at Various D/T Ratios

Hours of		A-11-11-11-11-11-11-11-11-11-11-11-11-11	D/T Ratio	**************************************	
Exceedence per Year	4	7	20	50	100
0-10	Acceptable	Acceptable	Acceptable	Acceptable	Acceptable
10-50	Acceptable	Acceptable	Acceptable	Acceptable	Not Acceptable
50-100	Acceptable	Acceptable	Acceptable	Not Acceptable	Not Acceptable
100+	Acceptable	Not Acceptable	Not Acceptable	Not Acceptable	Not Acceptable

^{1.} These acceptable hours are based on CH2M HILL's previous experience at several U.S. and global wastewater treatment and sludge lagoon facilities. However, public response is highly subjective and the above scenarios are intended as a planning guide only. A highly energized and sensitive community may have lower acceptable hours per year exceedence thresholds.

The State odor standard of 7 D/T or more is applicable at all times; it is not possible to obtain a waiver for certain times of the year or for a number of hours. However, to determine compliance with the regulation, the State does not perform any routine sampling of odors. Any testing done by the State would likely be done as the result of a complaint. When the State does come out to sample, they would determine compliance if two samples exceed the standard within a one-hour period. The State does take into account plant upsets and equipment problems that may cause the odors to exceed the limit. Other municipalities within Colorado have been successful by conducting public outreach to educate the surrounding community to call the WWTP with odor complaints rather than the State or county. As part of this Odor Management Project, CH2M HILL recommends has developed an odor control capital improvement program that will allow the City to comply with the State Standard. Due to the conservative nature of the analysis conducted, CH2M HILL recommends that the improvements recommended meet a model-predicted odor control goal that the odor emissions will be less than 7 dilutions-to-threshold (D/T) 99 percent of the time. This will allow the City to respect the boundaries between the community's odor objective and to be consistent with the State Standard.

Odor Complaint History

The City has a procedure in place for responding to odor complaints, which has assisted in expediting the process and response to odors. Odor complaints are received by the plant operator, who logs the complaint and attempts to identify the source of the odor. When possible, action is taken to minimize the release of odors. Follow-up with the residents is conducted if necessary. In March 2004, the City began to monitor the odor complaints received by maintaining detailed logs of each complaint. The area of the most documented odor complaints is highlighted in Figure 8. This figure was used to validate the modeling results to the actual odor impacts indicated by the odor complaints. This provides support for the modeling results and aids in meeting the project objectives. The odor complaints agree with the selected odor control threshold criteria, at less than 7 D/T 99 percent of the time.

Odor Sampling

Two odor sampling events were performed at the Loveland WWTP as part of this odor management study. The purpose of the two sampling events was to capture the main odor generation periods when the City tends to see the most odor complaints, summer and fall. The first sampling was conducted by CH2M HILL and Stewart Environmental, consisting of 30 sampling rounds from October 2 to October 23, 2003. The Jerome meter sampling covered a wide range of the potential odor sources and identified the sources to be sampled as part of the following flux chamber sampling. The second sampling event was conducted by Environmental Management Consulting, using an Environmental Protection Agency (EPA)-approved flux chamber to capture the odor emissions from the plant processes. This was a one-day sampling event conducted on June 2, 2004.

Jerome Meter Sampling

The Jerome H₂S analyzer, shown in Figure 9, measures instantaneous (less than 30-second sampling time) H₂S concentrations. The H₂S concentration data is converted to mass emission rates using assumed air velocities, but their reliability is usually limited by the difficulty of determining the airflow rates and the fact that only a single odor compound concentration is available.

The potential odor sources sampled were identified during a plant walk-through on October 1, 2003, based on the consultant's experience and group members' observation and experience. The plant sample locations are identified on Figure 10. Photographs of each of the sources are included in Appendix C. The Jerome meter sampling results are summarized in Table 2 and in Appendix D, which includes charts that show H₂S concentration over time for each odor source sampled.

Flux Chamber Sampling

With a flux chamber, samples are taken directly from the liquid surface through a closed vessel (innertube with a sampling port on top). The air flow off the liquid surface is measured as well as the mass or quantity of odorous compounds emitted. Together, these two measurements are the flux (or mass emission) of the compounds off the surface. This sampling method is illustrated in Figure 11. The air samples are analyzed in a laboratory for specific compounds and by an odor panel to determine odor intensity. Flux chambers provide the most accurate emission measurements from the surface areas.

During the flux chamber sampling event, stack testing and hand-held instruments such as the Jerome H_2S analyzer and gas detector tubes were also utilized to obtain the data on field H_2S , field ammonia, lab H_2S , lab reduced sulfur compounds, and odor panel responses (results expressed in D/T). Flux chamber sampling results are summarized in Table 3 and included in the Appendix E. The sampling results indicate that the odor from the Loveland

WWTP is caused by more than just H_2S . To account for the combined effect of all odorous compounds, odor was modeled instead of just H_2S .

TABLE 2
Summary of Loveland WWTP Jerome Meter Sampling Results

		Total Number of	H₂S	Concentration (opm)
Location Number	Location Description	Samples Taken	Average	Maximum	Minimum
1	Influent collection well	30	1.10	6.1	0.01
2	Grit hopper	30	2.33	4.7	0.61
3	Headworks odor control exhaust*	30	1.98	4.5	0.50
4	Headworks vent to 1st floor	30	2.84	7.1	0.57
5	Grit truck loading		Not	sampled	
6	Headworks effluent channel	29	6.82	18	0.65
7	Aerated grit chamber	30	4.63	21	0.02
8	Aerated grit effluent channel	30	1.17	9.6	0.00
9	Screw pumps (bottom)	30	1.42	8.1	0.14
10	Screw pumps (top)	30	2.88	9.3	0.12
11	Primary splitter box	30	2.67	14.9	0.25
12	Primary clarifier W (center)	30	0.14	0.60	0.01
13	Primary clarifler W (effluent weir)	30	0.54	2.2	0.02
14	Primary clarifier E (center)	29	0.12	0.65	0.01
15	Primary clarifier E (effluent weir)	29	0.37	1.33	0.02
16	Primary effluent wetwell	30	3.45	31	0.14
17	Trickling filter E	30	0.80	3.0	0.03
18	Trickling filter W	30	0.91	2.5	0.02
19	Trickling filter effluent channel E	30	2.77	28	0.04
20	Aeration basin N	30	0.07	0.58	0.01
21	Aeration basin effluent channel	30	0.10	0.45	0.00
22	Final clarifier	30	0.02	0.25	0.00
23	DAF thickener	30	3.00	19	0.61
24	Anaerobic digester (cover)	30	4.54	22	0.04
25	Anaerobic digester (PRV)	28	1.23	31	0.00
26	Digester boiler room vent	30	1.31	17	0.01
27	E digester junction box	30 .	1.40	31	0.01
28	W digester junction box	30	9.53	31	0.01
29	Biosolids truck loading - at hatch	8	23.0	> 50	23
30	Ambient air 10' from truck loading	7	2.31	18	0.00
31	RAS well	28	0.05	0.33	0.00

^{*}Prior to carbon replacement - after carbon replacement = 0.13 ppm H_2S Date sampled: October 7-23, 2003 and June 2, 2004

ppm = parts per million

 TABLE 3

 Summary of Loveland WWTP Flux Chamber Sampling Results Based on Laboratory Analysis

Location				Carbonyl Sulfide	Methyl Mercaptan	Dimethyl Sulfide		Dimethyl Disulfide
Number	Location Description	Odor (D/T)	H ₂ S (ppmv)	(nmdd)	(ppmv)	(ppmv)	CDS (ppmv)	(hpmv)
က	Headworks odor control exhaust	06	Q	0.017	S.	Q	0.0018	QN.
۷	Aerated grit chamber	4,000	26.1	S	0.339	Q	N	S
12	Primary clarifler W (center)	2,400	0.75	9	0.011	N	Ö	2
13	Primary clarifier W (effluent weir)	4,400	9.61	S	0.153	S	Ω Z	2
₩ ₩	Trickling filter W	2,700	7.07	N O	0.579	S	Q N	S
20	Aeration basin N (Old)	370	0.001	Q.	Q.	0.0015	0.001	0.006
23	DAF thickener	4,400	9.65	9	0.415	Q	2	S
28	W digester junction box	2,900	3.09	Q.	N N	Ω Ω	S S	8
58	Biosolids truck loading - at hatch	3,100	0.002	Q N	Q.	ON O	ΩN	QN
32	Aeration basin (New)	1,500	S	8	S	0.003	ΩN	0.027

ND = non detect
ppmv = parts per million by volume
Date sampled: June 2, 2004

In the flux chamber sampling, the new aeration basins had much higher odor levels (1,500 D/T) than expected based on the H₂S concentrations detected. There were significant levels of non-H₂S odorous compounds detected in those samples (dimethyl disulfide [DMDS] and dimethyl sulfide [DMS]) potentially contributing to the elevated odor concentration. Since the new aeration basins had only recently been started when the sampling was conducted, CH2M HILL believes that they are not a significant source of off-site odor impacts. To confirm this, it is recommended that the City resample the aeration basins when all the new basins are optimized.

Nasal Ranger Sampling

As part of both the Jerome Meter and Flux Chamber sampling events, additional sampling was conducted at the WWTP fenceline to determine H₂S and odor concentrations at the property line. A new product by St. Croix Sensory, Inc., called a Nasal Ranger Field Olfactometer, and shown on Figure 12, was used to determine the ambient odor dilution-to-threshold (D/T) values at the fenceline. This nasal organoleptic instrument directly measures and quantifies odor strength in the ambient air using the principle of mixing odorous ambient air with odor-free filtered air in discrete volume ratios. The user's nose is placed firmly inside the nasal mask against the replaceable "comfort seal". The user inhales through the nasal mask at a comfortable breathing rate. The ambient air can pass through an activated carbon filter to remove the odor and then mixed with the odorous ambient air in a discrete volume ratio. The mixed air will pass to the nose. The user chooses dilution factor by adjusting the rotational position of the Nasal Ranger D/T Dial to determine the orifice size and, therefore, the volume of odorous air that enters through the selected orifice.

The fenceline sample locations are identified on Figure 13. A summary of the fenceline sampling results is provided in Table 4, with the detailed results included in Appendix F. When measuring odor strength, the higher D/T number, the stronger the odor. The area to the west of the treatment plant near the Headworks Building had the most significant odors at the fenceline. On a few occasions the odors were found to be at or above 7 D/T, which is in exceedence of the state standard for residential areas. The highest odors detected along the fenceline were detected directly north of the digesters.

TABLE 4
Summary of Loveland WWTP Fenceline Sampling Results

Number Location Description		H ₂ S (_F	opm)	Odor	(D/T)
Number	Location Description	Average	Max	Average	Max
1	Fenceline at South Entrance to Headworks	0.123	0.620	4.1	15.0
2	Fenceline at manhole in driveway	0.263	1.500	4.2	30.0
3	Fenceline at rock in driveway	0.077	0.390	1.8	7.0
4	Fenceline at road sign	0.084	0.280	2.7	7.0
5	Main gate	0.039	0.280	3.3	30.0
6	1/2 way up hill from gate	0.039	0.300	1.3	4.0
7	NW corner of fenceline	0.034	0.160	1.9	7.0
8	Fenceline behind power pole	0.030	0.110	1.1	2.0
9	Fenceline past last tree (from W)	0.036	0/450	2.2	15.0
10	Fenceline 1/2 way b/w tree and sludge tanks	0.019	0.140	3.5	30.0
11	Fenceline behind sludge tanks	0.012	0.063	1.3	2.0
12	Fenceline b/w sludge tanks and digesters	0.014	0.130	1.9	15.0
13	Fenceline due East of digester (north of flare)	0.005	0.079	1.0	1.0
14	Canal at road	0.024	0.140	1.3	2.0
15	Canal at 1st break in trees	0.016	0.180	1.5	7.0
16	Canal just past trees	0.020	0.119	3.2	30.0
17	Canat due N of light at sludge tanks	0.016	0.120	1.1	2.0
18	Canal b/w sludge tanks & digesters	0.007	0.066	1.7	7.0
19	Canal at NE corner of plant	0.005	0.021	1.3	2.0
20	Fenceline behind digesters	0.016	0.150	4.7	30.0

Date sampled: October 7-23, 2003 and June 2, 2004

Baseline Model

The baseline odor modeling assessment used emission rates obtained from sampling performed during 2003 and 2004. Several sampling methods were used to obtain reliable and comprehensive odor data, including the EPA's flux chamber for area sources. The sample analyses included measurements of field H₂S, field ammonia, lab reduced sulfur compounds, and odor panel data. The sampling results indicate that the odor from the Loveland WWTP is caused by more than just H₂S. To account for the combined effect of all odorous compounds, odor was modeled instead of just H₂S, ammonia, or reduced sulfur compounds.

Technical Approach

The odor modeling approach is described in the following section, which provides detailed information about the procedures used in the odor modeling analysis.

Odor

Odor is measured in four different ways:

- Intensity (strength)
 - Measures odor intensity as a volumetric dilution ratio final diluted volume at the odor threshold (Vf) to the initial sample volume (Vs) or D/T
- Butanol Equivalence (Intensity)
 - Measures odor intensity as an equivalent concentration of n-Butanol, volumetric parts per billion (ppbv)
- Character ("what does it smell like?")
- Hedonic Tone (degree of unpleasantness)

Odor strength quantifies the degree of odor perception of a whole air sample. Threshold is defined as the point where the odor is barely perceptible to the sampler. The number of dilutions of pure air required to barely perceive the odor then indicates the strength of the sample. The threshold is thus termed dilutions-to-threshold (D/T). Relatively speaking, the higher D/T number indicates the stronger the odor.

To measure odor, air samples are typically collected using a portable air pump and stored in inert sample bags. The sample bags are taken offsite and analyzed by odor specialists using an odor panel comprised of various people that smell the sample. When half the panel does not detect the odor, that is the D/T level reported. Table 5 describes various D/T levels and human reactions.

TABLE 5
D/T Ratio and Typical Human Reactions

D/T Ratio	Description	Reaction
0 Human Threshold ¹	The lowest concentration at which the average noses can detect the odor.	Human nose can sense the odor and determine a difference from normal background odors. The odor is not alarming at this level, just barely noticeable.
4	The odor is very slightly noticeable above background odors.	Human nose can sense the odor and determine a difference from normal background odors. The odor may cause slight discomfort to some humans, but typically it's not alarming or at nuisance levels.
7	The odor is very slightly noticeable above background odors.	Human nose may determine the source if the nose has previously experienced higher strengths of the particular odor compound. The odor may cause slight discomfort to some humans, but typically it's not alarming or at nuisance levels.
20	The odor is slightly noticeable above background levels.	The human nose may determine the source, regardless if it has been previously detected or not (may cause a slight nuisance odor reaction ² with some individuals). Typically odors lower than this ratio do not cause odor complaints.
50	The odor is noticeable above background levels.	The human nose can determine the source and may result in a nuisance odor reaction with some individuals.
100 (plus)	The odor is extremely noticeable above background levels.	The human nose can detect the source, and typically results in a nuisance odor reaction.

Notes:

1. Odor threshold concentrations for typical odor causing compounds are ("ppmv" = parts per million measured volumetrically):

 $H_2S = 0.0008 \text{ ppmv}$

Sulfur/mercaptan compounds = 0.001 ppmv

Ammonia = 2.4 ppmv

2. A nuisance odor reaction typically causes one or several of the following reactions: public complaint, extreme discomfort, sleeplessness, agitation, and/or a strong motivation to stop the odor impact.

As with most wastewater treatment plants, the Loveland WWTP modeling assessment used the odor intensity in the unit of D/T to measure the odor because it is a comprehensive parameter to quantify the odor impact resulting from all kinds of compounds. The odor thresholds used in this model analysis was 7 D/T, required by the State of Colorado regulation for predominantly commercial or residential land, as described earlier in this report.

Emission Sources

Odor emission sources must be defined in terms of their odor emission rates and physical characteristics to be modeled. Sources can be characterized as point, area, or volume sources. Point sources include exhaust air through a duct or vent at a known rate. The height of the release, outlet diameter, exit velocity, and exit gas temperature can be readily

defined. Area sources are open tanks or basins. Emissions are released from the liquid surface. Area sources are defined by their release height, width and length of surface area, and angle of rotation. Volume sources are releases that are not easily defined as point or area sources. The physical parameters, actual sampling data, and calculated emission rates for each plant odor source are summarized in Appendix G. The sources modeled are shown in Table 6.

TABLE 6
Summary of Loveland WWTP Odor Sources Included in the Modeling Effort

Area Sources	Point Sources	Volume Sources
Rectangular Area Sources: Aerated Grit Chamber Old Aeration Basin New Aeration Basin East Digester Junction Box West Digester Junction Box Screw Pump Primary Effluent Wetwell Trickling Filter Effluent Channel Primary Splitter Box Aerated Grit Effluent Channel	Headworks Odor Control Exhaust Flare	 Grit/Screening Trucks Loading Digester Boiler Room Vent* DAFT Door DAFT Window
Circular Area Sources: East Trickling Filter West Trickling Filter East Primary Clarifier West Primary Clarifier Biosolids Truck Loading Hatch 1 Biosolids Truck Loading Hatch 2 Biosolids Truck Loading Hatch 3 Anaerobic Digester Cover Ring Final Clarifier 1		

^{*} Digester boiler room vent does not have sufficient vertical momentum to be considered a point source. It tends to create mixing and turbulence around boiler box. Therefore, it is considered a volume source.

The site plan drawings (LL05c01.dlv and LL05c02.dlv) were used as the base map to locate the individual sources when setting up the modeling input files. These site plan reference drawings were developed in 2003 from the recent Step Feed, Ultraviolet (UV) Disinfection, and Secondary Electrical Improvements project. The Universal Transverse Mercator (UTM) coordinate system was used to orient each source.

Emission Calculations

For sources near the entrance to the plant (grit handling and primary clarifiers), H₂S measurements are strongly correlated to odor threshold levels. Odors from aeration basins and solids handling areas are more complex and are not accurately characterized by H₂S alone. Odorous compounds from these process areas include amines, reduced sulfur compounds, mercaptans, and fatty acids. These compounds have high odor intensities even without H₂S present. Therefore, the modeling was run based on the odor intensities (D/T)

emission, expressed as odor units per second (OU/s), which is the equivalent of D/T \times m³/s. From the perspective of dispersion model, the odor unit is equivalent to the mass of any odor compound, like H₂S, in the unit of gram.

To obtain the appropriate odor emission data for the model input, the following steps were conducted:

1. Convert H₂S data obtained from sampling to odor threshold data (D/T) using H₂S -to-odor unit correlation developed as part of the Orange County Sewer District (OCSD) Odor Control Master Plan:

```
1 ppbv H_2S = 2.3355 Odor units (D/T)
```

2. For stack samples, the odor emission rate is determined by stack flow rate:

```
OU/s = (D/T) \times (exhaust flow rate, ft^3/min) \times (m^3/35.34 ft^3) \times (min/60s)
```

3. For non-aerated area sources, the sweep air flux through the flux chamber is 5 L/min. The surface area of the flux chamber is 0.13 m², Therefore, the odor flux is

Odor flux
$$(OU/min/m^2) = (D/T) \times (5 Lpm/1000) / (0.13 m^2)$$

And the odor emission is:

```
Odor Emission (OU/s) = (Odor Flux, OU/min/m<sup>2</sup>) x (surface area, ft<sup>2</sup>)/ (10.76 ft<sup>2</sup>/m<sup>2</sup>) /(60 s/min)
```

4. For the aerated area sources, the odor emissions from these processes is:

$$OU/s = (D/T) \times (aeration air, ft^3/min) / (35.34 ft^3/m^3) / (60s/min)$$

The emissions calculated from sampling results are presented in Appendix G.

Model Selection

Dispersion modeling is a mathematical method that relates emissions from a source to ambient air concentrations located downwind. The dispersion model selected for this analysis was the Industrial Source Complex – Short Term Version 3 (ISCST3). The model is recommended by EPA for use in demonstrating compliance with ambient air quality standards. It is designed to assess the combined impacts from multiple sources and source types in simple and intermediate terrain.

Two other models can be used for odor dispersion modeling, AERMOD and CALPUFF. AERMOD is also a Gaussian plume model. The dispersion coefficients are based on boundary layer theory rather than empirically derived from sampling data. AERMOD uses a continuous turbulence spectrum whereas ISCST3 uses discrete stability categories. Validation of the model has been done with data sets with sampling data averaged over a one-hour time period. Although proposed by EPA as a replacement for ISCST3, it has not been used for odor impact assessments.

The CALPUFF model is a Lagrangian puff model. It is approved by EPA for use in long-range transport studies. The model can be used for short transport times. The meteorological data needed to run the model can be a single meteorological station (as

would be the case for ISCST3) or developed from several stations (as would be required for long range transport studies). Use of the CALPUFF model for odor studies has been limited due to the large amount of input data required and the little, if any, benefit over ISCST3. For the Loveland WWTP, the ISCST3 output was adjusted using the power law to represent puff conditions, which is the same method by which CALPUFF simulates puff conditions.

A comparison of the ISCST3, AERMOD and CALPUFF models was conducted by Diosey¹. This comparison showed that maximum predicted impact from a typical wastewater treatment plant was similar for ISCST3 and CALPUFF run in the refined mode. Predicted impacts for AERMOD were a factor of 24 lower than ISCST3 and a factor of two lower for CALPUFF run in the screening model. Therefore, ISCST3 results are the most conservative of the odor dispersion models used in the air quality industry. The other two models were not used for the Loveland WWTP because CALPUFF is very complicated with much longer run times resulting in little benefit and AERMOD is not as conservative as ISCST3.

Model Inputs

The ISCST3 model has several required inputs. The control options (CO) define how the model is to be executed. Many of these control options are default values or options EPA requires for regulatory compliance. The source options (SO) define the physical source parameters and emission rates. As discussed above, different types of sources (point, area and volume) have different physical characteristics. Large buildings close to the stacks or other point sources can radically influence the dispersion pattern, which is known as building downwash. There is an algorithm developed in ISCST3 to estimate the impact of the building on the dispersion of the plume, which is included in this section. The receptor grid (RE) array needs to be defined or the receptor coordinates can be input to define the discrete receptors of interest. Receptors are the off-site locations downwind where ambient concentrations are predicted. The meteorological (ME) data and terrain data to be used in the modeling analysis are defined next. The output (OU) options define how the resulting concentrations are to be summarized and presented in the output file.

The shortest averaging period that can be selected to present the modeling results is one hour because the meteorological data contains only one value for each hourly period. One-hour averaging tends to reduce peak values. Impacts over the 1-hour period tend to round out any puff conditions. From experience, puffs of odor in as little as 3-minute durations can cause odor complaints. Therefore, a power law correction is used to allow an assessment of puff conditions that may occur. The irregular isopleths are due to the variable nature of the wind direction, wind speed, and stability categories. The power law affects only the magnitude of the predicted impact.

As a conservative assumption, the model output is interpreted as a 1-hour average concentration. To make comparisons to odor thresholds with shorter averaging periods (such as five minutes), the following relationship is used:

Diosey, Phyllis G., Maureen E. Hess, and Larraine Farrell, Evaluation of Alternative Dispersion Models for Use in Odor Management, WEFTEC 2002 75th Annual Technical Exhibition and Conference, Conference Proceedings, WEF, Alexandria, VA

 $C_1 = C_0 * (t_0 / t_1)^p$

Where:

 C_0 = initial (1-hour) concentration with an averaging time, t_0 (60 minutes)

 C_1 = desired concentration with an averaging time, t_1 (5 minutes)

p = power law factor of 1/5

The 1/5 power law factor has been demonstrated as the peak-to-mean scaling factor during field and wind tunnel studies performed at wastewater treatment plants and low level releases (Porter et al., 1994). Applying a peak-to-mean scaling factor provides a conservative estimate of short-term puff impacts when demonstrating compliance with ambient odor thresholds. For this odor study, the model runs completed for each of the five years (1999 to 2003) produce the 1-hour maximum concentration based on a 1-hour (or 60-minute) average. To obtain the 5-minute average concentration, the 60-minute concentration is multiplied by $1.64 ((t_0/t_1)^p = (60/5)^{1/5} = 1.64)$. The probability of odor complaints depends on odor intensity and number of hours that the odors exceed the determined acceptable threshold. By measuring surface and upper air in short averaging periods, the magnitude and duration of peak intensities is better quantified.

Meteorological Data

Two types of meteorological data are used to characterize the dispersion environment – surface meteorological data and mixing height data. The surface meteorological data used in this modeling assessment were measured from the Fort Collins-Loveland Airport, which is the closest airport to the Loveland WWTP. The surface data defines the wind speed, wind direction, temperature, and cloud cover used in this analysis. The mixing height data had to be derived from upper air measurements collected at the Stapleton International Airport site, which was the closest location that had all the necessary mixing height data. Mixing height data defines the depth of the surface layer that a plume will disperse. Both surface and upper air data for the 5-year period from year 1999 to year 2003 were used in the screening level model analysis. Then, the year that resulted in the highest off-site impacts (2003) was used in all the modeling described below. The data was purchased through the National Climatic Data Center in Asheville, North Carolina. The ISC-ready meteorological data files were prepared using the PCRAMMET preprocessor program in accordance with EPA procedures.

Terrain Data

Typically, the terrain files used in the dispersion modeling analysis are obtained from the U.S. Geological Survey (USGS) 7.5-minute Digital Elevation Model (DEM) data sets. These terrain files normally contain 30-meter intervals. Based on the terrain data, the dispersion modeling program can calculate the elevations at receptors and odor sources. In this modeling analysis, plant-specific terrain information was used because it has the smaller intervals (10 meters) and is more accurate and up-to-date for the plant location. The terrain elevations were obtained from the topographical information provided by the City using the GIS program for all the defined receptors and odor sources, which were then input back to the dispersion model.

Model Runs

The baseline odor condition at the Loveland WWTP included all the treatment processes units typically on-line in the summer. ISCST3 predicts 1-hour average pollutant concentrations. However, odor nuisances are most often associated with puff conditions, or exposure times on the order of seconds or minutes rather than hours. Averaging over an hour has the effect of smoothing out the concentration peaks. Therefore, the 1-hour concentrations predicted by ISCST3 were converted to peak 5-minute concentrations (using the power law). This reduces the number of data points analyzed by the model from one a minute to one every five minutes. Typically, the shorter the averaging period means the more conservative the values because fewer data points are averaged. The peak 5-minute concentrations are greater than the 1-hour average concentration and better represent puff conditions. The peak 5-minute concentrations of all the model runs were compared to a fenceline threshold of 7 D/T.

A baseline model was created from both sampling events. A review of the emissions in Appendix G shows that the odor emissions obtained from the H₂S data from the Jerome meter sampling are generally higher than those obtained from the flux chamber sampling. The difference may be caused by the following reasons:

- Seasonal differences between the sampling events. The Loveland WWTP typically
 experiences more odor complaints in the late fall.
- The Jerome sampling results used in the emission calculations were the highest odor that occurred at each process during all 30 sampling times, over a period of 21 days. In reality, not all the highest odor events at each process will occur at the same time. Therefore, this is considered a worst-case condition. The flux chamber sampling was performed on a single day, which may not have captured the worst odor event during the summer. Therefore, it is considered as an average or one-day condition.
- The conversion relationship between odor (D/T) and H₂S used is specific to the Orange County Sanitation District (OCSD) wastewater treatment plant and may overestimate the odor concentrations at other plants. OCSD completed an extremely thorough odor control study in 2001. The data generated provided a good correlation for converting H₂S emissions to D/T that is widely used. A similar correlation factor could not be estimated for Loveland WWTP because the odor concentrations were insensitive to H₂S concentrations reported during the flux chamber sampling. The odor concentrations were not correlated to H₂S concentration.

Two baseline models were performed and compared.

- Worst Case Baseline: Model input based on Jerome meter sampling data
- One-Day Baseline: Model input based on flux chamber sampling data

Results of Baseline Odor Modeling

Odor impacts can lead to complaints when the off-site concentrations are significantly above the odor threshold or occur at or near odor threshold levels with regular frequency. Odor modeling data were analyzed from five aspects:

- Duration of odor above the threshold at off-site receptors
- Maximum source contribution to off-site impacts and extent of the impacts
- Off-site D/T distribution at certain receptors
- Off-site impact distribution by time of day at certain receptors
- Meteorological conditions when the maximum impact occurred at certain receptors

Duration of Odor Above Threshold

Figures 1 and 2 show the number of hours when odor levels are above the odor threshold at each receptor for the Worst-Case and One-Day sampling, respectively. The area inside the circle, or isopleth, is the area impacted at the number of hours shown.

Worst-Case Baseline (Jerome Meter Sampling)

In the worst-case baseline (based on the Jerome meter sampling), the odor impact from all the existing sources at Loveland WWTP based on a 5-minute averaging period with an odor standard of 7 D/T is shown in Figure 1. There is a significant off-site area that can perceive the 7 D/T or higher odor levels greater than one percent of the time. The residential area northwest of the plant could potentially perceive the odor that is higher than 7 D/T up to 500 hours a year. The residential area further north of the plant could be impacted up to 50 or 100 hours per year. The isopleths are centered at the north end of the plant, which means the highest odor impact occurs at that area. This could be explained by the observed prevalent wind direction that will bring the odor from those big odor sources, such as the headworks, aerated grit chamber, and other sources, to north and northeast areas.

Figure 3 shows the receptors where the highest maximum 5-minute D/T occurred at the plant (Receptor A) and where the highest exceedence occurred at the plant (Receptor B).

One-Day Baseline (Flux Chamber Sampling)

A similar isopleth was created for the one-day baseline (flux chamber sampling) modeling results, shown in Figure 2. This Baseline represents a typical day without much noticeable odors in the community surrounding the Loveland WWTP. It shows a much smaller impact area focused on the north end of the plant. The highest odor impacts are more likely due to two areas - aeration basins/grit chamber area and digester/boiler room area.

Maximum Source Contribution to Off-Site Impacts and Extent of the Impacts

The highest off-site odor impacts from both baseline models were tabulated by source groups to assess their contribution to off-site impacts. Table 7 presents the maximum 5-minute odor impacts and maximum annual average odor impacts expressed as D/T for each major process area (source group). The ratio of the maximum annual odor to the maximum 5-minute odor, peak-to-mean ratio, is a parameter indicating the frequency of the

maximum odor occurrence, and is also shown in the table. Note that the maximum source group impacts are not additive because they occur at different times and locations.

For the worst-case baseline, the maximum combined 5-minute odor impact from all the sources was 1,128 D/T, which is significantly higher than the odor threshold of 7 D/T. The maximum combined 5-minute odor impact from the digester boiler room vent was 1,000 D/T. The digester boiler room vent is the most significant contributor to the off-site odor impact in terms of strongest odors. The next source having the highest maximum 5-minute odor impact is the aerated grit chamber. It generated 857 D/T of maximum 5-minute odor impact. The DAFT is the next source having the maximum odor impact of 233 D/T, followed by the trickling filters. The remainder of the sources that had maximum 5-minute odor impact higher than 7 D/T include screw pumps, primary clarifiers, flare, headworks building door, and aeration basins. The ratio of maximum 5-minute odor to the maximum annual odor at the digester boiler room vent was only 56, suggesting the mean impact from this source is almost as significant as the peak impact. While the peak-to-mean ratio for the aerated grit basin was 242, suggesting that that odor source is less chronic and more acute in nature.

For the One-Day baseline modeling, the maximum combined 5-minute odor impact from all sources was 136 D/T, about one eighth of the impact of the Worst-Case baseline. The aeration basins are shown as the biggest contributor to the off-site odor impact for the maximum 5-minute odor, while the digester boiler room vent is still the biggest contributor on an average annual basis.

The prioritization of the odor sources was based on the maximum 5-minute odor strength (D/T) and the peak-to-mean ratio analysis from the Worst-Case baseline model. Figure 4 summarizes the ranking of the major odor sources at the plant. The remainder of the analyses conducted are focused on the Worst-Case baseline since those odor impacts are more consistent with the odor complaints from the surrounding community.

Off-Site D/T Distribution at Certain Receptors

A more detailed analysis of odor impacts was performed at Receptors A and B (see Figure 3) for the worst case baseline. Receptor A is the location where the highest maximum 5-minute D/T occurred based on the 2003 modeling. Receptor B is the location where the maximum exceedence occurred based on the 2003 modeling.

Figure 14 shows that 26 percent of the time (2,278 hours) the odor impact from all the sources at Receptor A was above 7 D/T. Within this time, 11 percent of the time the odor impact was above 100 D/T (964 hours) and 11 percent (964 hours) when the odor was between 20 D/T and 100 D/T. During the remainder of the time (4 percent, 350 hours), the odor was between 7 D/T and 20 D/T. Approximately 74 percent of the time during a year, Receptor A received an odor impact less than 7 D/T.

The odor exceeded 7 D/T for about 2,366 hours per year (27 percent of the time) at Receptor B. Among this time, only one percent of the time the odor impact was above $100 \,\mathrm{D/T}$ (88 hours), and eight percent (701 hours) when the odor was between $20 \,\mathrm{D/T}$ and $100 \,\mathrm{D/T}$. During the remainder of the time (18 percent, 1,577 hours), the odor impact was between 7 D/T and $20 \,\mathrm{D/T}$.

TABLE 7
Maximum 5-Minute and Annual Average Odor Impacts from Existing Sources at Fenceline Receptors

~~~	1	rst-Case rome Me		(	One-Day Flux Chan	Baseline nber Data)
Source Group	Max 5-min D/T	Avg Annual D/T	Peak-to-Mean (5-min D/T)/ (Annual D/T)	Max 5 min D/T	Avg Annual D/T	Peak-to-Mean (5-min D/T)/ (Annual D/T)
All Source	1128	20.3	55	136	2.2	61
Digester boiler room vent	1000	18.0	56	67	1.2	56
Aerated Grit Basin	857	3.5	242	71	0.3	238
DAFT	233	8.0	293	50	0.2	293
Trickling Filter	174	1.3	132	70	0.5	133
Screw Pumps	163	1.5	107	18	0.2	107
Primary Clarifier	146	0.7	197	49	0.3	159
Flare	79	0.6	134	3	0.0	135
Headworks Door	30	0.5	63	3	0.0	63
Aeration Basins	28	0.4	69	81	1.0	81
Headworks Building Exhaust	5	0.07	70	1	0.0	69
Digesters	1	0.0	98	1		
Biosolids Loading	0	0.0				

Notes:

Predictions based on 2003 surface meteorological data from Fort Collins-Loveland Airport.

Model output was converted to 5-minute average concentrations using a factor of 1.64.

### Off-Site Impact Distribution by Time of Day at Certain Receptors

The distribution of off-site impacts by time of day over a year at Receptors A and B are shown in Figure 15. Each slice of the pie chart represents the percentage of the exceedences over 7 D/T that occurred during a 4-hour interval of a day in 2003. At Receptor A, approximately 75 percent of the exceedences over 7 D/T occurred between 9 PM and 8 AM, during which time most people are in the hours sleeping. Among these nighttime exceedences, , 21 percent occurred during 9 PM to 12 AM; 26 percent occurred during 1 AM to 4 AM; and 28 percent during 5 PM to 8 PM, respectively. At Receptor B, approximately 67 percent of the exceedences over 7 D/T occurred between 9 PM and 8 AM. In summary, more odor intensities above 7 D/T occurred in the evening and night between 9 PM and 8 AM at Receptor A, and more noticeable odor events occurred between 9 AM to 8 PM at Receptor B.

# Meteorological Conditions when the Maximum Impact Occurred at Certain Receptors

Odor impacts, to a large extent, depend on meteorological conditions such as wind direction and wind speed. The meteorological conditions at the specific times in 2003 when the maximum impacts were predicted to occur at Receptors A and B are identified in Table 8. There are a lot of similarities between the meteorological conditions at these two receptors when the maximum impact (maximum D/T) occurred. The maximum impacts at these two receptors both occurred in winter late night, when the temperature was very low. The wind speeds were both 1.03 meters per second. In addition, both occurrences occurred during stability class F, which is the most stable and tends to have the least turbulence and mixing causing the odors to be higher closer to the fenceline. At receptor A, the wind blew from the southwest to northeast when the maximum impacts occurred. At receptor B, the wind blew from the southeast to the northwest when the maximum impacts occurred. This is consistent with the relative location of the receptors and the plant processes since the wind carried the odor emitted from the majority of wastewater treatment processes to the receptors.

TABLE 8
Meteorological Conditions When The Maximum Impact Occurred

Receptor	Date	Hour	Temporature (°F)	Wind Speed (m/s)	Wind Direction	Stability Class
Α	01/16/2003	2 AM	18	1.03	From southwest	F
В	11/13/2003	10 PM	34	1.03	From southeast	F

# **Odor Control Modeling**

# **Technical Approach**

Four odor control scenarios were modeled in this analysis to investigate the effect of positively controlling the odor sources. The odor control improvements either eliminate the identified big odor sources completely, such as the trickling filters, or convert the major odor sources into the odor control scrubbers that emit significantly less odor, such as the chemical scrubber treating the headworks and grit chambers at Stage 3. The major sources controlled were selected based on the prioritization in baseline modeling. The four odor control scenarios modeled are:

**Stage 1** – Discontinue the operation of the trickling filter as a result of the aeration basin improvement project.

The construction project that is currently being done at the plant includes converting the existing aeration basin to a step-feed process, and adding more aeration basin volume. After these process changes have been completed, the secondary treatment capacity will be sufficient to treat the plant flow without the use of the trickling filter. Since the trickling filters are the fourth biggest odor source based on the baseline modeling results, elimination of trickling filters will reduce the off-site odor impact from the plant.

Stage 2 – In addition to Stage 1, relocate the digester boiler room HVAC intake vent to reduce the odor emission from the digester boiler room vent.

The current sampling results show the maximum H₂S concentration measured at the digester boiler room vent is 17 parts per million (ppm), which is comparable to the H₂S concentration in the digester gas. The normal H₂S concentration from the similar building (such as solids building) HVAC vent is between 0.003 ppm and 0.08 ppm. The high H₂S concentration from Loveland WWTP boiler room is due to the HVAC intake location directly between the digester overflow weirs. The HVAC system is pulling in fugitive odor emissions from the digesters and overflow weirs, circulating through the HVAC system, and blowing the odors directly towards the residential areas with a flowrate of 2,700 cubic feet per minute (cfm). Relocating the HVAC intake vents could bring the H₂S level down to the typical HVAC vent H₂S level. Therefore, in this modeling analysis, it is assumed that the digester boiler room vent emits 0.05 ppm of H₂S after the HVAC intake is relocated. The ventilation air flow in this room is 2,700 cfm. Therefore the odor emission from the vent is reduced to 150 OU/s.

Stage 3 – In addition to Stage 2, the aeration grit chamber would be covered with a new carbon odor control unit installed to treat the air from grit chamber.

The major assumptions made in Stage 3 modeling include:

1. The ventilation airflow from the aerated grit chamber is selected based on 6 air change per hour (ACH) in the air space of the grit chamber. This would required an

airflow of approximately 250 cfm, which is an increase from the current aeration air of 100 cfm.

- 2. The new carbon unit has 95 percent odor removal efficiency.
- 3. The carbon unit discharge stack diameter is about 4 inches to allow an appropriate exit velocity (approximately 3,000 fpm).

Stage 4 – In addition to Stage 3, provide odor control for the entire headworks building as part of the new or modified headworks facility currently listed in the City's CIP for the Loveland WWTP. Headworks replacement would include replacing the screw pumps, aerated grit basins, and screening processes with new processes, all contained within a building. In addition, the influent collection well would also be contained for odor control purposes. The air from this facility would be treated in a new chemical scrubber followed by a bioscrubber or carbon scrubber at the same location as the carbon unit modeled in Stage 2, to the east of the existing headworks building. Stage 4 would provide odor control for a new headworks building or a modification of the existing headworks building.

The major assumptions made in Stage 4 modeling include:

- 1. Ventilate the entire headworks building at 12 ACH, so the air flow is approximately 13,000 cfm.
- 2. The new chemical scrubber followed by a bioscrubber or carbon scrubber has 99 percent odor removal efficiency.
- 3. The chemical scrubber discharge stack diameter is about 2.5 feet to allow an appropriate exit velocity (approximately 3,000 fpm).

Stage 5 – In addition to Stage 4, provide odor control for the DAFT by installing a new carbon unit nearby.

- 1. The ventilation airflow from the DAFT is based on 12 ACH in the DAFT dome. This would required an airflow of approximately 800 cfm, which is higher than the current ventilation airflow of 700 cfm.
- 2. The new carbon unit has 95 percent odor removal efficiency.
- 3. The carbon unit discharge stack diameter is about 8 inches to allow an appropriate exit velocity (approximately 3,000 fpm).

**Stage 6** - In addition to Stage 5, cover the primary clarifiers and provide the odor control by installing an dedicated odor control chemical scrubber.

- Ventilate the headspace of the two primary clarifiers and the effluent well at 6 ACH.
   Assuming 4 feet of free board, the ventilation air would be approximately 3,800 cfm for two 78-foot diameter primary clarifiers and 200 cfm for the effluent wet well.
- 2. The new chemical scrubber would have 95 percent odor removal efficiency.
- 3. The chemical scrubber discharge stack diameter is about 16 inches to allow an appropriate exit velocity (approximately 3,000 fpm).

317516.DR

Stage 7 – In addition to Stage 6, cover the aeration basins and provide the odor control by installing an dedicated odor control chemical scrubber for the aeration basins. In addition, install fixed covers for each digester with a gas collection system so that there are no odor emissions from the digester cover perimeters.

- 1. Ventilate the headspace of the two aeration basins at 6 ACH. Assuming 4 feet of free board, the ventilation air is about 8,600 cfm, which is slightly higher than the aeration air. The odor control chemical scrubber is sized based on 8,600 cfm.
- 2. The new chemical scrubber has 95 percent odor removal efficiency.
- 3. The carbon unit discharge stack diameter is about 22 inches to allow an appropriate exit velocity (approximately 3,000 fpm).

The conditions represented in these seven odor control scenarios are shown in Table 9. The check marks indicate which proposed odor control improvements (shown in rows) were modeled in each control scenario (shown in columns). The odor control modeling was performed using the same protocols as Baseline modeling, such as the emission sources, the emission rates, the model selection, and the meteorological data. The odor threshold of 7 D/T was modeled. Equipment cut sheets for each recommended type of odor control are included in Appendix H.

TABLE 9
Conditions Represented in the Odor Control Modeling

Odor Control Project	Description	Stage 1	Stage 2	Stage 3	Stage 4	Stage 5	Stage 6	Stage 7
Trickling Filters	Discontinue the use of trickling filters.	✓	✓	✓	✓	<b>√</b>	<b>√</b>	<b>√</b>
Digester Boiler Room Vent	Eliminate the fugitive odors being collected in the HVAC exhaust		$\checkmark$	$\checkmark$	$\checkmark$	$\checkmark$	$\checkmark$	$\checkmark$
Aerated Grit Chamber	Cover aerated grit chamber and install a new carbon unit to treat the air from grit chamber (95% odor removal)			✓	$\checkmark$	$\checkmark$	✓	$\checkmark$
Headworks Building	Ventilate new or modified Headworks building at 12 ACH. Provide a new chemical scrubber to treat the air from both the aerated grit chamber and the headworks building (99% odor removal). Replace screw pumps or cover and ventilate to the odor control scrubber.				✓	✓	✓	✓
DAFT	Maintain negative pressure inside DAFT by providing 12 ACH ventilation. Add a new carbon unit to treat the air from DAFT (95% odor removal)					✓	✓	✓
Primary Clarifiers	Cover and vent primary clarifiers to odor control scrubber (95% removal efficiency)						✓	<b>√</b>
Aeration Basins and Digesters	Cover and vent aeration basins to odor control scrubber (95% removal efficiency). Provide odor control for digesters with fixed roof tanks.							✓

## **Results of Odor Modeling with Control Scenarios**

#### **Duration of Odor Above Threshold**

The results of the odor control modeling are shown in Figures 16 through 22, as described below, by showing the number of hours when odor levels are above the odor threshold for each control scenario. These exceedences are not actual exceedences, but worst-case predictions based on the modeling analysis conducted.

The odor exceedences above 7 D/T from all the plant processes under Stage 1 is shown in Figure 16. Compared with the current condition (Baseline, Figure 1), the isopleths under Stage 1 showed the similar shape, but slightly reduced exceedences.

Under odor control stage 2 (Figure 17), the odor impact was reduced significantly compared with the baseline. The exceedence above 7 D/T at the WWTP's north end was reduced from

approximately 1,500 hours per year at Baseline to approximately 1,000 hours per year with Stage 2. The location where the highest exceedence occurred within the plant moved from the east boundary of the plant to the west boundary of the plant, and the highest exceedence was reduced from approximately 2,428 hours per year at Baseline to approximately 1,700 hours per year for Stage 2.

The odor impact of the plant processes with the odor threshold of 7 D/T during Stage 3 and Stage 4 are shown in Figure 18 and Figure 19. By controlling the odor emission from the aerated grit chamber and the Headworks, the odor impact was reduced further. The location where the highest exceedence occurred within the plant was on the west plant boundary. It was reduced to 1,400 hours per year under Stage 3 and 970 hours per year under Stage 4. Figures 20 and 21 show the overall impact of the plant during Stage 5 and Stage 6, respectively. Odor control the DAFT under Stage 5 had the significant improvement on the off-site odor impact. The 50-hour –per year isopleth was reduced to a fairly small area around the northern end of the plant. The highest exceedence on the plant boundary was about 700 hours per year. Covering and odor controlling the primary clarifiers under Stage 6 further reduced the off-site odor impact. Only at a limited area at the northwestern corner of the plant can people perceive the odor stronger than 7 D/T (less than 50 hours per year).

Controlling the odor emissions from the aeration basin and digesters under Stage 7 (Figure 22) reduced the off-site odor to an almost non-detectable level at most of the areas. The rare odor impact that is above 7 D/T only occurred at the northwestern corner of the plant.

Although, these seven odor control stages will meet the odor control goal of odors less than 7 D/T 99 percent of the year, it is not required to implement all seven stages to meet the plant's odor control goals. CH2M HILL recommends that the City plan to incorporate Stages 1 through 5 in their current CIP. It is anticipated that this level of odor control will meet the proposed odor control standard, given the conservative nature of the analysis. At each stage, the City should conduct additional sampling and monitoring to see if more improvements are required.

#### **Maximum Source Contribution**

The maximum off-site odor impacts are summarized by process unit from the results of odor control modeling as well as the baseline modeling. Table 10 lists the maximum 5-minute odor impacts and annual average odor impacts, expressed as D/T, for the major odor sources controlled and the new odor sources –chemical scrubbers and carbon units.

 TABLE 10

 Maximum 5-Minute and Annual Average Odor Impact (D/T) from the Entire Plant for Odor Control Scenarios

	-70000470000000000000000000000000000000	All	Digeste Roon	Digester Boiler Room Vent	Grit C Odor	Grit Chamber Odor Control	Headwo	Headworks Odor Control	DAFT	DAFT Odor Control	Primary Odor	Primary Clarifiers Odor Control	Aeratio Odor (	Aeration Basins Odor Control
Model	Max. 5- min D/T	Max. Ann. Ave. D/T	Max. 5- min D/T	Max. Ann. Ave. D/T	Max. 5- min D/T	Max. Ann. Ave. D/T	Max. 5- min D/T	Max. Ann. Ave. D/T	Max. 5- min D/T	Max. Ann. Ave. D/T	Max. 5- min D/T	Max, Ann. Ave. Drī	Max. 5- min D/T	Max. Ann. Ave. D/T
Baseline	1,128	20.6	1,000	18.0			*1105741788300				Person Dave			
Stage 1	1,110	ئ ئ	1,000	18.0			Fanty ( M. D. C. )				· Oraș publicare a construi			
Stage 2	873	6.7	2.9	0.1	Ø	0.03					thebeng trapper			
Stage 3	347	3.2	2.9	0.1	,74 T ₂ ,414h		O she are so	.,. (882)			FF. 11. 18. 18. 19. 19. 19. 19. 19. 19. 19. 19. 19. 19			
Stage 4	298	1.7	2.9	0.1			3.6	0.02		27.70				
Stage 5	154	1.06	2.9	0.1			3.6	0.02	2.5	0.023	MA 174-11-11			
Stage 6	80	0.86	2.9	0.1	integral and a second		3.6	0.02	2.5	0.023	0.5	0.0088		
Stage 7	80	0.65	2.9	0.1			3.6	0.02	2.5	0.023	0.5	0.0088	0.1	0.0014

# **Liquid Phase Treatment**

Although domestic wastewater odors are caused by a variety of organic and inorganic compounds, H₂S is normally the predominant odor-causing compound found in collection systems and at the front end of WWTPs. Liquid phase odor control strategies reduce odors by reducing the hydrogen sulfide concentration in the liquid waste stream to reduce the amount of H₂S released to the atmosphere. There are several liquid phase strategies and chemicals that are used to counter hydrogen sulfide odors. CH2M HILL completed an analysis of collection system, liquid phase treatment alternatives as part of this Odor Management Plan.

The City's wastewater collection system consists of a network of large interceptor sewers (gravity), as well as several lift stations and corresponding forcemains. The location of the major lift stations and interceptors is shown in Figure 23. Wastewater enters the treatment facility primarily by gravity, with one forcemain coming from the Southside lift station directly to the influent collection well. The four main gravity interceptors all have lift stations further upstream that are contributing to elevated sulfide levels in the wastewater. The significant lift stations are South Horseshoe, East Side (or Jellystone), South Side, and Boyd Lake. Hydrogen sulfide concentrations detected in the headworks area of the Loveland WWTP are generally higher than typically found in similar WWTP and have led to odor complaints within both the collection area and the treatment plant vicinity.

## **Technical Approach**

To help determine the cause of the elevated H₂S levels, samples of the influent wastewater were collected in conjunction with the odor sampling effort. In addition, some limited modeling of sulfide production and atmospheric H₂S levels in the conveyance system was performed. This modeling provided rough estimates of the anticipated, worst-case dissolved sulfide and H₂S emissions from each interceptor flowing into the WWTP. The model also predicted the wastewater detention times in each interceptor. The estimated concentrations from the modeling formed the basis of the comparison of liquid phase odor control alternatives.

### Sampling

In conjunction with the odor sampling, the City measured the dissolved sulfide levels of the influent wastewater and interceptors to identify potential correlation between influent wastewater concentration and odor emissions. The results of the dissolved sulfide sampling that occurred are shown in Table 11. The locations of the sampling, along with the laboratory analyses are included as Appendix I. These results represent a snapshot of conditions during the sampling period and do not necessarily show the worst-case condition. Rather, the data proves the presence of significant levels of sulfide in the collection system wastewater and points to one potential cause of odors at the plant.

TABLE 11
Summary of Dissolved Sulfide Sampling (Grab Samples)

Sample				S	ample Da	te			
Description	10/7/03	10/8/03	10/11/03	10/13/03	10/15/03	10/17/03	10/20/03	10/22/03	Average
WWTP Boyd	3.8	2.2	2.4	1.5	1.9	0.7	2.0	1.8	2.0
WWTP - SS	3.8	3.2	3.1	-	10.1	26	14	~	10.0
WWTP SE 8th	2.0	4.6	3.3	1.3	1.3	0.9	11.0	0.9	3.2
WWTP NAM	4.2	2.6	3.5	1.1	1.1	0.9	0.2	0.6	1.8
WWTP - Inf	1.8	5.8	2.7	1.1	0.7	0.7	0.3	1.0	1.8
Jellystone – Out	w	3.8	2.7		*	<b>w</b>	•	1.4	2.6
Jellystone – In/E		-	•		-	-	*	2.7	2.7
Jellystone – In/W	-	•		~	*		-	1.7	1.7
Jellystone In/S	-	-	-	-	-	-	-	1.7	1.7
M Cove – In	3.5	3.8	-	1.7	-	-	-	-	3.0
M Cove Out	-	2.6	-	2.3	-		w		2.5
Denver & 34	2.8	-	-	-		-	-	-	2.8

The sampling results indicate that sulfide generation within the collection system contributes significantly to the elevated H₂S levels at the WWTP. As part of this investigation, additional H₂S sampling was conducted with an OdaLog, an H₂S sampling device that continuously monitors H₂S concentrations. The OdaLog was installed downstream of the Auger monster, halfway down the channel sidewall in the Headworks Building. The results are shown on Figure 24. During the week of installation, the average H₂S concentration in the Headworks building was 22 ppm, with peaks greater than 100 ppm.

The wastewater interceptor sampling results indicate that the highest levels of dissolved sulfide comes from the Southside Interceptor. In addition, the frequency of the high peaks shown in the Odalog results correlates to the frequency of the Southside Lift Station cycles. However, the Southside Lift Station interceptor only represents two percent of the overall flow. The peaks are contributing to spikes seen at the WWTP, but the overall mass loading of sulfide is generated by other interceptors.

### Modeling

CH2MHILL has developed a spreadsheet model (FMSULFIDE) to estimate sulfide concentration in force mains. It is based on an algorithm published by Boon², but incorporates in-house, proprietary algorithms that allow for situations where dissolved

² Boon, Arthur, "Septicity in Sewers: Causes, Consequences and Containment", Water Science and Technology, Vol. 31, No. 7, pp 237-253, 1995

oxygen (DO) is not initially equal to zero. Under this type of situation, the time required to deplete DO is calculated and subtracted from the total residence time providing the actual reaction time available for sulfide production.

The FMSULFIDE model has been developed to facilitate sensitivity analyses through varying flow, biochemical oxygen demand ( $BOD_5$ ) or temperature data. This allows quick determinations to be made regarding sensitivity of the results to the selected input parameter values, and also helps identify any required data acquisition (e.g., field sampling). In addition, the model calculates the sulfide mass produced on a daily basis (pounds per day [lbs/day]).

A different algorithm was used to follow the fate of the sulfide in gravity sewers. This algorithm was developed by Pomeroy and Parkhurst³. The algorithm applies only to pipes flowing less than full and in which little or no DO exists. The equation accounts for sulfide generation by the slime layer, losses of sulfide due to oxidation in the stream, and sulfide emissions to the sewer atmosphere.

Both the force main and gravity sewer algorithms are combined in a model developed by CH2M HILL called the Interceptor Model. The Interceptor Model was used to estimate wastewater liquid-phase sulfide and vapor-phase hydrogen sulfide loading under various conditions and to analyze potential odor control strategies. The Interceptor Model is a predictive, not absolute, tool to determine sulfide loading in the collection system. The model predicts hydrogen sulfide dynamics in wastewater gravity and force main collection and transmission systems. The model accounts for sulfide generation, oxidation, mass transfer across the air/water interface, and liquid-phase bulk transport. Given the flow and wastewater characteristics at the upstream end of the interceptor and each collector or lateral intersection, the Interceptor Model calculates liquid and vapor-phase sulfide concentrations and vapor flow rate due to the liquid drag at downstream locations.

To develop a basis for the comparison of chemical alternatives to treat the wastewater coming to the Loveland WWTP, the main interceptors coming into the WWTP were modeled using the Interceptor Model to determine potential for H₂S generation for each interceptor. The interceptors were then prioritized as potential candidates for liquid phase treatment. The system modeled included approximately 41,400 feet of varying diameter pipe that typically handles a peak flow of 10.6 million gallons per day (mgd): 39,400 ft of gravity sewer ranges from 24-inches to 33-inches and 2,000 feet of forcemain (20-inches).

In addition to the sampling data, average annual data for the influent to the WWTP were collected and used in this analysis. A summary of the actual data used in the Interceptor Model is included in Appendix J. The following assumptions were used in the analysis:

- Chemical addition would occur only in the dry season of June through October.
- Wastewater temperature = 20.3 ° C
- $BOD_5 = 275 \text{ mg/L}$
- Target dissolved sulfide concentration = 0.5 mg/L

^{3:} Design Manual "Odor and Corrosion Control in Sanitary Sewerage Systems and Treatment Plants EPA/625/1-85/018, pp 20-24, October 1985

Table 12 contains a summary of uncontrolled peak sulfide concentrations predicted by the model for each interceptor. The Boyd Interceptor and Boyd Relief Interceptor have the highest potential for  $H_2S$  generation, due to the high concentrations of dissolved sulfide and the significant amount of flow (40 percent of total influent) from these interceptors. While the Southside Lift Station had the highest dissolved sulfide concentration in the sampling, its contribution to the total flow is relatively insignificant. Liquid phase treatment would not be as effective at that lift station for reducing overall sulfide, but could help reduce some of the spikes observed.

TABLE 12 Summary of Interceptor Model Results

Interceptor (listed in order of priority)	Dissolved Sulfide in (mg/L)	Dissolved Sulfide out (mg/L)	H₂S out (g/m³)	H₂S out (ppmV)	Туре
Boyd Interceptor	7.1	7.5	0.79	561	Gravity
Boyd Relief Interceptor	3.1	4.7	0.471	333	Gravity
Southeast 8th Interceptor	4.1	4.5	0.46	322	Gravity
Namaqua Interceptor	4	4.2	0.408	288	Gravity
Southside Liftstation Interceptor	4.2	5.1	0	0	Forcemain

This dissolved sulfide data taken from the City's collection system demonstrates that the City's system has levels significantly above what is found in a typical wastewater collection system. Liquid phase treatment is generally considered if the dissolved sulfide concentrations exceed 1.0 mg/L.

## **Description of Alternatives**

Liquid-phase odor-control strategies reduce odors by reducing the unionized or total sulfide concentration of the liquid waste stream. Although domestic wastewater odors are caused by a variety of organic and inorganic compounds, H₂S is typically the predominant odor-causing compound. A summary of these alternatives is presented in Table 13.

### **Oxygenation and Aeration**

Oxygen inhibits the growth of sulfate-reducing bacteria, chemically oxidized sulfide, and promotes aerobic growth that biologically oxidizes sulfide. At dissolved oxygen levels over 0.5 mg/L, liquid sulfide levels will typically be below 0.1 mg/L. Oxygen reacts with  $H_2S$  in accordance with the following reaction:

$$H_2S + 2O_2 \rightarrow S + H_2SO_4$$

The reaction with oxygen is very slow (half-life of about 30 minutes).

Wastewater oxygenation can be accomplished by using low-pressure compressors or blowers to inject air into open channels or basins, Venturi aspirators in combination with pumping, or pure oxygen injection into force mains. The effectiveness of air injection in controlling odors is affected by the detention time. If the system detention time is greater than 4 hours, the positive effects of oxygenation are overcome by the oxygen uptake rate of the wastewater and additional injection points will be required. Typical uptake rates for domestic sewage range from 2-26 mg/L per hour. Higher temperatures, higher soluble BOD, and longer detention times will result in higher uptake rates.

#### **Chemical Oxidants**

Liquid oxidants may be injected into the wastewater to remove sulfides. Since they are not target-specific, some of the injected oxidant will oxidize other materials within the wastestream. Thus, more oxidant must be injected than would be required to stoichiometrically react with the sulfide. Chemical oxidants used to remove sulfides from wastewater include the following:

- Hydrogen peroxide
- Chlorine
- · Sodium hypochlorite
- Potassium permanganate

#### Hydrogen Peroxide

Hydrogen peroxide ( $H_2O_2$  or peroxide) provides a source of dissolved oxygen, which reacts with sulfides at a stoichiometric rate of 1 part  $H_2O_2$  to 1 part  $H_2S$  in the following reaction:

$$H_2O_2 + H_2S \rightarrow S + 2H_2O$$

However, literature sources indicate that higher dosage rates are required due to interference with other constituents within the wastewater. In previous studies, a San Francisco Bay Area POTW found required  $H_2O_2$  dosages ranging from 5.5-8.3 parts  $H_2O_2$  per one part  $H_2S$ .

At high concentrations (50 percent or greater),  $H_2O_2$  is hazardous to handle. However,  $H_2O_2$  is an economically viable alternative only at these higher concentrations.  $H_2O_2$  also requires adequate mixing to achieve complete reaction and has a relatively long reaction time (approximately 30 minutes) compared to other oxidants. Very often,  $H_2O_2$  is injected too far upstream of the control point to allow for this relatively long reaction time.

#### **Sodium Hypochlorite**

An alternative to gaseous chlorine is sodium hypochlorite (NaOCL), also known as bleach. Household bleach, such as Chlorox brand, is approximately 5-percent sodium hypochlorite. Sodium hypochlorite used for odor control is typically delivered in concentrations between 10 and 15 percent. Hypochlorite is a strong oxidizing agent and reacts with H₂S in wastewater. It reacts stoichiometrically at a rate of 8.8 parts hypochlorite per 1 part H₂S in the following reaction:

$$4NaOCl + H_2S \rightarrow 4NaCl + H_2SO_4$$

As in the case of gaseous chlorine, hypochlorite acts as an indiscriminate oxidant. As a result, the dosage range is between 10 to 15 parts sodium hypochlorite per 1 part H₂S. One disadvantage of sodium hypochorite is that if anaerobic conditions are encountered, hydrogen sulfide will be present again. Therefore, oxidants need to be injected closer to the treatment plant.

#### **Nitrate Addition**

Nitrates do not react with the H₂S; rather, they prevent its formation. Normally, in the absence of free oxygen, sulfate-reducing bacteria will preferentially use nitrate as the terminal electron acceptor, thereby preventing the formation of H₂S. Any H₂S that has already formed is not affected because nitrates act only with the bacteria.

Nitrate is available in both liquid and dry forms from a number of sources. The various types of nitrate are sodium nitrate, ferric nitrate, and calcium nitrate. Calcium nitrate is commonly used in wastewater odor control and corrosion control applications and is available under the trade name of BIOXIDETM. This proprietary calcium nitrate solution has been tested in the City of Los Angeles's sanitary system, the Clark County Sanitation District's collection system, and the New Haven, Connecticut, interceptor systems with success. Sodium nitrate is also available under the trade name of NITRAZYMETM.

#### **Iron Salts**

Iron salts can be added to the waste stream to form a metal sulfide precipitate. This reaction binds the  $H_2S$  in solid precipitants so it cannot escape into the air. Ferric chloride salts (FeCl₃) react stoichiometrically with  $H_2S$  in wastewater at a rate of 2 parts ferric chloride per 3 parts  $H_2S$  in the following reaction:

$$2FeCl_3 + 3H_2S \rightarrow Fe_2S_3 + 6HCl$$

Iron salts, however, also act indiscriminately with other materials. As a result, the dosage ratio ranges from 7 to 20 parts ferric chloride per 1 part H₂S.

Collateral benefits of using iron salts include increased BOD and total suspended solids removal at primary sedimentation tanks, lowered wastewater phosphorus, improved solids settling in secondary clarifiers and digesters, and reductions in the amount of polymer needed for solids conditioning at dewatering. Disadvantages include the need for special handling, including eye and skin protection requirements. In addition, iron salts may have very low pH (0.5-2.5) and can corrode stainless steel, brass and aluminum pumps. Other concerns include the availability of a reliable source of chemicals.

### pH Stabilization

There are two methods of reducing H₂S-related odors using pH adjustment. One method shifts the wastewater pH so that chemical equilibrium favors non-odorous sulfide species. The other method uses a temporary, but drastic, pH shift to kill the sulfur-reducing bacteria that produce H₂S. Both methods typically rely on sodium hydroxide as their chemical agent. Only caustic shock dosing is discussed here.

### **Caustic Shock Dosing**

Shock dosing the bacteria living in the interceptor slime layer can also be used to control odor. At very high pH's, sulfate reducing bacteria activity stops. Caustic shock dosing, achieved by adding enough caustic to raise the pH of the wastewater to 13.0 or higher for 20 to 30 minutes, has been demonstrated to inactivate the sulfate-reducing bacteria for periods of 3 to 14 days. Caustic shock loading, practiced by the County Sanitation Districts of Los Angeles, found that a dose of approximately 3,125 pounds of 50-percent caustic solution per

million gallons of wastewater was required for 30 minutes to obtain odor control from shock loading.

TABLE 13
Chemical Control of H₂S and Corrosion in Sewers

Approach	Method	Objective	Advantages	Disadvantages	Typical Dosage ^a	Capital Cost ⁶	Operating Costs ^c
Improve oxygen balance in wastewater	Good operation and maintenance	Maintain good flow velocity, minimize solids deposition	No additional chemical costs	Effectiveness limited by sewer design and operating conditions	NA	NA	Included in system O&M cost
Notice and the second s	Air injection	Increase oxygen in wastewater using compressed air, venturi aspirators, or U-tubes	No chemical costs for air	Low efficiency Control limited Possible off-gassing of odors	10 mg air /mg sulfide	\$4.5/ m ³ ·d	Power, compresso r facility life cycle
	Oxygen injection	Increase oxygen in wastewater using liquid oxygen or on- site generation	High efficiency vs. air Low chemical hazard	Must be introduced in pressurized pipe (force main, sidestream or U-tube)	2 mg O ₂ /mg sulfide	\$4.5/ m³·d	\$0.75/kg O ₂ + facility life cycle
Chemical oxidation in wastewater	Sodium hypochlorite solution injection	Oxidize dissolved sulfides to sulfate	Safe vs. chlorine gas	Unstable in storage More cumbersome and costly in bulk quantity	6 mg Cl/mg sulfide	\$3/m³.d	\$1.30/kg Cl ₂ + facility life cycle
	Hydrogen peroxide solution injection	Oxidize dissolved sulfides to sulfate	Rapid reaction rate Simple equipment	High chemical cost Unstable in storage	1 mg H ₂ O ₂ /mg sulfide	\$3/m³.d	\$4.5/kg H ₂ O ₂ + facility life cycle
	Nitrate addition (BIOXIDE™)	Provide chemical source of oxygen preferred over sulfate by bacteria	Slow-reacting; long lasting Low chemical hazard Simple equipment	High chemical cost Adds nitrogen	10 mg NO₃ /mg sulfide	<\$1.5/m ^{3.} d	\$2.00/kg NaNO ₃ + facility life cycle
Precipitation of sulfides from wastewater	Iron salts such as ferrous sulfate or ferric chloride	Formation of solid particles of insoluble metallic sulfide	Simple equipment Usually available	Increases metal loading downstream	2 mg Fe/mg sulfide	<\$1.5/m ^{3.} d	\$11/kg Fe + facility life cycle
Alkaline pH shock of wastewater	Caustic Shocking: Periodic (weekly) dosing with sodium hydroxide solution	Upset slime layer and temporarily reduce sulfide generation	Minimal capital investment Moderate chemical cost	Hazardous chemical handling Unpredictable effectiveness	As required to produce target pH	<<\$1.5/m ³ .d	varies

^{*}One typical dosage shown; actual dosages vary widely, and pilot testing is recommended to confirm actual required dosage

## **Comparison of Alternatives**

Both the sampling results and modeling exercise indicate the production of sulfides in the collection system at levels that make liquid phase sulfide control a cost-effective part of an integrated odor management strategy. As part of an initial screening of options, CH2M HILL identified several liquid phase treatment alternatives that the City could initiate within the collection system. A short list of options that would most likely provide an acceptable level of sulfide control was developed that includes:

^bApproximate capital cost in \$ shown for installation of treatment at one site for 40,000 m³/day wastewater flow

^cApproximate chemical cost shown in \$ on m³/day unit basis (shown as m³ d) on dry weight basis and in required form (e.g., solution) Sources: USEPA, 1985; Sulfide in Wastewater Collection and Treatment Systems, presented to ASCE, 1989; and CH2M HILL

- Ferric Chloride (iron salts) addition the iron reacts with sulfide molecules to
  form a non-dissolvable product that is removed in the clarifiers of the treatment
  facility. If available, ferrous chloride can also be used. Ferrous chloride is
  produced by metal products producers during the "pickling" process of raw
  steel.
- Bioxide[™] addition this proprietary product adds nitrates to the wastewater, thereby preventing the production of sulfide compounds.
- Shock dosing using 25% Sodium Hydroxide solution this process raises the pH in the wastewater to more than 12 for a contact period of 20 minutes and is performed approximately every 10 to 14 days. The high pH condition kills the sulfide-generating bacteria. However, immediately following treatment, sulfide-generating bacteria repopulate the sewer and sulfide production begins to increase.

Table 14 provides information on differences in chemical demand and usage for the anticipated liquid phase treatment assumed to be used for five months during the dry season only (June-October), based on an annual average flow of 5.7 mgd. A summary of the cost evaluation results for all odor control alternatives is presented in Table 15. Material Safety Data Sheets (MSDS) for each chemical considered are included in Appendix K.

TABLE 14
Dosages and Annual Costs for Chemicals Evaluated

Item	Ferric Chloride (FeCl ₃ )	Calcium Nitrate (Ca(NO ₃ ) ₂ ) (Bioxide ^{1M} )	Sodium Hydroxide (NaOH) ¹
Interceptor to be Dosed	Boyd	Boyd	Southside
Dosing Location	Boyd Lake PS	Boyd Lake PS	Southside PS
Assumed Chemical dosage	20 lb FeCl ₂ /lb sulfide removed	1.3 lb Ca(NO ₃ ) ₂ /lb sulfide removed	3,125 lb/MGD wastewater
Chemical unit cost	\$0.15 lb active chemical (37% solution)	\$1.95/gallon	\$1.0/lb active chemical (50% solution)
Chemical Required (lbs/day)	2,552	189	17,902/dose
(gallon/day)			
Chemical Costs (\$/day)	\$378	\$367	\$17,902/dose
Chemical Costs (\$/season)	\$68,085	\$66,683	\$268,567

¹ Shock dosing once every 10 days.

TABLE 15
Cost Evaluation of Liquid-Phase Odor Control Alternatives

Cost Type	FeCl₂	Odor Control Alternative Bioxide TM	es NaOH
Capital cost ¹	\$35,000	\$20,000	\$0
Pump replacement cost ²	\$7,000	\$7,000	\$0
Annual Chemical Cost	\$68,085	\$66,383	\$268,567
Total 20-Year Life Cycle Cost ³	\$1,004,472	\$965,281	\$3,816,411

¹Capital costs include pumps, tanks, and containment and do not include additional building and SCADA costs

² Assume metering pumps replaced once every 10 years.

CH2M HILL considered both economic (capital, operating and maintenance costs) and qualitative (non-monetary) criteria when evaluating the four alternatives. Table 16 contains a summary of our assessment of the qualitative criteria. A rating value developed by City staff allowed CH2M HILL to rank the three technologies. A weighting level of 3 is considered the most favorable and a rating value of 1 is least favorable. The technology with the highest total is considered the most favorable from a non-economic perspective. Some evaluation criteria were more heavily weighted to reflect their higher importance. A weight of 1 is least important and a 3 most important. The alternatives are then ranked, with the highest weighted score ranked the highest.

TABLE 16
Qualitative Evaluation of Liquid-Phase Odor Control Alternatives

Evaluation Criteria	Criterion Weight	Ferric Chloride (FeCl₃)	Chemical Alternat Bioxide TM (Ca(NO ₃ ) ₂ )	Sodium
Proven technology/reliability	3	3	3	2
Odor removal efficiency	3	3	2	2
Space requirements	2	2	1	3
Maintenance requirements	1	1	2	3
Operational Ease	2	2	3	2
Hazardous nature of materials	3	1	3	1
Total Weighted	Score	30	34	28
Ranking		2	1	3

³ Life cycle costs include capital costs plus present worth of annual costs using an interest rate of 3.5% for 20 years.

## **Liquid Phase Treatment Conclusions**

Sampling results, combined with a modeling exercise using in-house models indicates that factors within the wastewater collection system contribute significantly to odor emissions at the treatment plant. These factors include long detention times and numerous forcemains that lead to the production of  $H_2S$  and other reduced sulfur compounds.

The modeling exercise indicates that the Boyd Interceptor and Boyd Relief Interceptor contribute most to the sulfides at the plant. The Southside Interceptor contributes a small portion of the overall sulfide loading to the plant, but the sampling program showed that the forcemain discharge generates high peak hydrogen sulfide concentrations within the headworks area. These peaks likely generate short-term odor releases that could lead to odor complaints. CH2M HILL recommends an odor management strategy that addresses both of these contributors.

Literature and CH2M HILL's experience indicates that liquid phase treatment of odor generating compounds in the collection system forms a cost effective component of multi-phased odor management plans for wastewater treatment facilities when the influent dissolved sulfide concentrations exceed 1.0 mg/L. The modeling exercise predicts a worst-case influent wastewater dissolved sulfide concentration of more than 5 mg/L. Accordingly, the City should consider incorporating a liquid phase program as part of the overall control strategy.

CH2M HILL has considered several sulfide control options. Ferric Chloride addition has the second highest life-cycle costs and ranks third in the non-economic evaluation. Ferric chloride requires special handling procedures and is a corrosive product. Bioxide™ has the lowest life-cycle cost, but may require more stations than ferric chloride. However, the product is relatively harmless and does not have the same handling and storage requirements. Based on the dosage rates and approximate chemical costs used in the analysis, sodium hydroxide (NaOH) appears to be cost prohibitive. The NaOH alternative cost is calculated on shock dosing every 10 days, and actual shock dosing requirements could vary. However, even with major adjustments in unit chemical costs and dosage requirements, the costs would not be competitive with the other chemicals.

CH2M HILL recommends that the City begin with Bioxide™ (or equivalent) on the basis that it is the most cost effective and will be added at the lift stations, which will provide an additional benefit of corrosion control in the collection system. The City should consider contacting Castle Rock, Colorado staff regarding their Bioxide™ program and its success. The following approach is suggested for proceeding with the liquid phase, sulfide control program:

- 1. Conduct a pilot test with Bioxide™ (or equivalent) being added at the Eastside lift station. During the pilot test, conduct sampling of both the dissolved sulfide levels of the influent and the H₂S concentrations at the odors sources.
- 2. If the pilot test is effective, implement permanent Bioxide™ (or equivalent) dosing stations for Boyd systems first (Eastside and Boyd Lake lift stations), then addresses the smaller contributors should further odor reductions be needed.

- 3. If the Bioxide™ is not effective, conduct a pilot test with another liquid phase treatment chemical, such as ferric chloride.
- 4. Commit to a data collection program that will allow stakeholders to evaluate the impact of the proposed mitigation measures. The data collection program would involve monthly sampling of the dissolved sulfide levels at the influent, as well as sampling the odor sources for H₂S using a Jerome meter.

## **Conclusions**

The baseline odor assessment provides useful information that will enable the development of effective odor control improvements. The assessment establishes:

- Extent of off-site impacts from the existing treatment plant.
- 2. Process units that are potential contributors to off-site odor impacts.
- 3. Effectiveness of various odor control scenarios.

The Loveland WWTP currently has several significant sources that contribute to off-site odor impacts, including the digester boiler room vent, aerated grit chamber, DAFT, and trickling filters.

The worst-case baseline modeling, based on the maximum  $H_2S$  concentrations obtained from Jerome meter sampling events in October 2003, shows that the current odor impacts above the 7 D/T odor threshold extend off-site mainly in northeast and southwest directions. The number of hours above 7 D/T is greatest along the northern side of the plant boundary (over 1,500 hours per year). The average condition baseline modeling, based on the flux chamber sampling results, shows the much smaller impact than the worst-case baseline modeling, although the shape of the isopleths is similar. The isopleths also tend to extend mainly in northeast and southwest directions. The highest exceedences (about 1,000 hours per year) also occurred at the north end of the plant.

The control modeling results show that odor control approaches represented at Stage 1 to Stage 4 can efficiently reduce the off-site impact. The maximum 5-minute off-site odor impact is reduced from about 1,130 D/T at Baseline to about 150 D/T at Stage 4. The highest exceedence is reduced from about 2,700 hours per year in the Baseline modeling to approximately 840 hours per year at Stage 4. They either eliminate the identified big odor sources completely, such as the trickling filter, or convert the major odor sources into the odor control scrubbers that emit significantly less odor, such as the chemical scrubber treating the headworks and grit chambers at Stage 3. In order to bring the Loveland WWTP within their desired odor control goal of less than 7 D/T 99percent of the time, the City may be required to conduct additional odor control. The primary clarifiers would be the next significant source of odor control.

## Recommendations

In general, Loveland WWTP should continue its ongoing policy of implementing source control and general odor prevention O&M policies, procedures, and approaches to ensure that:

- The headworks scrubber is fully functional and effective
- Short-term fugitive sources are handled
- Process equipment going out of service or drained is controlled

The results of the modeling conducted as part of this Odor Management Plan indicate that the currently planned odor control projects will move the Loveland WWTP toward its odor reduction goal of no odors less than 7 D/T 99 percent of the time, set as part of this project. In addition, some immediate suggestions are provided to help reduce the off-site odor impact quicker.

### **Immediate Recommendations**

Several other best management practices (BMPs) and operation and maintenance (O & M) enhancements could improve the odor prevention program at the Loveland WWTP. The BMPs and O & M enhancements can be implemented immediately and can help reduce the risk of off-site odor impacts. These BMPs and O & M enhancements include:

- Investigate the boiler room for potential leaks to the HVAC system. As recommended
  in Stage 1, this is a significant odor source should be reduced through fairly minor
  investigation and repair.
- General housekeeping to reduce fugitive emissions. Several housekeeping measures are already in place such as:
  - Primary clarifiers are cleaned regularly.
  - Digester gas is combusted.
  - Vessels are cleaned immediately after they are removed from service and drained.

Additional housekeeping measures to consider include washing down process tanks during draining to reduce odor generation and adding hypochlorite tablets to the tanks that are already drained and have small amounts of liquid collected on the bottom.

Monitor the sludge blanket in the primary clarifiers to keep it at a minimum and, if
possible, reduce the amount of vertical drop in the effluent weirs. The drop at the
effluent weirs promotes stripping of odorous compounds.

As the community surrounding the Loveland WWTP becomes more odor sensitized it will be increasingly more important for the Loveland WWTP to be perceived as a good neighbor. Several recommendations are provided to improve the Odor Response Program, be proactive in the neighborhood, and respond to off-site odor complaints. Loveland WWTP should consider increasing public outreach efforts and informing key community members

of plant upset conditions, for example, and steps being taken to address odor events. One way to increase community involvement is to invite members of the community on-site before and after anticipated events that would cause an increase in odors.

Additional Odor Response actions to consider include:

- Odor Monitoring. Odor monitoring programs are helpful to understand the plant's odor sources and the conditions that contribute to significant odor problems off-site. Loveland WWTP should develop on- and off-site odor monitoring using operators or selected staff to routinely check for odors and their off-site impacts at selected odor monitoring stations. This team should visit odor monitoring stations once a day, as well as monitor collection system locations to ensure that the collection system is not adding to the odor problem. The Jerome meter should be used, as well as the nose, to estimate odor and H₂S levels. The Jerome meter sampling performed as part of the Odor Management Plan can be considered the first round of odor monitoring.
- Consider installing a meteorological station at the Loveland WWTP to provide better data for future odor modeling.
- Develop response protocols for high odor events. Loveland WWTP should develop
  response protocols for high odor events that consist of a list of immediate odor control
  strategies available to prevent or reduce the odor from traveling off-site or adversely
  impacting the community.
- Have on hand portable odor control units that can be used for equipment take downs, digester cleanings, and short-term odor vents that need controls.

## **Short-Term and Long-Term Recommendations**

Based on the results of the modeling analysis, short- and long-term odor control improvements are also recommended, as shown in Table 17. These recommendations are based on the City's goal of reducing off-site odor impacts of less than 7 D/T 99 percent of the time.

Plant emissions are variable and so are removal efficiencies of odor control systems. After each phase of capital improvements, the sources should be resampled and the odor dispersion model rerun to predict the current plant conditions. This will enable the City to assess the effectiveness of the phased recommendations and confirm if all the capital improvements below are required, or if there are other new odor sources that require control. The cost of a Jerome meter is included in Odor Control Stage 3 so the City can conduct the confirmation sampling. The effort to re-run the dispersion model is included in Stage 4 to confirm the odor control benefits of the stages up through Stage 4. The long-term recommendations provided in Table 17 may or may not be necessary in the future, and careful evaluation should be performed before implementation.

The long-term recommendations describe in general what type of odor control can be provided for each source. Odor control consists of capturing the air with covers and/or equipment enclosures and treating the air with odor control equipment. Many odor control technologies are available to meet the newer, more stringent odor prevention and control

criteria. The technologies that are considered for the City are liquid-phase treatment, single-stage packed tower scrubbers, carbon adsorption, and biofiltration. For the purposes of budgetary planning, a reasonable control technology has been assumed. As the City progresses with each project, a detailed technology selection should be conducted.

A summary of the recommended long-term improvements, with cost estimates, are included in Table 18. The detailed cost estimates are included in Appendix L. CH2M HILL recommends that the City plan to incorporate Stages 1 through 5 in their current CIP. It is anticipated that this level of odor control will meet the proposed odor control standard, given the conservative nature of the analysis. For the City to have a zero odor emissions plant, the cost would include all stages and would be approximately \$5 million.

The cumulative odor reductions to be expected from each odor control stage, including liquid phase treatment, are shown in Figure 5. It is assumed that liquid phase treatment is implemented after the trickling filter is taken off-line (Stage 1) and the digester boiler room HVAC intake vent is relocated (Stage 2). For Stages 3 through 7, the predicted odor reduction is shown for each stage with and without the cumulative impact of liquid phase treatment. As additional odor control improvements are implemented, the additional odor reduction impact of liquid phase treatment becomes insignificant. However, liquid phase treatment continues to have benefit by reducing the chemical requirements for the odor control scrubbers.

TABLE 17
Summary of Recommendations for Loveland WWTP Odor Sources

Odor Source	Immediate Recommendations	Short-Term Recommendations	Long-Term Recommendations
WWTP Site	- Select a liquid phase chemical treatment process Consider a short-term, shock dosing program (sodium hydroxide) on the Southside forcemain to reduce odor peaks at the treatment plant.	- Develop a phased implementation program that addresses the Boyd systems first, then addresses the smaller contributors should further odor reductions be needed (\$35,000 + up to \$68,000 annual cost for seasonal use)	Address future odor impacts from new sources under CIP program.  Update Odor Management Plan after each phase of the odor control program to verify results and if additional improvements are still needed.  Consider odor control for primary clarifiers if still getting small odors that add up from fugitive emissions occurring from all sources.
Digester Boiler Room Vent	<ul> <li>Investigate boiler room, boilers, and digester system for potential fugitive leaks into the boiler room HVAC. Repair any leaks found.</li> </ul>	<ul> <li>Relocate HVAC intake vent away from the digesters and digester overflow weirs (Stage 2)</li> </ul>	If relocating HVAC vent does not reduce odors, may be required to install odor control for boiler room HVAC.
Aerated Grit Chamber	None recommended	<ul> <li>Cover aerated grit basin with aluminum covers and vent foul air to new, temporary carbon odor control unit (water regenerable carbon) (Stage 3)</li> </ul>	Will be replaced as part of new or modified Headworks Building
DAF Thickener	<ul> <li>Routine cleaning</li> <li>DAF Thickener</li> <li>Keep the doors closed and provide better</li> <li>ventilation or replace fan</li> </ul>	None recommended	Confirm offsite impacts from DAF thickener If necessary, maintain negative pressure inside DAF, and ventilate foul air to new odor control equipment
Trickling Filters	- Remove trickling filters from service in December 2004 (Stage 1)	- None recommended	None recommended

TABLE 17
Summary of Recommendations for Loveland WWTP Odor Sources

Odor Source	Immediate Recommendations	Short-Term Recommendations	Long-Term Recommendations
	- Carefully consider wind direction and strength when open garage and removing grit bins		Accelerate the schedule for the Headworks Building and associated odor control prior to the WAS thickening project. Start design in 2005. Screw pumps and aerated
Headworks Building	<ul> <li>Direct as much building air as possible into the carbon southber seal off rooms and</li> </ul>	hydrogen sulfide loads for the odor control and hydrogen sulfide loads for the odor control and hydrogen sulfide hatter odor and control or the hatter odor and control or the	gnt chamber odor sources will be replaced as part of the new or modified Headworks building.
	bins to better focus odor removal and supply air.	collection system.	Ventilate new Headworks facility to minimum of 12 to 20 air changes per hour (ACH), and treat with new single-
ARTH AND AND HANDA AND HANDA AND AND AND AND AND AND AND AND AND	<ul> <li>Minimize entry into the building.</li> </ul>		stage chemical scrubber that is polished by the carbon scrubber or biofilter (Stage 4).
Screw Pumps	None recommended	<ul> <li>Install liquid-phase treatment that will reduce the hydrogen sulfide loads for the odor control and provide better odor and corrosion control in the collection system.</li> </ul>	Will be replaced as part of the new or modifled Headworks Building
Primary Clarifiers	<ul> <li>Consider flooding launders and removing sludge blankets quickly.</li> </ul>	- If odor complaints persist, consider odor neutralizer for primary clarifiers on days when strong odor/H ₂ S is observed (\$10,000 + up to \$8,000 annual chemical costs)	After completion of improvements listed above and if odor complaints persist, cover primary clarifiers, splitter box, influent junction boxes, and effluent junction box and ventilate to new odor control equipment (Stage 6).
	- Maintain burner ignition system		THE REPORT OF THE PROPERTY OF
Flare	- Increase preventative maintenance programs and focus during odor compliant season	None recommended	After completion of improvements listed above and odor complaints persist Install enclosed flare system
Aeration Basins	None recommended	- Resample aeration basins to ensure they are not - a significant source of remaining off-site odor impacts	After completion of improvements listed above and if odor complaints persist, odor control would be to cover and treat similar to primary clariflers (Stage 7).
		THE PROPERTY OF THE PROPERTY O	والمقاولا والمتعلق والمقاول والمتعاول والمتعاو

TABLE 17
Summary of Recommendations for Loveland WWTP Odor Sources

		Laboration of the state of the	
Odor Source	Immediate Recommendations	Short-Term Recommendations	Long-Term Recommendations
	- Routine maintenance and cleaning		None currently recommended. If odor complaints persist
Digesters	<ul> <li>Removal of all foam from the cover immediately</li> </ul>	None recommended	after the above recommendations are implemented, consider retrofitting digesters to have fixed roofs. Fixed roof digesters to discovery would aliminate flightling leake from the
	<ul> <li>Conduct routine maintenance to prevent foaming and upset conditions</li> </ul>		organics would eminister tograve reach not are circumference of the digester (Stage 7)
Biosolids Truck Loading	Biosolids Truck None recommended Loading	None recommended	None recommended. Odor control would be an enclosed truck loading area with odor control provided.

11

TABLE 18
Cost Summary for Long-Term Recommendations

Odor Control Stage	Long Term Recommendations	Air Flow Rate (cfm)	Capital Cost*	Annual Cost	Timing
1	Discontinue use of trickling filters	NA	\$10,000	\$0	2004
2	Rearrange digester boiler vent HVAC system	NA	\$200,000	\$0	2005
LPT	Conduct a pilot test of Bioxide™ or equivalent chemical	NA	\$37,000	NA	2005
	Implement a liquid phase treatment program	NA	\$35,000	\$68,000	2005
3	Cover aerated grit chamber and vent to a carbon scrubber	250	\$68,000	\$6,000	2005
4	Provide odor control for modified Headworks processes, including screw pumps and influent collection well, within existing Headworks building. Vent air from Headworks building a new chemical scrubber polished with bioscrubber or carbon to achieve 99% removal efficiency.	13,000	\$892,000	\$87,000	2006 / 2009
5	Vent air from DAFT in a new carbon scrubber.	800	\$84,000	\$18,000	2008
6	Cover primary clarifiers and vent to new chemical scrubbers	3,800	\$1,614,000	TBD	TBD
7	Cover aeration basins and vent to new chemical scrubbers. Replace digester covers with fixed roof covers	8,600	\$3,353,000	TBD	TBD

^{*}Total capital costs include construction and engineering costs. Construction costs include 30% contingency; engineering costs are estimated at 25% of construction cost cfm = cubic feet per minute

The average annual costs are also estimated in Table 18. For future operations at the Loveland WWTP with full scale odor control, the annual operating costs for odor control could be as high as 5 to 15 percent of the annual operating budget. This is what a typical WWTP spends on odor control.

## References

Diosey, Phyllis G., Maureen E. Hess, and Larraine Farrell, Evaluation of Alternative Dispersion Models for Use in Odor Management, WEFTEC 2002 75th Annual Technical Exhibition and Conference, Conference Proceedings, WEF, Alexandria, VA.

Odor Control in Wastewater Treatment Plants, WEF Manual of Practice No. 22, Water Environment Federation, 1999, pg. 8.

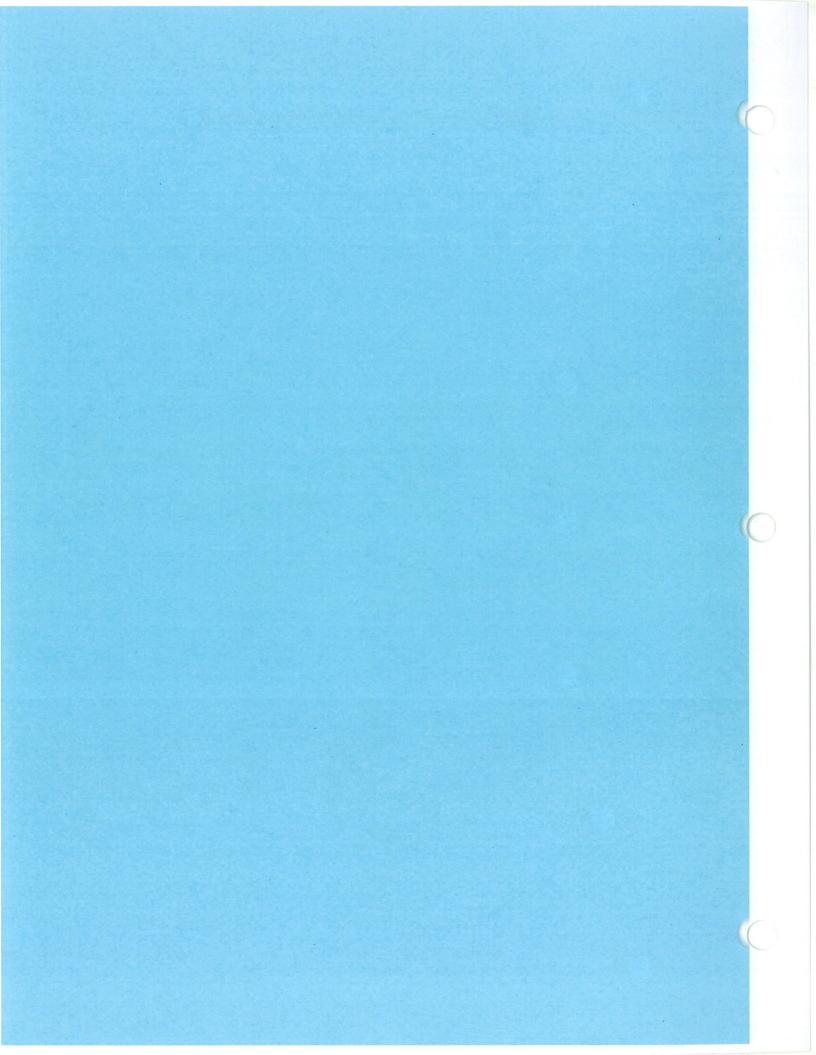
Porter, R.C.; W.G. Hoydysh; and E.T. Barfield. 1994. Odors: Demonstrating Compliance at Publicly Owned Treatment Works. WEF Specialty Conference Proceedings, Jacksonville, FL, Odor and Volatile Organic Compound Emission Control for Municipal and Industrial Wastewater Treatment Facilities, Water Environment Federation, pp. 11-35 to 11-51.

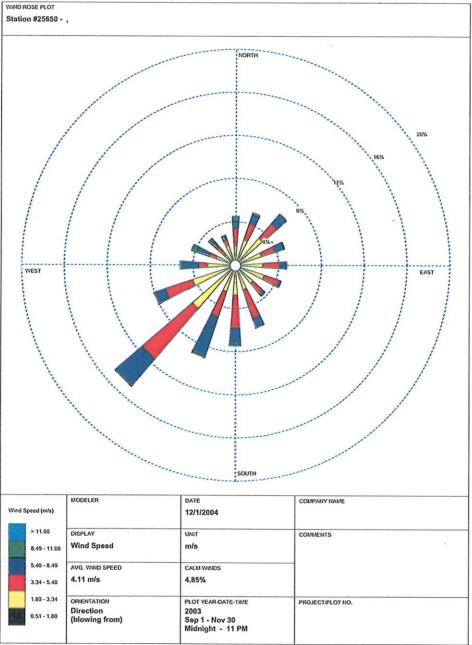
TNRCC, Air Permit Technical Guidance For Chemical Sources: Flares and Vapor Oxidizers, October 2000.

CH2M HILL, Odor Control Investigation and Odor Response Manual for the South Treatment Plant, July 2003.

CH2M HILL, Spokane Advanced Wastewater Treatment Plant PMO Odor Management Plan, December 2003.

# Appendix A – Windroses for 2003 by Season

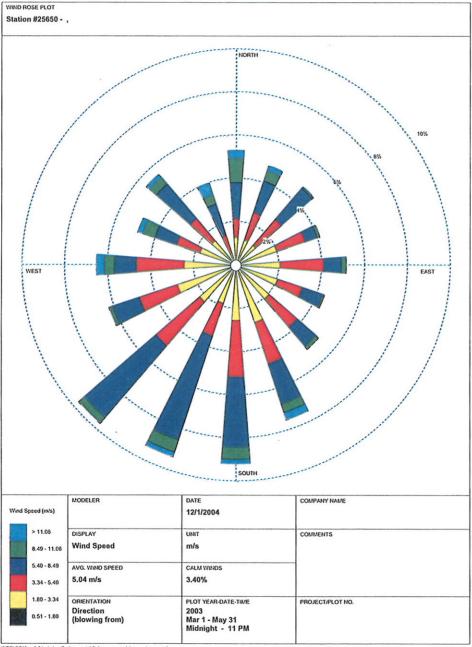




WRPLOT View 3.5 by Lakes Environmental Software - www.lakes-environmental.com

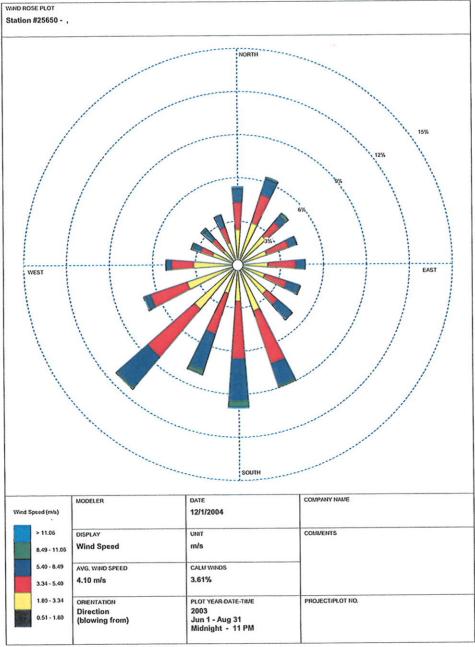
The state of the s

They are



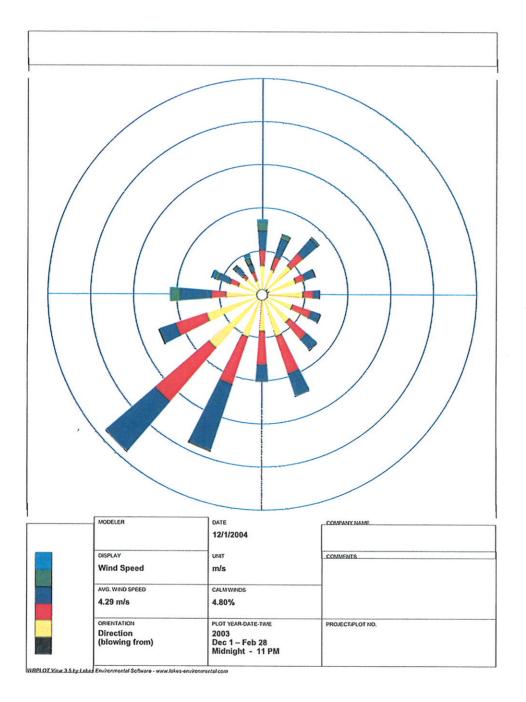
WRPLOT View 3.5 by Lakes Environmental Software - www.lakes-environmental com





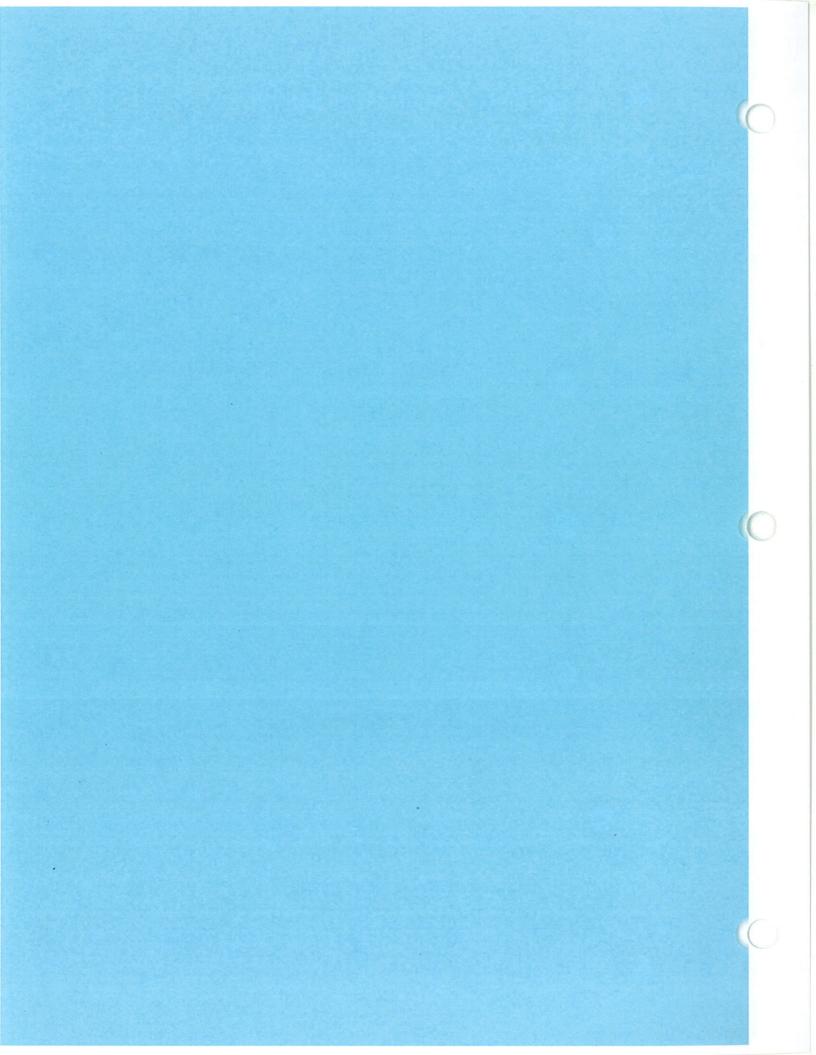
WRPLOT View 3.5 by Lakes Environmental Software - www.lakes-environmental.com







**Appendix B – State of Colorado Regulation 2, Part A – General Provisions** 



#### REGULATION NO. 2 Odor Emission Regulations Table of Contents

PART A GEN	IERAL PROVISIONS	. 1
PART B HOU	JSED COMMERCIAL SWINE FEEDING OPERATIONS	2
l.	Applicability	, <u>た</u>
11.	Definitions	. <u>2</u>
111.	Odor Standards for Housed Commercial Swine Feeding Operations	. ಒ ନ
	III.A. Odor Concentration Standard at Property Boundary	. o ล
	III.B. Odor Concentration Standard at Any Receptor	. บ ล
IV.	Technology Requirements for Process Wastewater Vessels and Impoundments	. 0
	***************************************	7
	IV.A. Anaerobic Process Wastewater Vessels and Impoundments	. 7
	IV.A.1. New or Expanded	. 7
	IV.A.2. Existing	. 7
	IV.A.3. All Anaerobic process Wastewater Vessels and Impoundments IV.B. Aerobic Impoundments	. 8
		10
	IV.B.1. New	10
V.	IV.B.2. Existing	10
٧.	Setback Requirements for New Land Waste Application Site or New Waste	
	Impoundment	10
		10
VI.	The same of the sa	11
VI.	Permit to Operate	11
		11
	VI.A.1. Existing Sources	11
	VI.A.2. New or Expanded Sources	12
	VI.A.3. New, Expanded, and Existing Sources	12
	VI.A.4. Transfer or Assignment of Ownership VI.B. Option for a Pre-Application Meeting	12
	the state of the s	13
	VI.C. Application for a Permit to Operate	13
	VLD. Content of Permit to Operate and Application for a Permit to Operate	4 44
	VI.E. Hearing and Public Comment Requirements	15
	The state of the s	17
		18
	= or and a difficulty of the control	19
		19
VII.		20
VII.	Odor Management Plan	20
VIII.	Modification or Reopening of a Permit to Operate	21
	VIII.A. Modification	21
<b>8</b> ×-	VIII.B. Revocations/Reopening for Cause	22
IX.	Specific Odor Control Requirements	22
	IX.A. Mandatory Specific Odor Control Requirements	23
•	IX.A.1. Swine Confinement Structures	23
	IX.A.2. Solid Waste and Process Wastewater Collection, Storage, and	
	Treatment Systems IX.A.3. Manure Composting Storage Sites	24
•	IX.A.3. Manure Composting Storage Sites	25

		IX.A.4. Land Application
		IX.A.5. Carcass Disposal
	IX.B.	Recommended Specific Odor Control Requirements
		IX.B.1. Swine Confinement Structures
		IX.B.2. Solid Waste and Process Wastewater Collection, Storage, and
		Treatment Systems
		IX.B.3. Manure Composting Storage Sites
		IX.B.4. Land Application
		IX.B.5. Carcass Disposal
X.	Testing	g, Recordkeeping, Reporting, and Monitoring Requirements 30
	X.A.	Testing Requirements
	X.B.	Recordkeeping Requirements
	X.C.	Monitoring Requirements
	X.D.	Reporting Requirements
XI.	Enviro	nmental Leadership Program
	XI.A.	Applicability
	XI,B,	Compliance Demonstration
XIII.	Statem	nent of Basis, Specific Statutory Authority, and Purpose
	XIII.A.	February 19, 1999

#### Regulation History

Adopted: Effective:

March 11, 1971 April 20, 1971

Revised: Effective:

February 19, 1999 March 30, 1999

#### PART A GENERAL PROVISIONS

Pursuant to Section 25-7-109(2)(d), C.R.S., the following Emission Regulations are issued:

- I. No person, wherever located, shall cause or allow the emission of odorous air contaminants from any single source such as to result in detectable odors which are measured in excess of the following limits:
- I.A. For areas used predominantly for residential or commercial purposes it is a violation if odors are detected after the odorous air has been diluted with seven (7) or more volumes of odor free air.
- I.B. In all other land use areas, it is a violation if odors are detected after the odorous air has been diluted with fifteen (15) or more volumes of odor free air.

I.C.

- I.C.1. When the source is a manufacturing process or agricultural operation, no violation of Sections I.A. and I.B., Part A, of this Regulation No. 2 shall be cited by the Division, provided that the best practical treatment, maintenance, and control currently available shall be utilized in order to maintain the lowest possible emission of odorous gases and, where applicable, provided there is compliance with Item 4r of the Colorado Department of Health Pasteurized Fluid Milk and Milk Products Regulation adopted April 18, 1967. In determining the best practical control methods, the Division shall not require any method which would result in an arbitrary and unreasonable taking of property or in the practical closing of any lawful business or activity, if such would be without corresponding public benefit.
- 1.C.2. For all areas it is a violation when odors are detected after the odorous air has been diluted with one hundred twenty seven (127) or more volumes of odor free air in which case provisions of Section 1.C.1., Part A, of this Regulation No. 2 shall not be applicable.
- II. For the purposes of this Part A of Regulation No. 2, two odor measurements shall be made within a period of one hour, these measurements being separated by at least fifteen (15) minutes. These measurements shall be made outside the property line of the property from which the emission originates.
- III. For the purposes of this Part A of Regulation No. 2, personnel for evaluating odors shall be selected using an "intensity rating test" as outline in "Selection and Training of Judges for Sensory Evaluation of the Intensity and Character of Diesel Exhaust Odors." USPHS Pub. #999-AP-32.
- IV. The Barnebey-Chaney Scentometer, suitable calibrated, or any other instrument, device, or technique designated by the Colorado Air Pollution Control Division, may be used in the determination of the intensity of an odor and may be used as a guide in the enforcement of this Part A of Regulation No. 2.
- V. The provisions of this Part A of Regulation No. 2 shall apply throughout the State of Colorado. Except that this Part A of Regulation No. 2 shall not apply to housed commercial swine feeding operations.